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Energy and Power 101 – Basics of conversions and calculations and application to WRRFs

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David A. Vaccari, Ph.D., P.E., BCEE, F.ASCE

dvaccari@stevens.edu



Outline

- Energy and Power Units
- Electrical energy
- Chemical Energy of COD
- Hydraulic energy and pumping
- Aeration energy
- Energy recovery from digester gas
- Social cost of energy (carbon)



Energy Conversion

$$\mathbf{Work = Force \cdot d}$$

$$[N \cdot m] = \mathbf{Joules}$$

$$[ft \cdot lb_f]$$

$$[BTU]$$

$$\mathbf{Force = mass \cdot acceleration}$$

$$[kg \cdot m / s^2] = \mathbf{Newtons}$$

$$1 \text{ BTU} = 1054.4 \text{ Joules } (= \sim 1 \text{ kJ})$$

$$1 \text{ BTU} = 778.15 \text{ ft} \cdot \text{lb}_f = 1.355 \text{ J}$$

$$1 \text{ kW} \cdot \text{hr} = 3600 \text{ J} = 3412 \text{ BTU}$$

$$1 \text{ calorie} = 4.184 \text{ J}; \quad 1 \text{ Calorie} = 1000 \text{ calories!}$$



Power Conversion

$$\mathbf{Power = Energy/time}$$

S.I. Unit: $[Joules/second] = [kg \cdot m^2 / s^3] = Watts$

$$1 \text{ W} = 3.414 \text{ BTU/hr}$$

$$1 \text{ hp} = 550 \text{ ft-lb/s}$$

$$1 \text{ hp} = 745.7 \text{ W} (= \sim 0.75 \text{ kW})$$

$$1 \text{ hp} = 17.9 \text{ kWh/day}$$



Electrical Power

Volts = Energy per unit charge = *Joules/Coulomb*

(1 Coulomb = $6.24 \cdot 10^{18}$ charges)

Current = Flow of charge per unit time = *Coulomb/second*

Power = Energy per unit time = Joules/second = Watts

$$\text{Joules/second} = \text{Watts} = \text{Joules/Coulomb} \cdot \text{Coulombs/second}$$

$$P = E \cdot I$$

$$120V \cdot 20Amps = 2400 W$$



Bad energy unit #1

What is a kW per hr?

$$kW = kJ/second$$

$$kW/hr = kJ/sec/hr = kJ/sec \cdot \frac{1}{3600}$$



Bad Energy Unit #2:

- Window air conditioner unit rating
- E.g. 12,000 “BTU”
- BTU per What?
- 12,000 BTU/second = 4.2 MegaWatts!
- 12,000 BTU/hour = 3,515 Watts ✓
- Note: A 12,000 BTU/hr A/C actually uses only about 1,170W
- Electric Power Usage =
Cooling power/Coefficient of Performance
- COP is typically about **3**
- $EER = (\text{Cooling Power in BTU/hr}) / (\text{Electric Power in W})$
- In this example, $EER = 12,000/1,170 = \mathbf{10.2}$

GE 12,000 British Thermal Unit WINDOW AIR CONDITIONER WITH REMOTE





Simple WWRF Energy Balance

- Chemical energy input (COD)
- Pumping energy
- Aeration energy
- Energy from digester gas

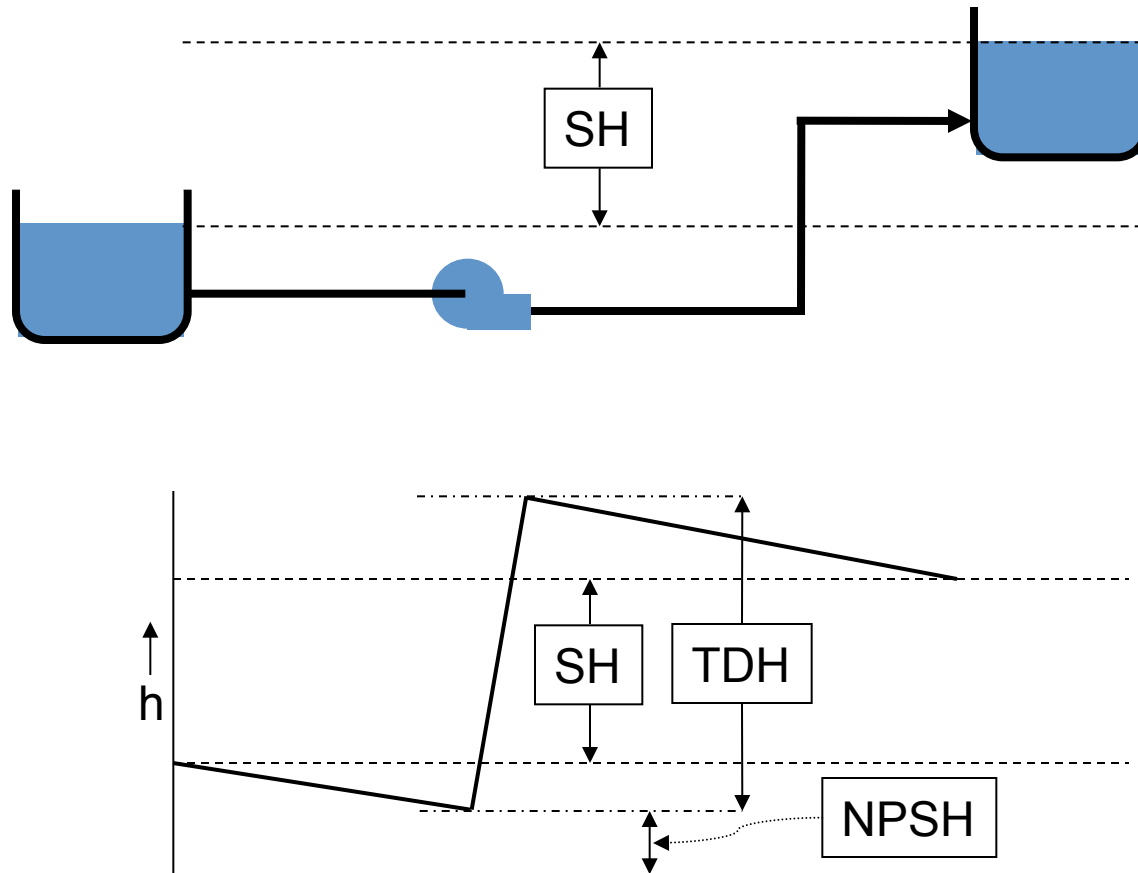


Energy from Influent COD

Influent flow rate	100,000	cu m/d
=	26.4	MGD
Influent VSS	96	g/cu m
Energy/COD	4	kWh/kgCOD
Influent COD Conc.	136	g/cu m
Influent COD Flux	13,632	kg/d
Energy input	54,528	kWh/d

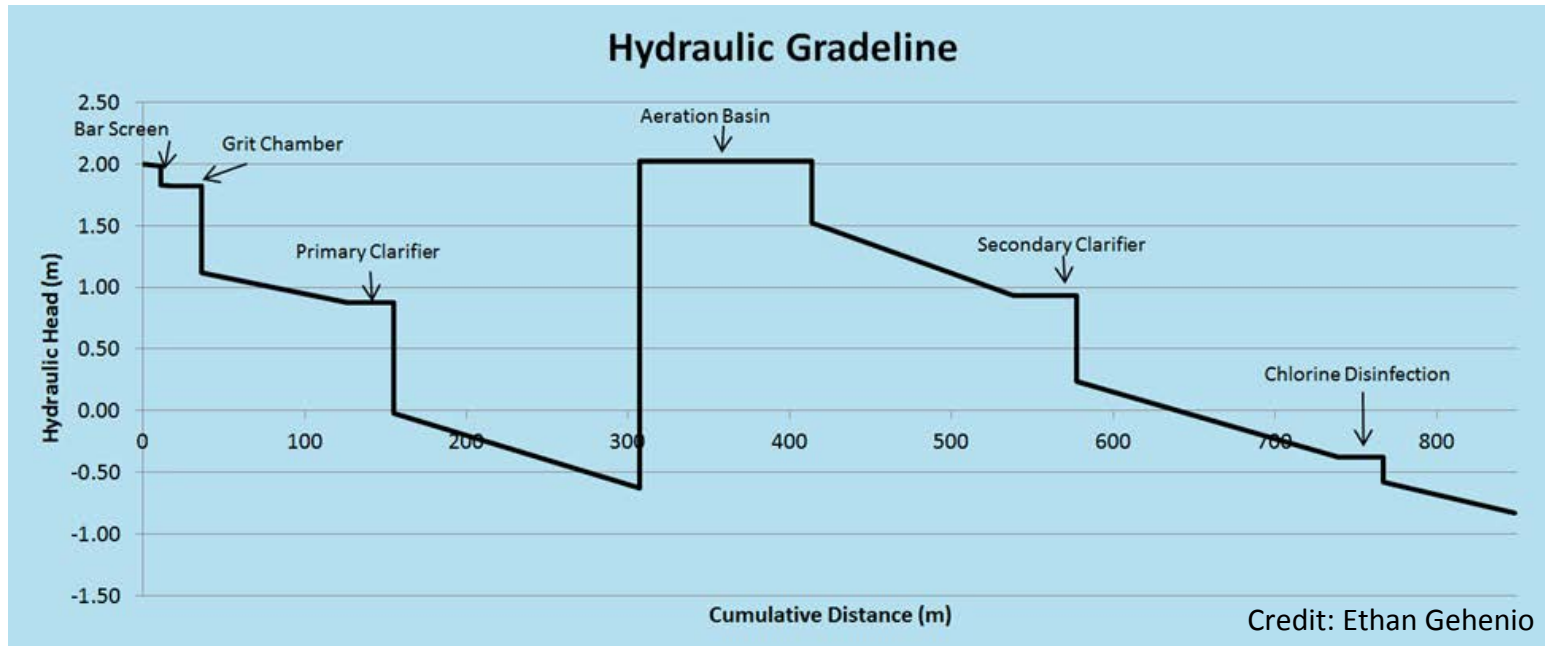


Hydraulic Energy Grade Line





Hydraulic Grade Line



Nominal headloss through plant: 5.5 meters (18 feet)

Water Power



$$\text{Water Power: } P \downarrow W = W \cdot h \downarrow L = Q \cdot \rho \cdot h \downarrow L$$

E.g. Pumping 26.4 MGD against a head change of 18 feet:

$$\dot{W} = 26.4 \times 10^6 \frac{\text{gal}}{\text{day}} \times 8.34 \frac{\text{lbs}}{\text{gal}} \times \frac{\text{day}}{86,400 \text{sec}} = 2550 \frac{\text{lbs}}{\text{s}}$$

$$P_W = \dot{M} \cdot h_L = 2550 \frac{\text{lb}}{\text{s}} \times 18 \text{ft} = 46,010 \frac{\text{ft} \cdot \text{lb}}{\text{s}}$$

$$P_W = 46,010 \frac{\text{ft} \cdot \text{lb}}{\text{s}} \times \frac{\text{hp} \cdot \text{s}}{550 \text{ft} \cdot \text{lb}} = 83.7 \text{hp}$$



Brake horsepower

$$P_B = \frac{P_W}{\varepsilon_P}$$

E.g. If the previous pump were 80% efficient:

$$P_B = \frac{83.7 \text{ hp}}{80\%} = 104.6 \text{ bhp}$$



Motor horsepower

$$P_M = \frac{P_B}{\varepsilon_M} = \frac{P_W}{\varepsilon_P \varepsilon_M}$$

E.g. If the motor were 85% efficient:

$$P_M = \frac{104.6 \text{ hp}}{85\%} = 123 \text{ hp}$$

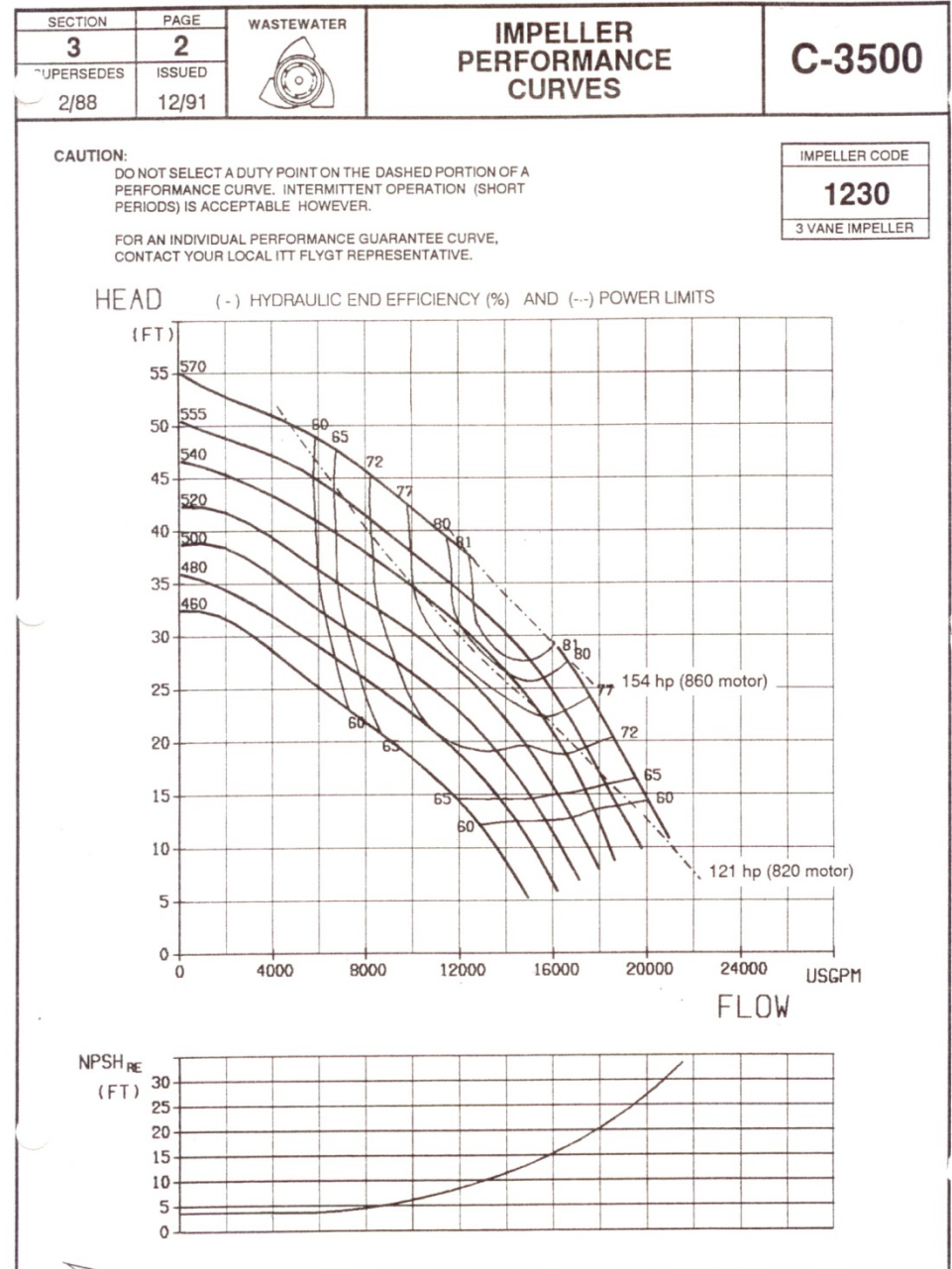
Note: 1 hp = 0.746 kW = 17.9 kWh/d; so

$$P_M = 123 \text{ hp} \cdot \frac{0.746 \text{ kW}}{\text{hp}} = 91.75 \text{ kW} = 2202 \text{ kWh / day}$$

$$2202 \text{ kWh/day} \cdot \$0.15 / \text{kWh} = \$330 \text{ per day} = \$120,565 \text{ per year}$$

Actual Pump Performance

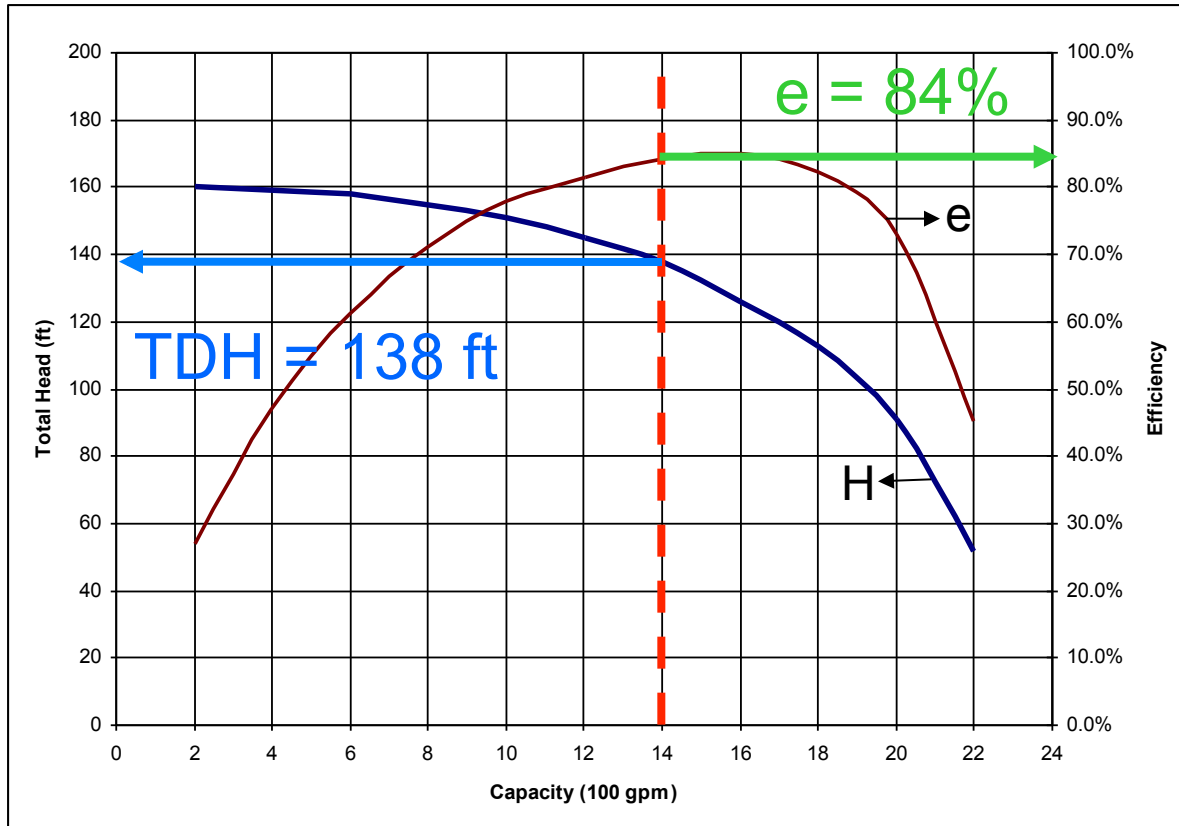
- The Pump Curve





Simplified Pump Curve

What will be the TDH, efficiency, and power requirement of this pump at **1400 gpm**?



$$P_W = 1400 \frac{\text{gal}}{d} \times \frac{8.34 \text{ lb}}{\text{gal}} \times \frac{\text{min}}{60 \text{ s}} \times 138 \text{ ft} \cdot \frac{\text{hp} \cdot \text{s}}{550 \text{ ft} \cdot \text{lb}}$$

$$P_W = 48.8 \text{ hp}$$

$$P_B = \frac{P_W}{\epsilon_P} = \frac{48.8 \text{ hp}}{0.84}$$

$$P_B = 58.1 \text{ hp}$$



S.I. Headloss Calculation

$$P \downarrow W = Q \cdot \rho \cdot h \downarrow L = M \cdot h \downarrow L$$

$$h \downarrow L = g \Delta h$$

$$P \downarrow W = M g \Delta h$$

Influent flow rate	100,000	cu m/d
=	26.4	MGD
Mass flow rate	1,157.41	kg/s
hL	5.5	meters
g	9.8	m/s/s
Pw	62,384	kg-m ² /s ³ [W]
Pw	1,497	kWh/day

Pump efficiency	80%	
Motor efficiency	85%	
Pumping power req'd	2,202	kWh/day



Empirical aeration system design

$$U \equiv \frac{Q \cdot (S_0 - S)}{V \cdot X} = F / M \cdot e \quad [\text{per day}]$$

$$SOUR = U - \frac{1.42}{\theta_c} \quad [\text{per day}]$$

$$OTR = OUR = SOUR \cdot X \quad [\text{kg/m}^3/\text{day}]$$

Fine bubble diffuser:

$$1.2 < OTE < 2.0 \quad [\text{kgO}_2/\text{kW-hr}]$$

$$OTP = V \cdot OTR / OTE \quad [\text{kW-hr/day}]$$

Q	100,000	cu m/d
=	26.4	MGD
S ₀	120	g/cu m
S	5.4	g/cu m
X (MLVSS)	1,110	g/cu m
V	25,000	cu m
F/M	0.43	per day
MCRT	6.77	days
e _B	95.5%	
U	0.413	per day
SOUR	0.203	per day
OTR=OUR	225.5	g/cu m/d
OTE	1600	gO ₂ /kWh
OTP	3,524	kWh/day



Sludge production mass balance

Primary removal	40%	VSS removal
Underflow VSS flux	3,840	kg/d
Act. Sl. Waste Flow	871	cu m/d
Waste VSS Conc.	3,331	g/cu m
Waste VSS flux	2,901	kg/d
VSS flux to digester	6,741	kg/d

Digester HRT	20	d
kd	0.03	per d
Kp	0.625	
VSS flux out of dig.	4,212.91	kg/d
VSS destruction rate	2,528	kg/d



Energy recovery from digester gas

Digester HRT	20	d
kd	0.03	per d
Kp	0.625	
VSS flux out of dig.	4,212.91	kg/d
VSS destruction rate	2,528	kg/d

Qgas	2,528	cu m/d
E dig gas	22,000	J/cu m
Power from gas	55,610,410	J/d
	15,447	Kwh/d
Engine eff	30%	
New Digester Power	4,634	Kwh/d



The Social Cost of Carbon

Social Cost of CO₂, 2015-2050 ^a (in 2007 dollars per metric ton CO₂)

<https://www.epa.gov/climatechange/social-cost-carbon>

Year	Discount Rate and Statistic			
	5% Average	3% Average	2.5% Average	High Impact (95th pct at 3%)
2015	\$11	\$36	\$56	\$105
2020	\$12	\$42	\$62	\$123
2025	\$14	\$46	\$68	\$138
2030	\$16	\$50	\$73	\$152
2035	\$18	\$55	\$78	\$168
2040	\$21	\$60	\$84	\$183
2045	\$23	\$64	\$89	\$197
2050	\$26	\$69	\$95	\$212

Emission Factor

7.03×10^{-4} metric tons CO₂ / kWh

(eGRID, U.S. annual non-baseload CO₂ output emission rate, year 2012 data)

= 703 g CO₂e/kWh

Using \$42/tonne CO₂e

Social cost of electricity = \$0.0295/kWh

At \$0.15/kWh → 20% of electric cost



WRRF Net Power

ENERGY BALANCE	kWh/day
COD power	54,528
Hydraulic power	(2,202)
Aeration power	(6,533)
Net digester power	4,634
NET	50,427

ELECTRICITY REQUIREMENT:		
Pumping	2,202	
Aeration	6,533	
Digester gas credit	(4,634)	
TOTAL	4,101	
COST/day (\$.15/kWhr)	\$ 615	\$ 224,526 (per year)

SOCIAL COST OF CARBON		
Cost per kWh	\$ 0.0295	
TOTAL (per day)	\$ 121	\$ 44,157 (per year)

Whitehouse Global Warming Web Site



The screenshot shows a web browser window with the URL <https://www.whitehouse.gov/omb/oira/social-cost-of-carbon>. The page features a dark blue header with the White House logo and navigation links: BRIEFING ROOM, ISSUES, THE ADMINISTRATION, PARTICIPATE, and 1600 PENN. The main content area has a background image of the Presidential Seal and two microphones. A dark blue box contains the text: "Thank you for your interest in this subject. STAY TUNED AS WE CONTINUE TO UPDATE WHITEHOUSE.GOV." Below this are three buttons: HOMEPAGE, LATEST NEWS, and OBAMA ARCHIVE. At the bottom, there are social media icons and a navigation bar with links: HOME, ISSUES, THE, PARTICIPATE, and 1600 PENN. The Windows taskbar is visible at the very bottom.



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Thank you

David A. Vaccari

dvaccari@stevens.edu

Department of Civil,
Environmental and
Ocean Engineering

