
Full Plant Deammonification for Energy Neutral Wastewater Treatment

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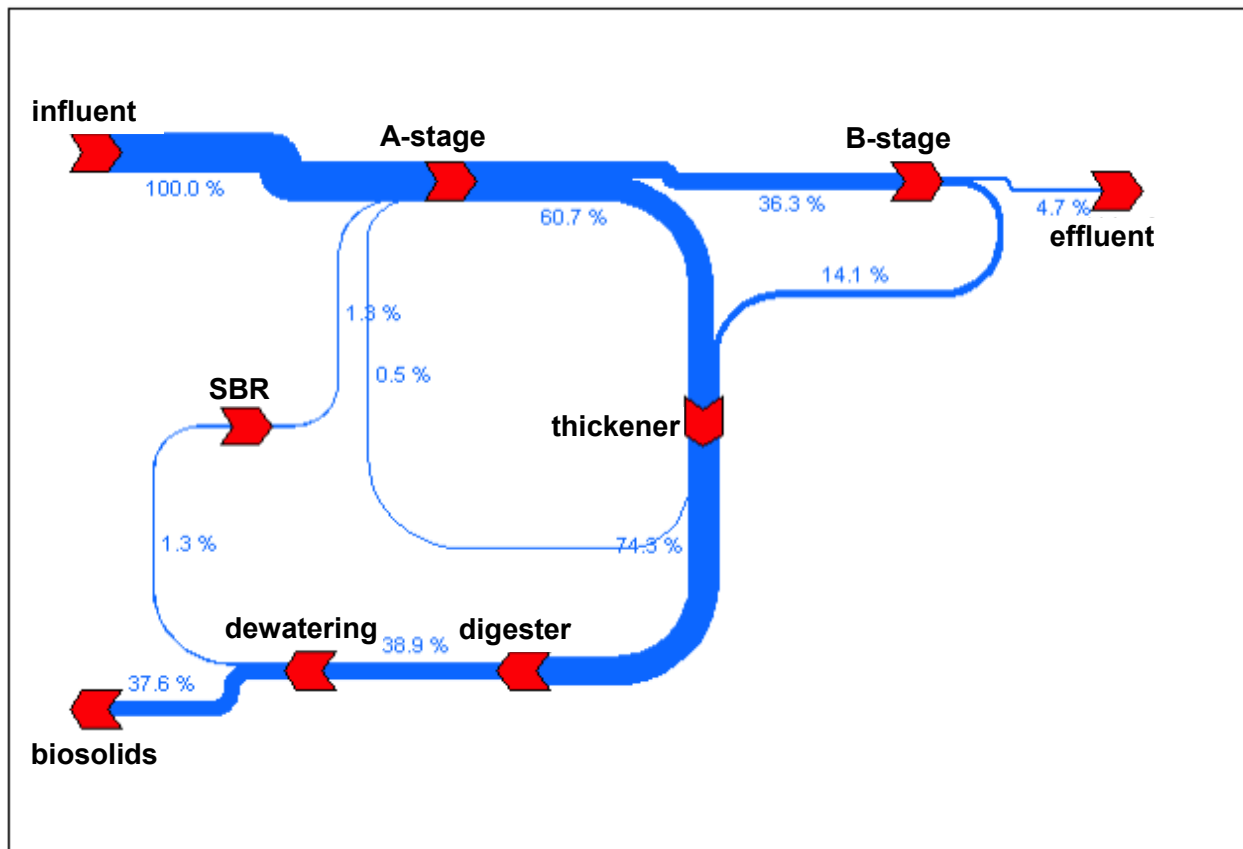
Beverley Stinson

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Claire Welling

Bernhard Wett

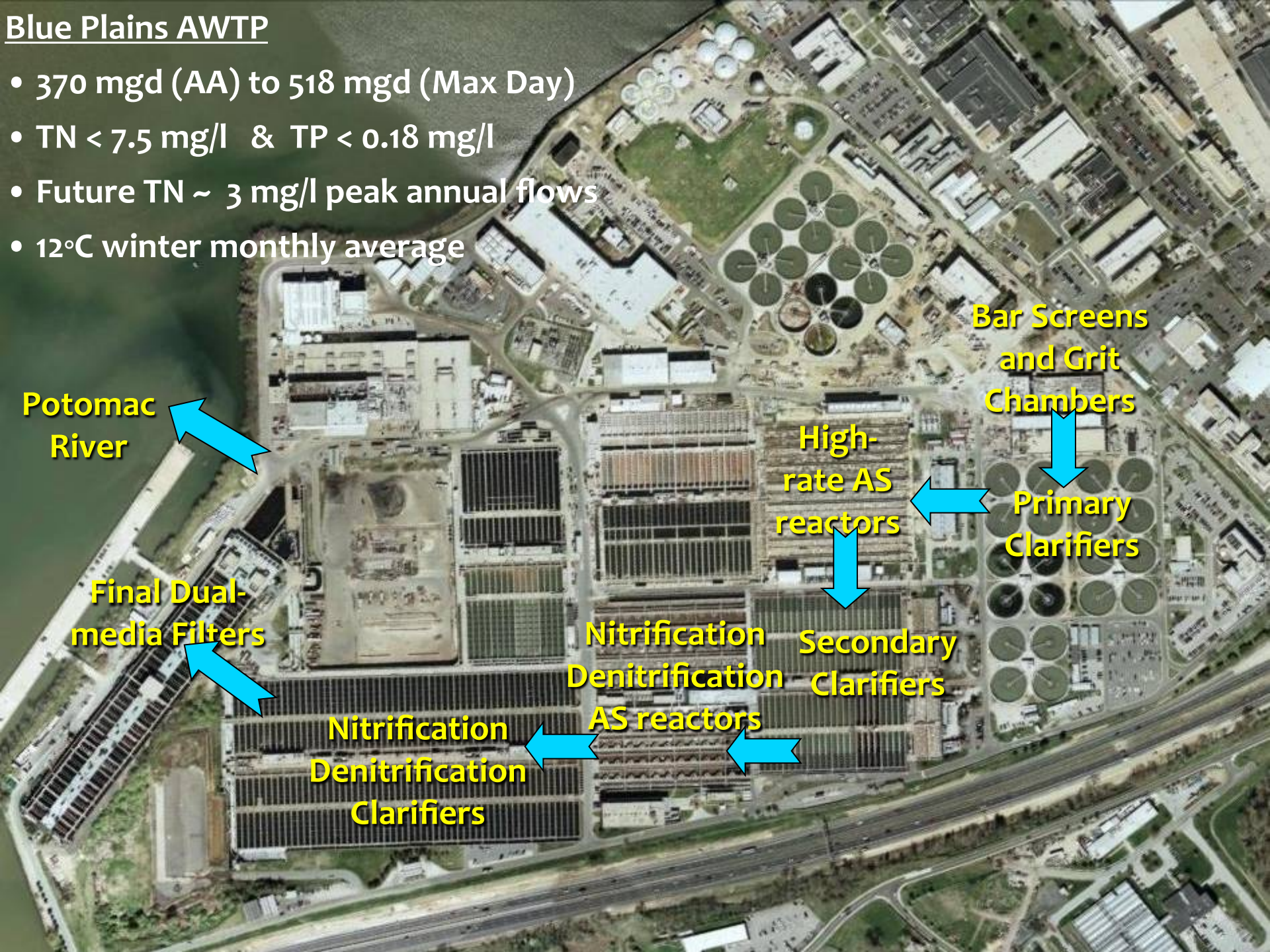
- High Rate, CEPT or A-Stage:
 - 55-75% COD removal
- B-stage: 10 - 15 days SRT
 - Deammonification



Carbon Removal

Blue Plains AWTP

- 370 mgd (AA) to 518 mgd (Max Day)
- TN < 7.5 mg/l & TP < 0.18 mg/l
- Future TN ~ 3 mg/l peak annual flows
- 12°C winter monthly average



Potomac River

Bar Screens and Grit Chambers

Primary Clarifiers

High-rate AS reactors

Secondary Clarifiers

Nitrification Denitrification AS reactors

Nitrification Denitrification Clarifiers

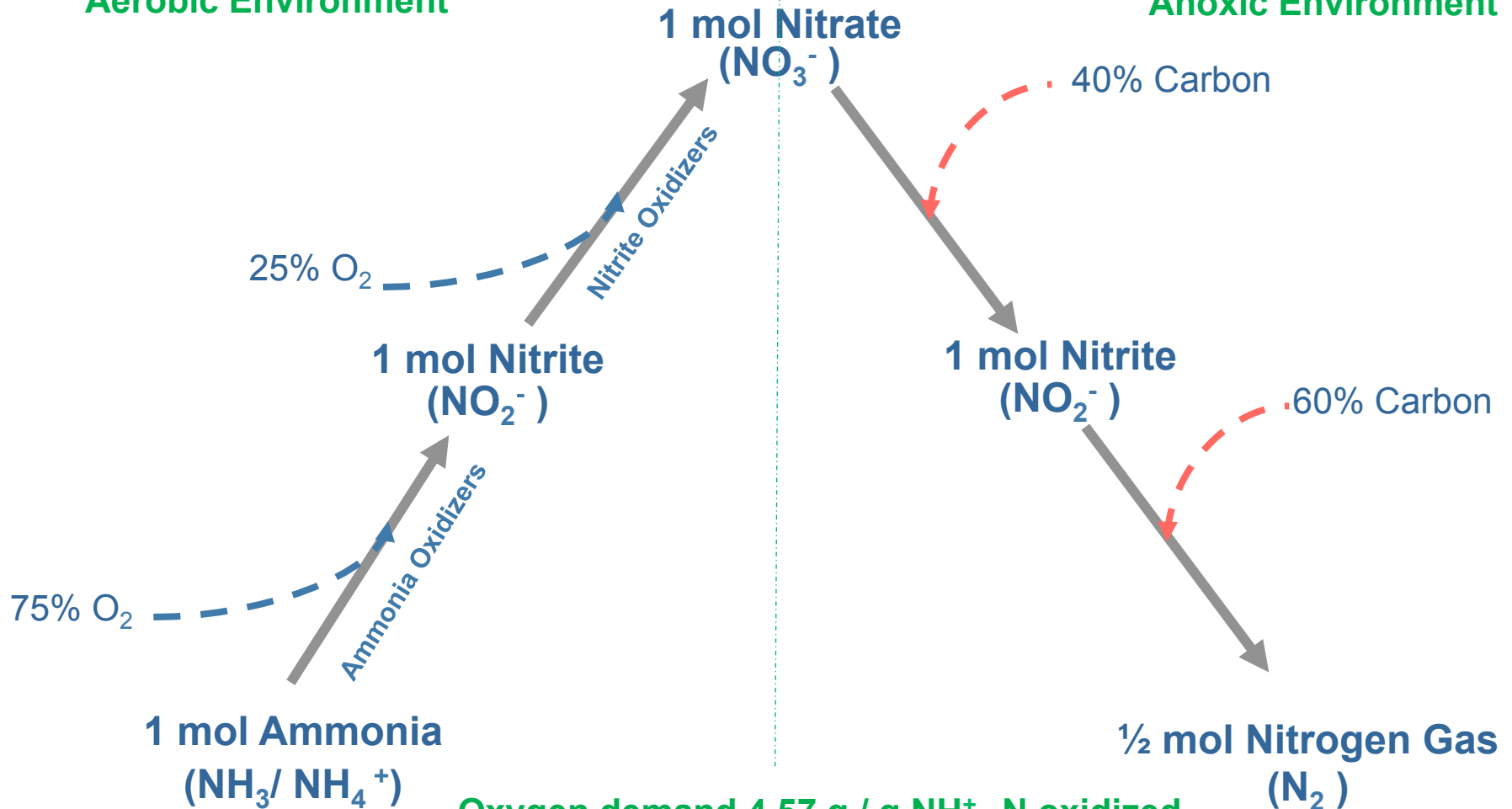
Final Dual-media Filters



Fundamentals of Nitrification - Denitrification

**Autotrophic
Aerobic Environment**

**Heterotrophic
Anoxic Environment**



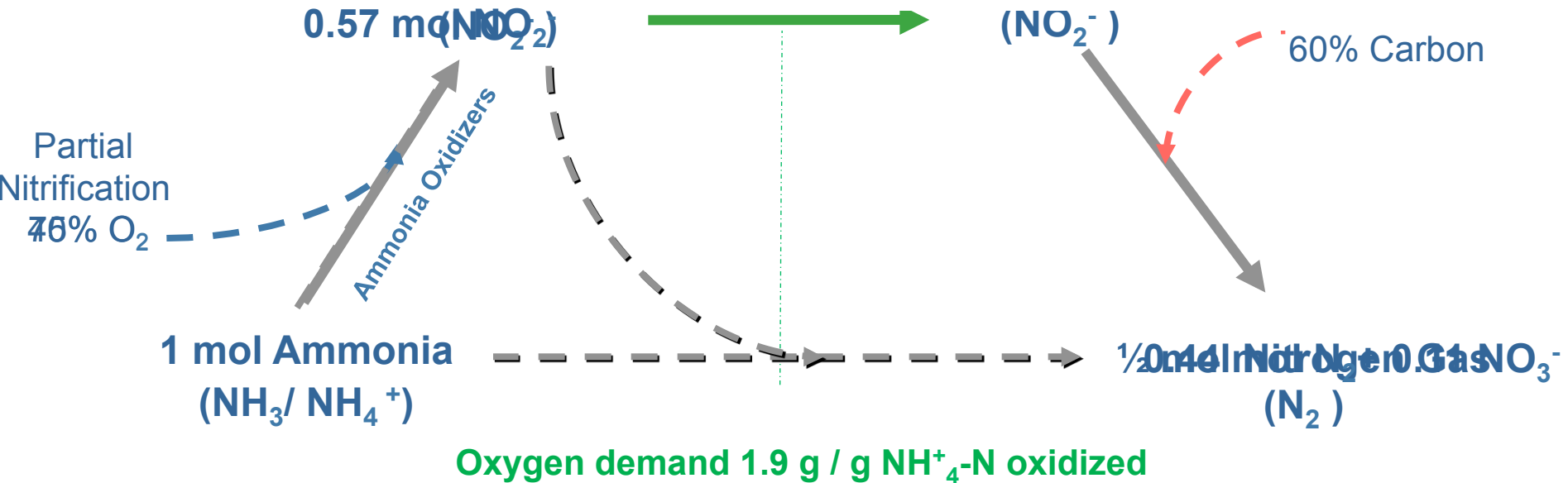
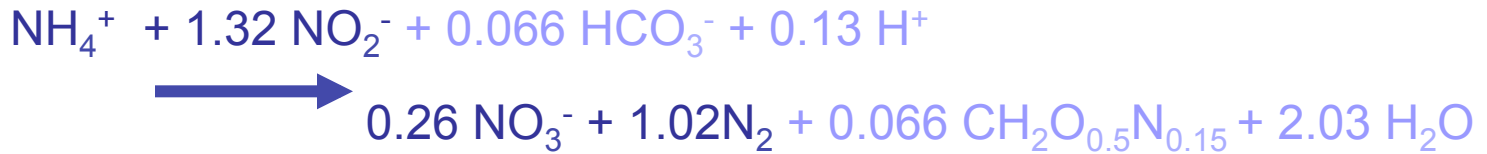
Oxygen demand 4.57 g / g $\text{NH}_4^+\text{-N}$ oxidized
Carbon demand 4.77 g COD / g $\text{NO}_3^-\text{-N}$ reduced



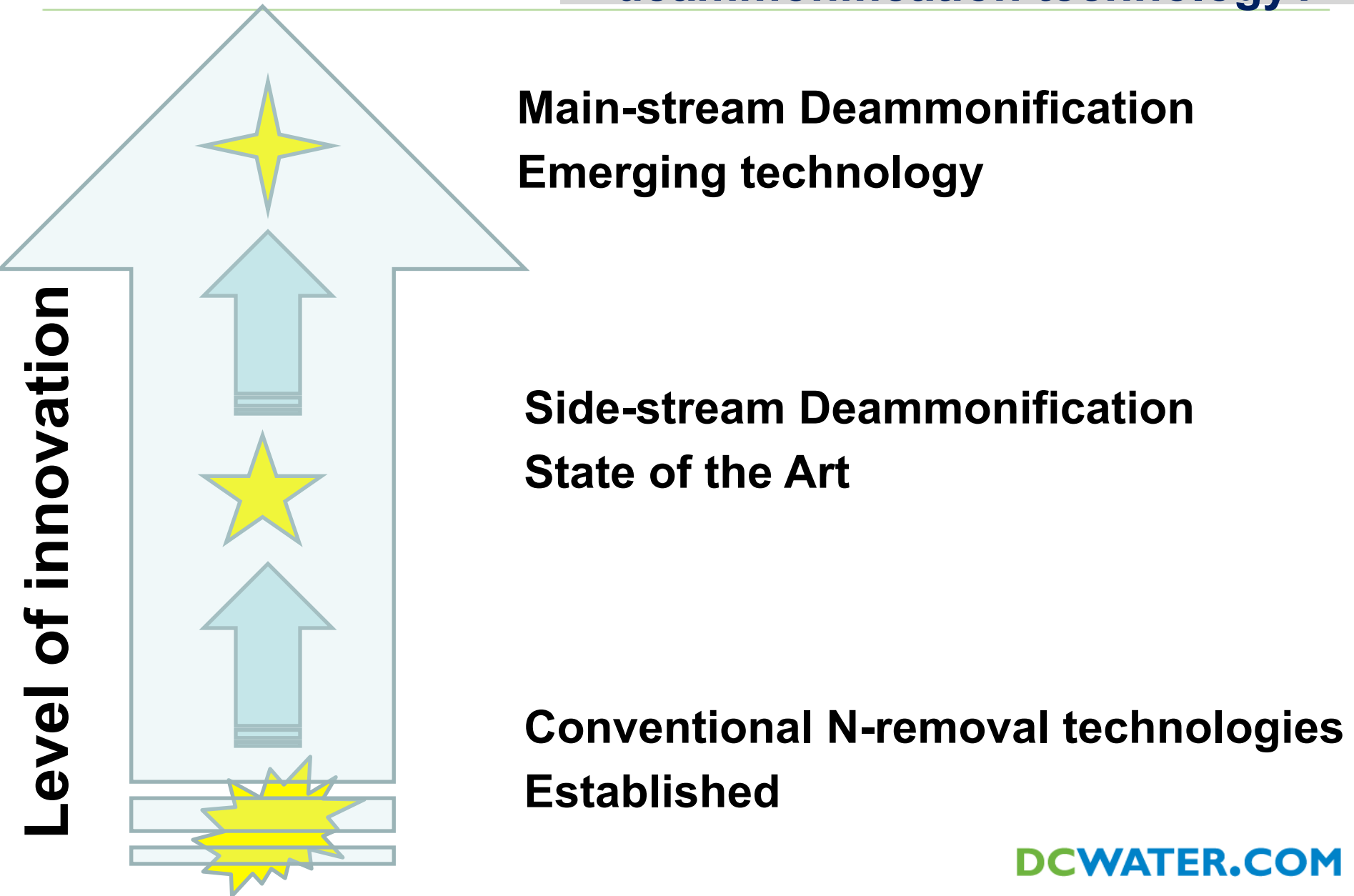
Fundamentals of Deammonification

**Autotrophic
Aerobic Environment**

ANAAMMOX
Anaerobic Ammonium Oxidation
Anoxic Environment
Autotrophic Nitrite Reduction
(New Planctomycete, Strous et. al. 1999)

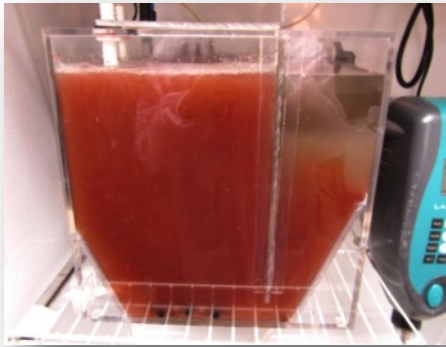


How mature is deammonification technology?



WERF-Mainstream Deammonification

3 different sites and scales



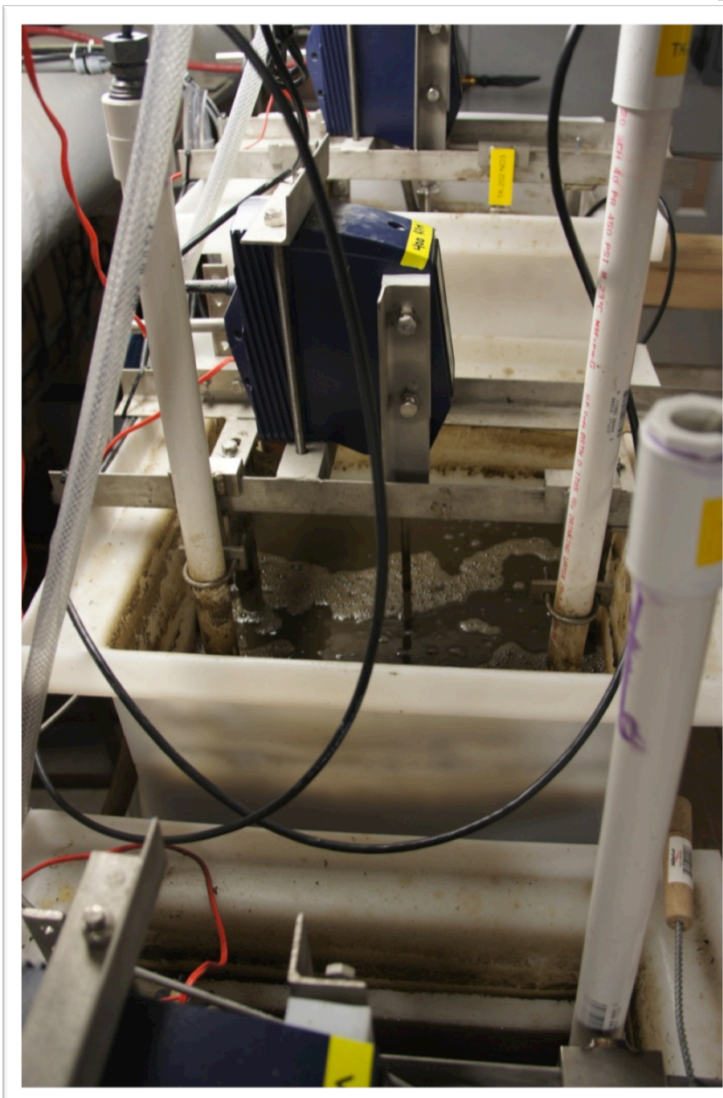
Objective of bench-scale pilot at DC Water

- Investigate fundamental process kinetics and control mechanisms identified for NOB out-selection, AOB and anammox enrichment, development and calibration of process model.



WERF-Mainstream Deammonification

3 different sites and scales



Objective of pilot-scale tests at HRSD, Virginia

- **Focus on NOB out-selection and control optimization to support design work at considered plant.**
- **Biofilm Post-Anoxic Anammox**

WERF-Mainstream Deammonification

3 different sites and scales



Objective of full-scale pilot at WWTP Strass

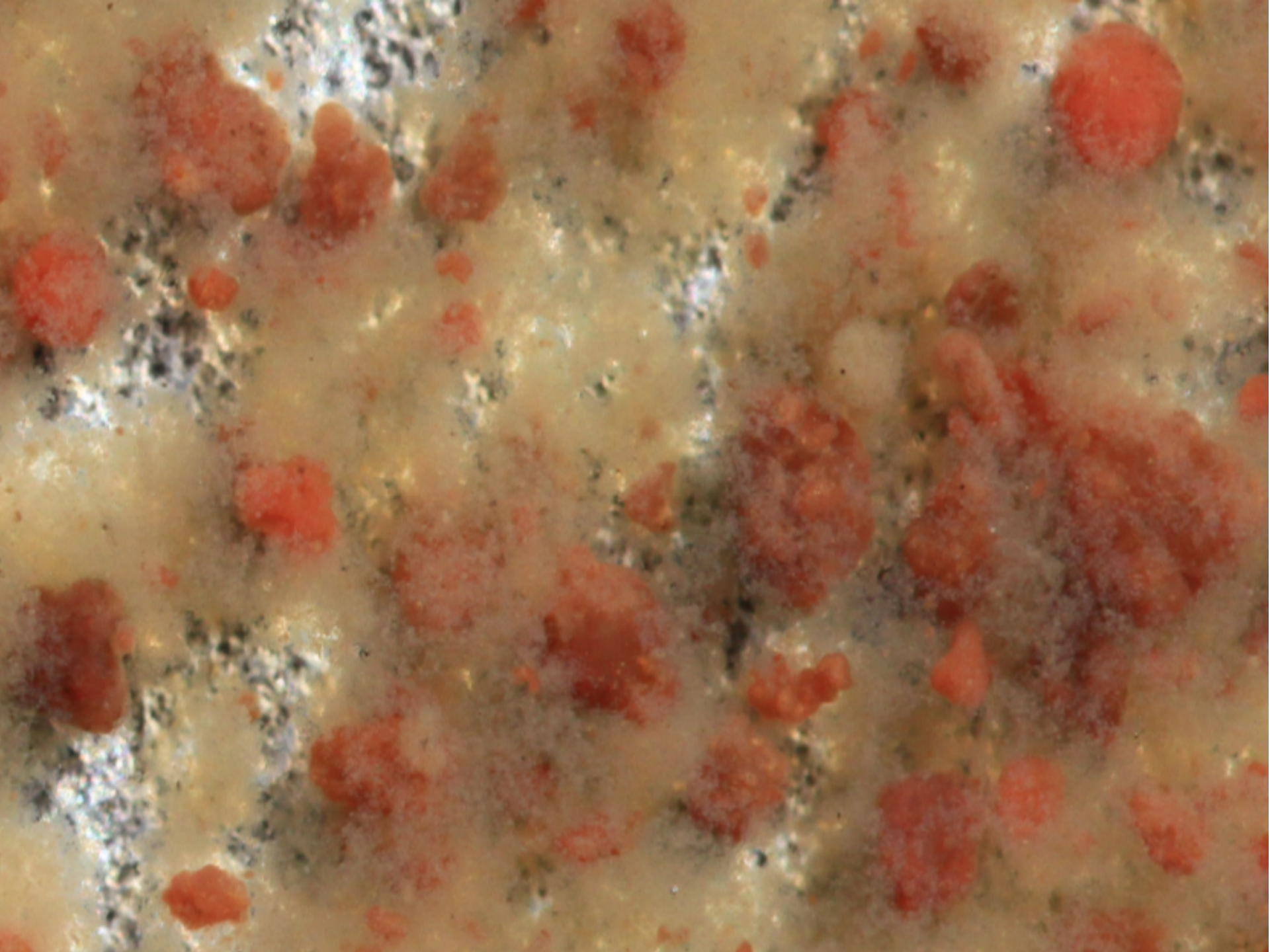
- **Demonstration** projects at Strass WWTP and Glarnerland WWTP is to demonstrate the feasibility of the deammonification concept, applicable control strategies.

Our Recipe

- Anammox
 - Anammox Bioaugmentation
 - Anammox Retention
- AOB
 - AOB Bioaugmentation
- NOB Out-Selection
 - Aggressive Aerobic SRT Management
 - Ammonia Residual
 - High DO
 - Intermittent Aeration
 - Rapid Transitions to Anoxia
- Effluent Polishing

Our Recipe

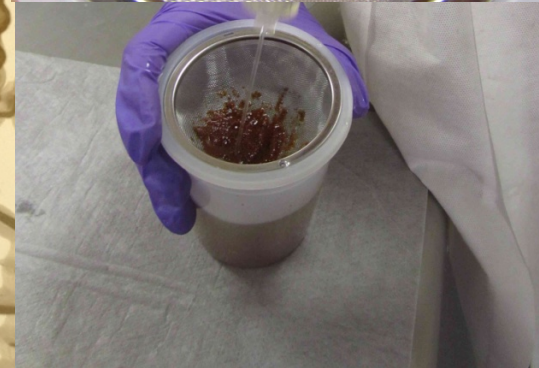
- Anammox
 - Anammox Bioaugmentation
 - Anammox Retention (long SRT maintained in granules or biofims)
- AOB
 - AOB Bioaugmentation



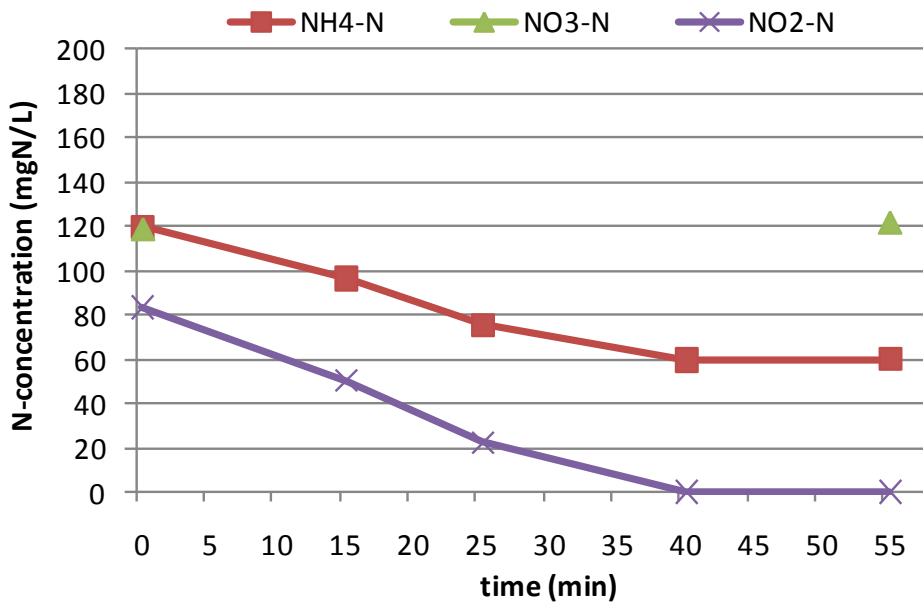
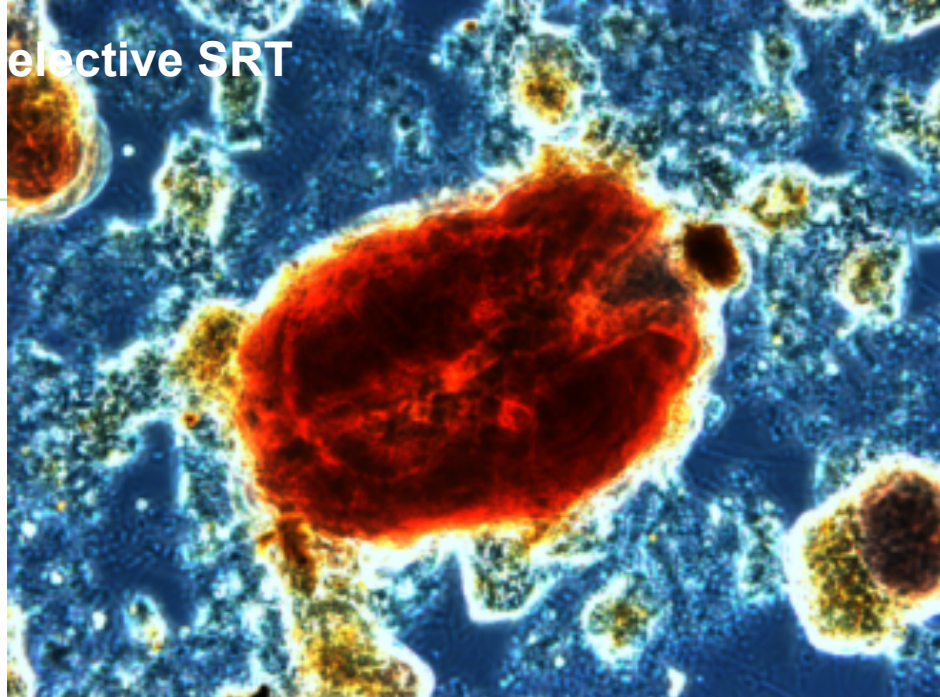
Cyclone, Sieve or Biofilm Media?

Three anammox retention procedures

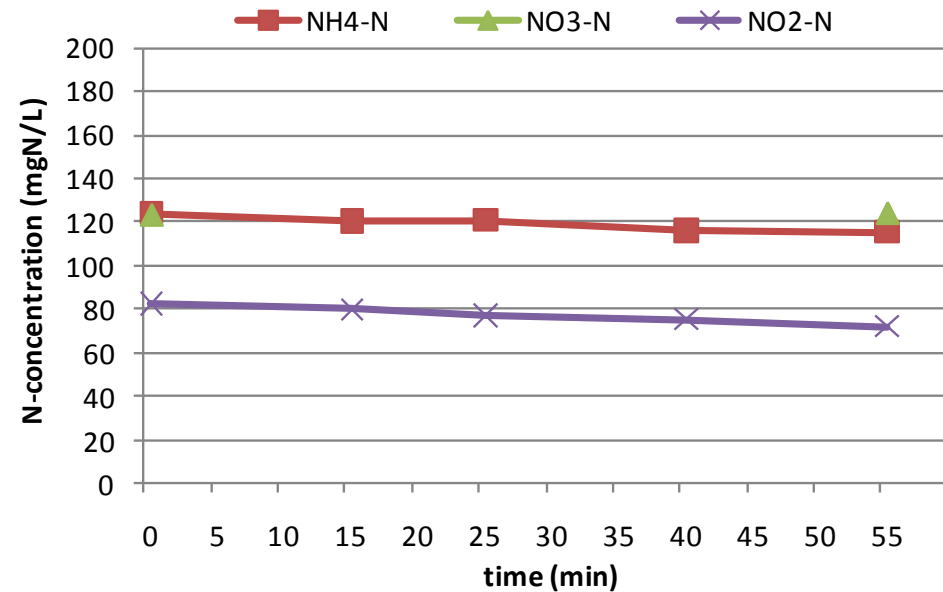
- 1) Cyclones- Strass
- 2) Sieves- Blue Plains
- 3) Biofilm Media- HRSD



selective SRT



cyclone under-flow (recycled)

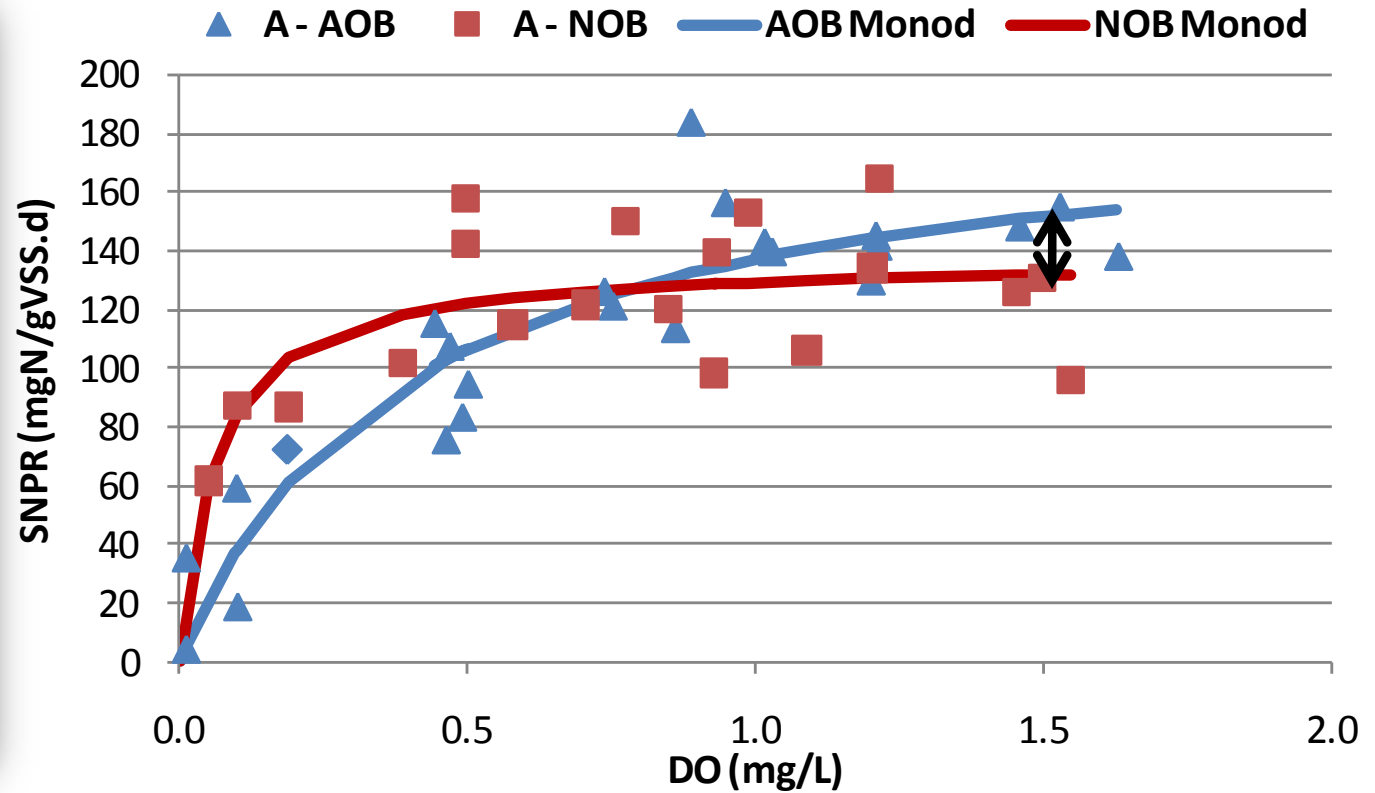


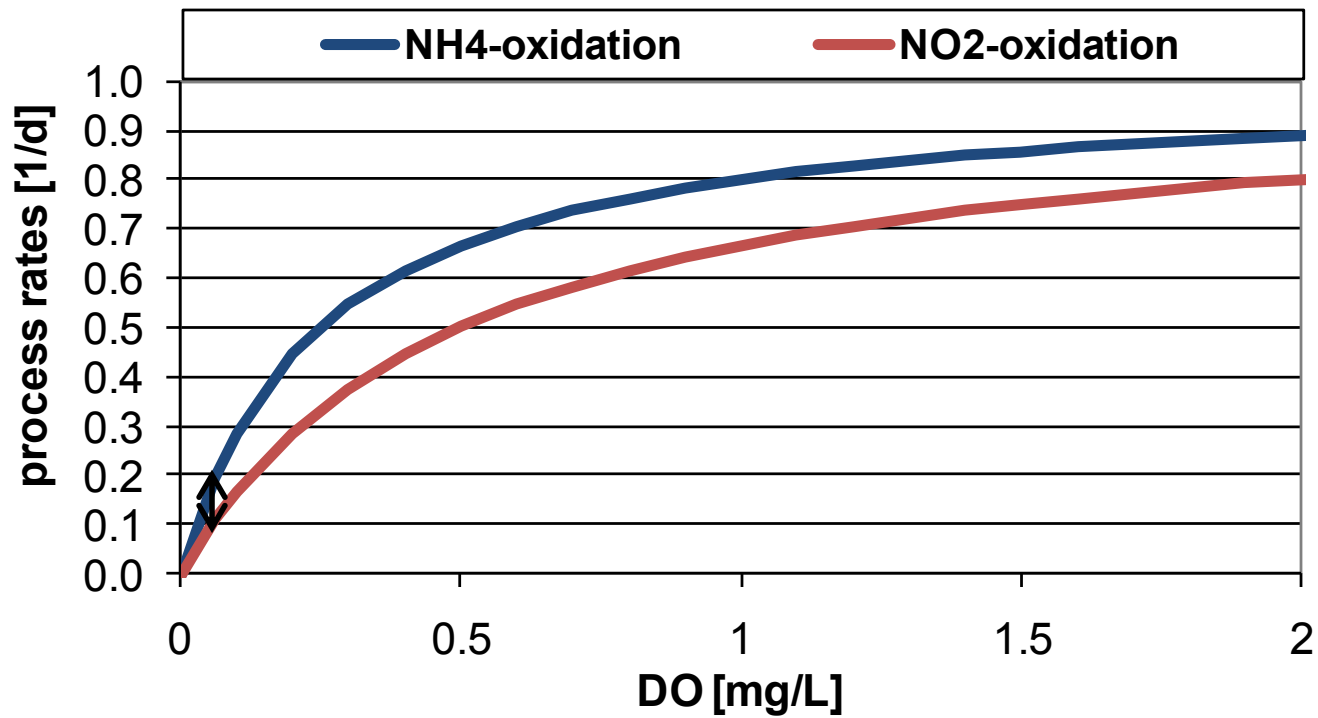
and overflow (wasted)

Our Recipe

- NOB Out-Selection
 - Aggressive Aerobic SRT Management
 - Ammonia Residual
 - High DO
 - Intermittent Aeration
 - Rapid Transitions to Anoxia
- Effluent Polishing

Oxygen Affinity



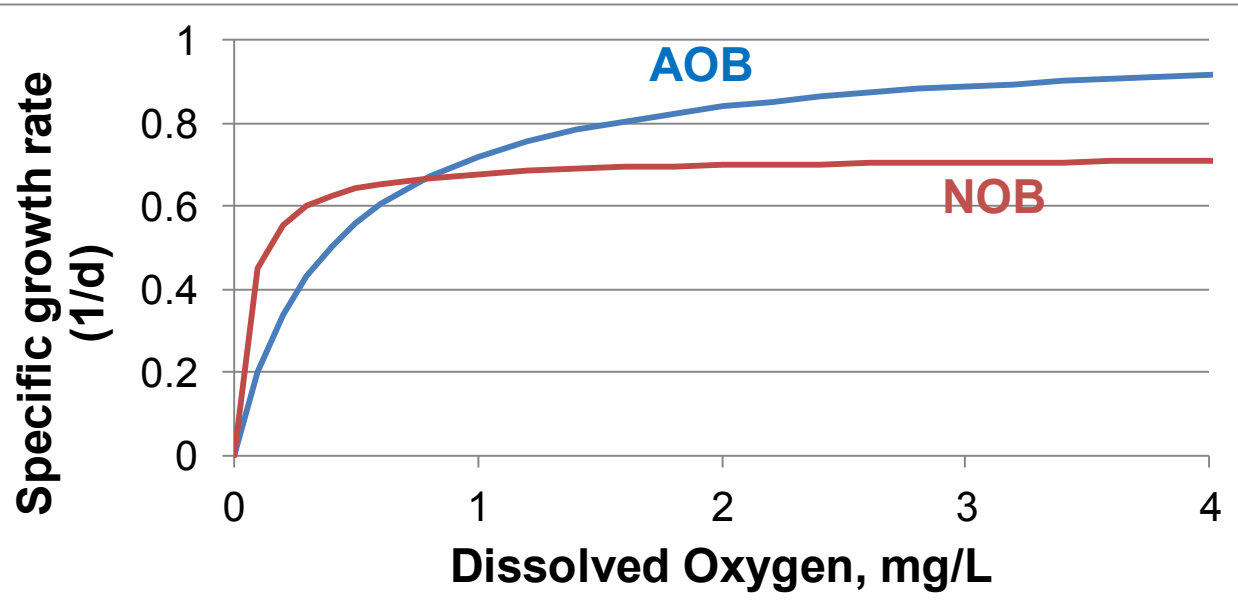


	AOB-growth Monod	NOB-growth Monod
μ_{\max} [1/d]	0.9	0.7
Arrhenius	1.07	1.06
k_O [mg DO/L]	0.25	0.50

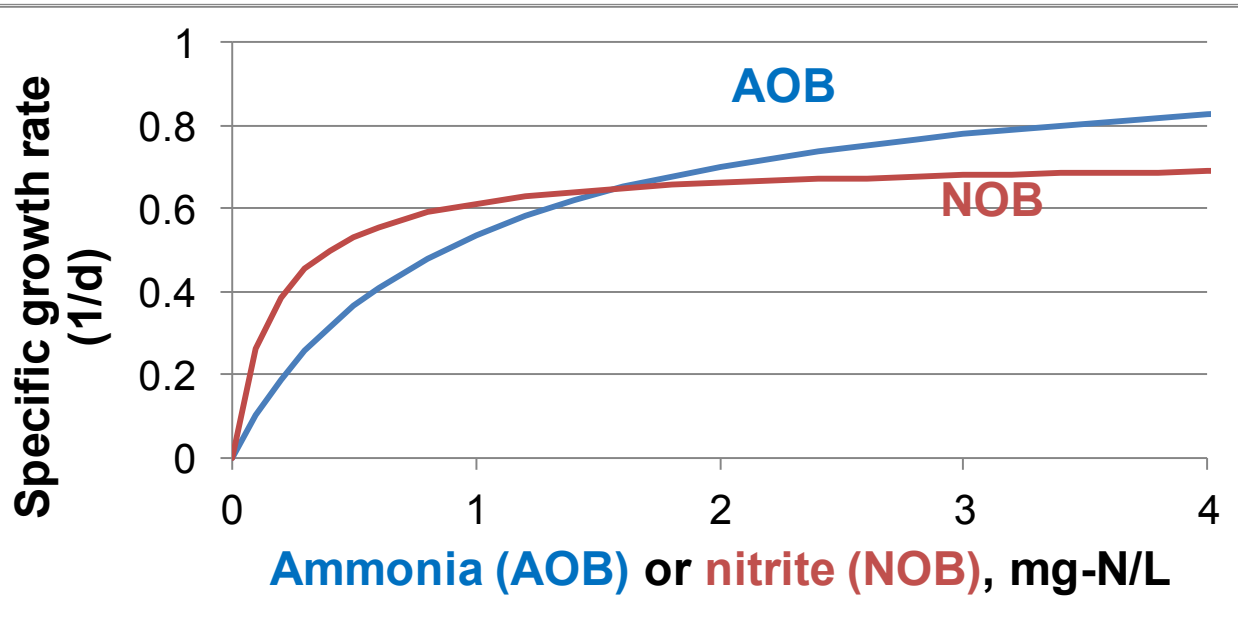
Frequently used parameter set for maximum AOB- and NOB-growth rates and oxygen affinity (K_O)

Oxygen and Nitrogen Affinities

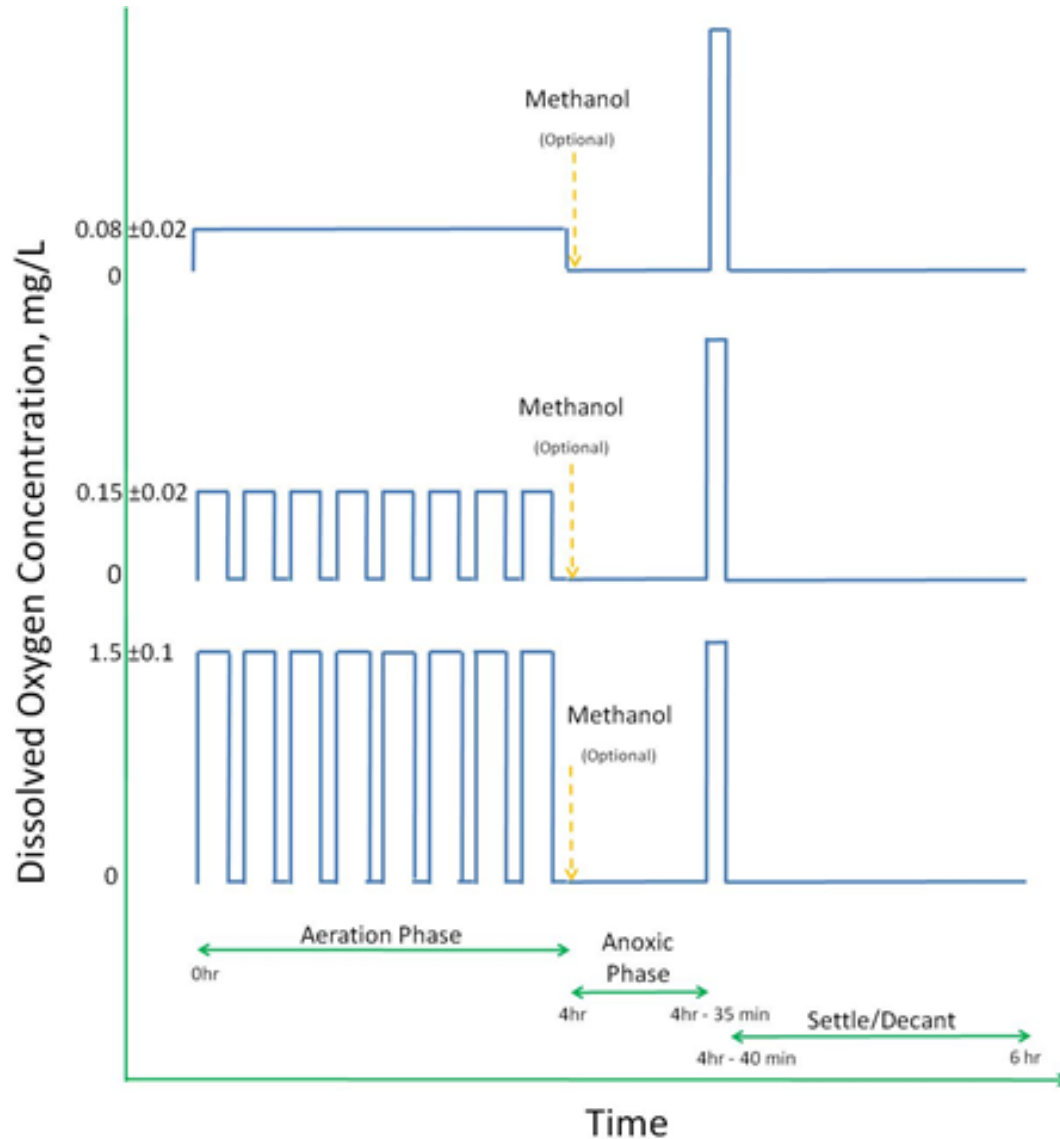
From:
Current WERF Study



Extracted From:
Chandran and Smets (2005)
Water Research, **39**, 4969



DC Water Trials

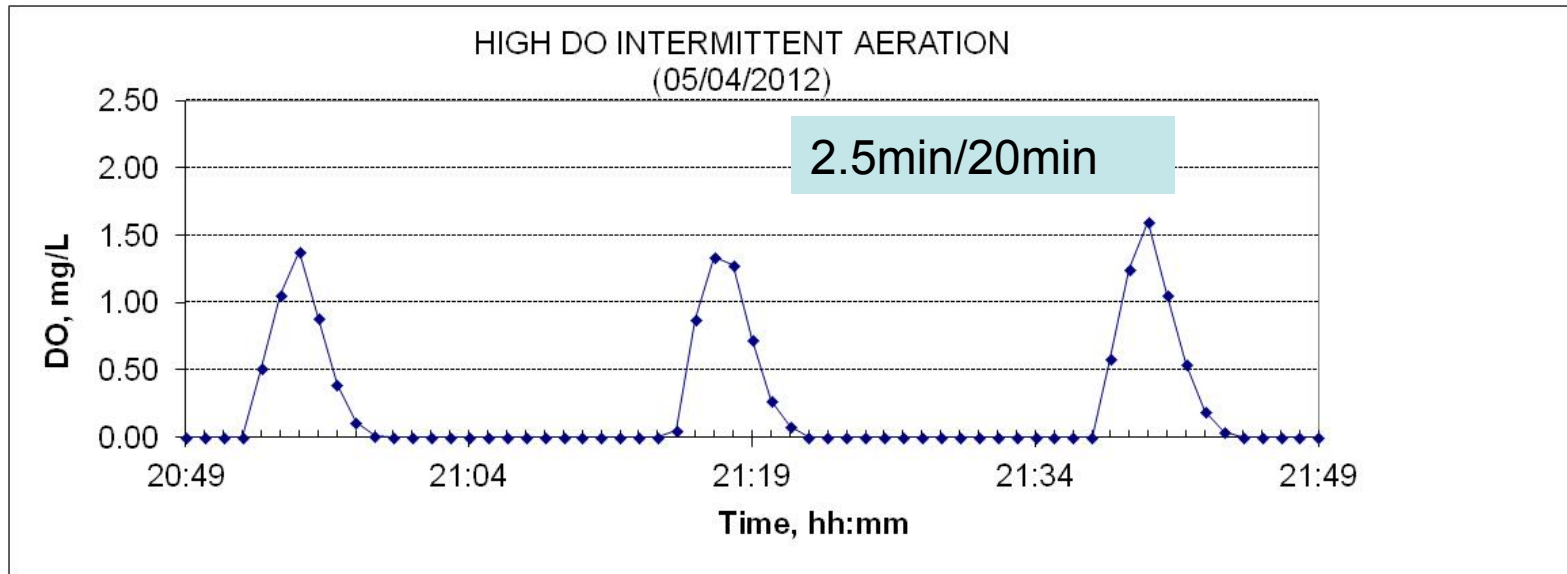


Low/Constant DO

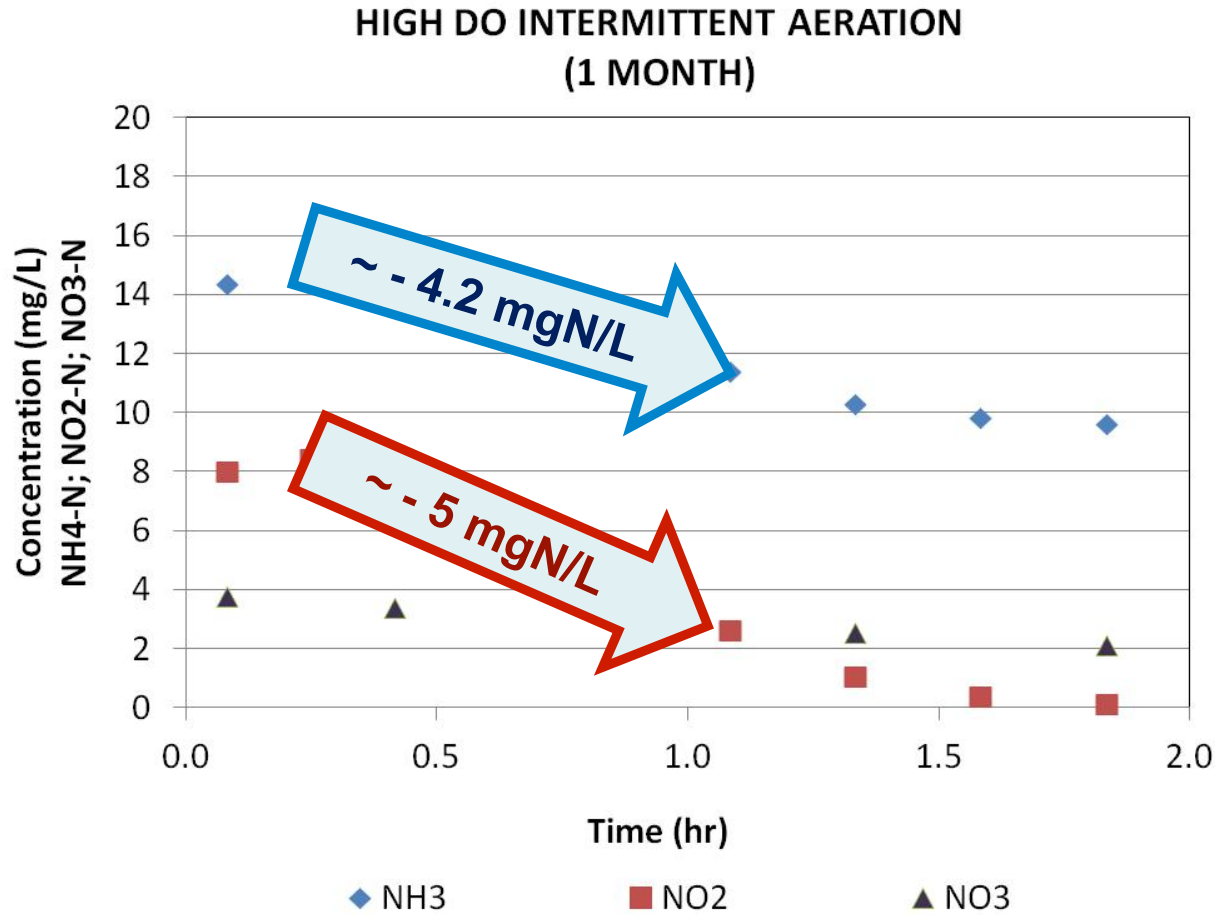
Low/Intermittent aeration

High/Intermittent aeration

Dissolved Oxygen Slope and Profiles

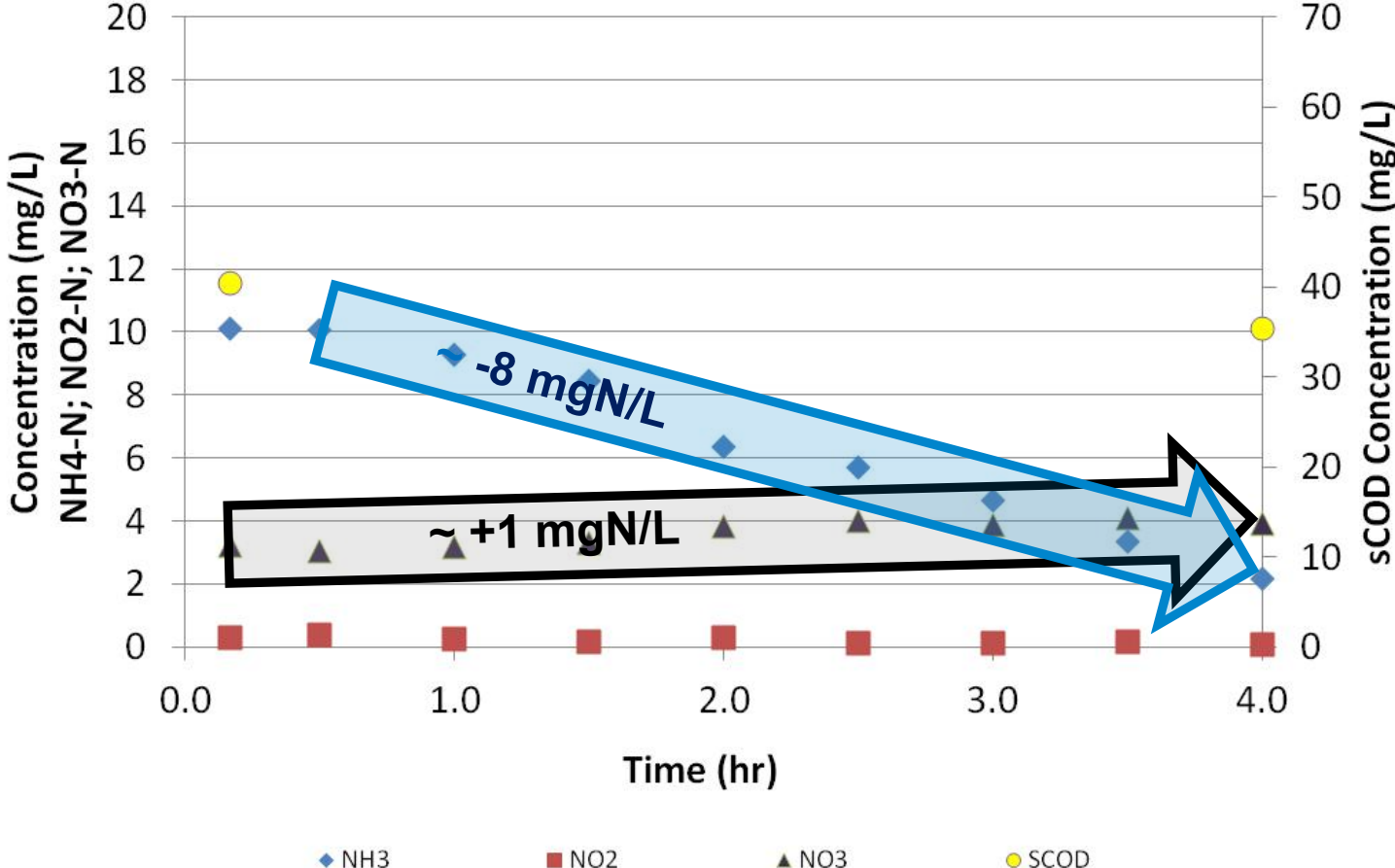


HIGH DO Intermittent Air – “Anammox Activity”

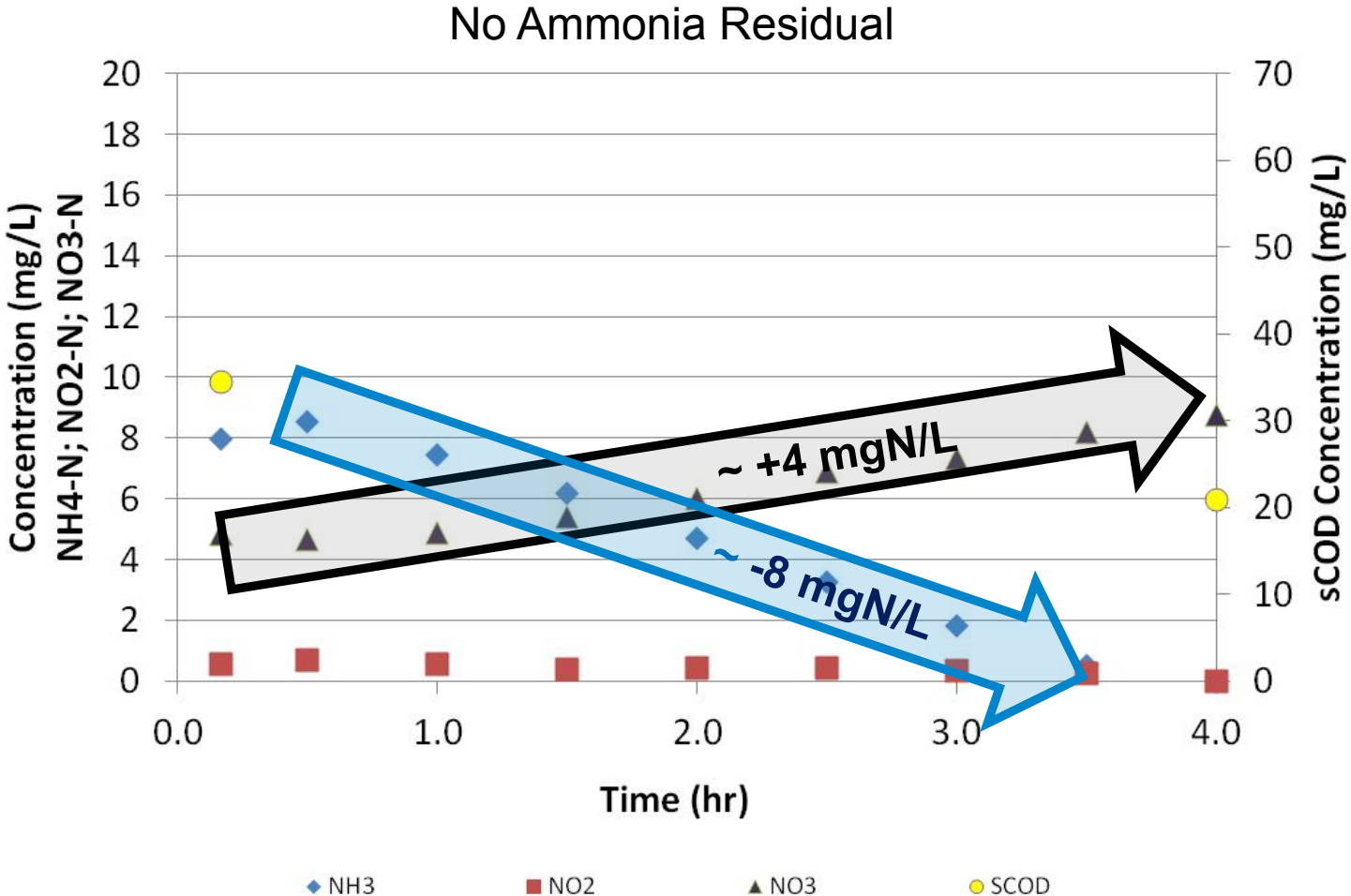


HIGH DO Intermittent Air – “N Profiles”

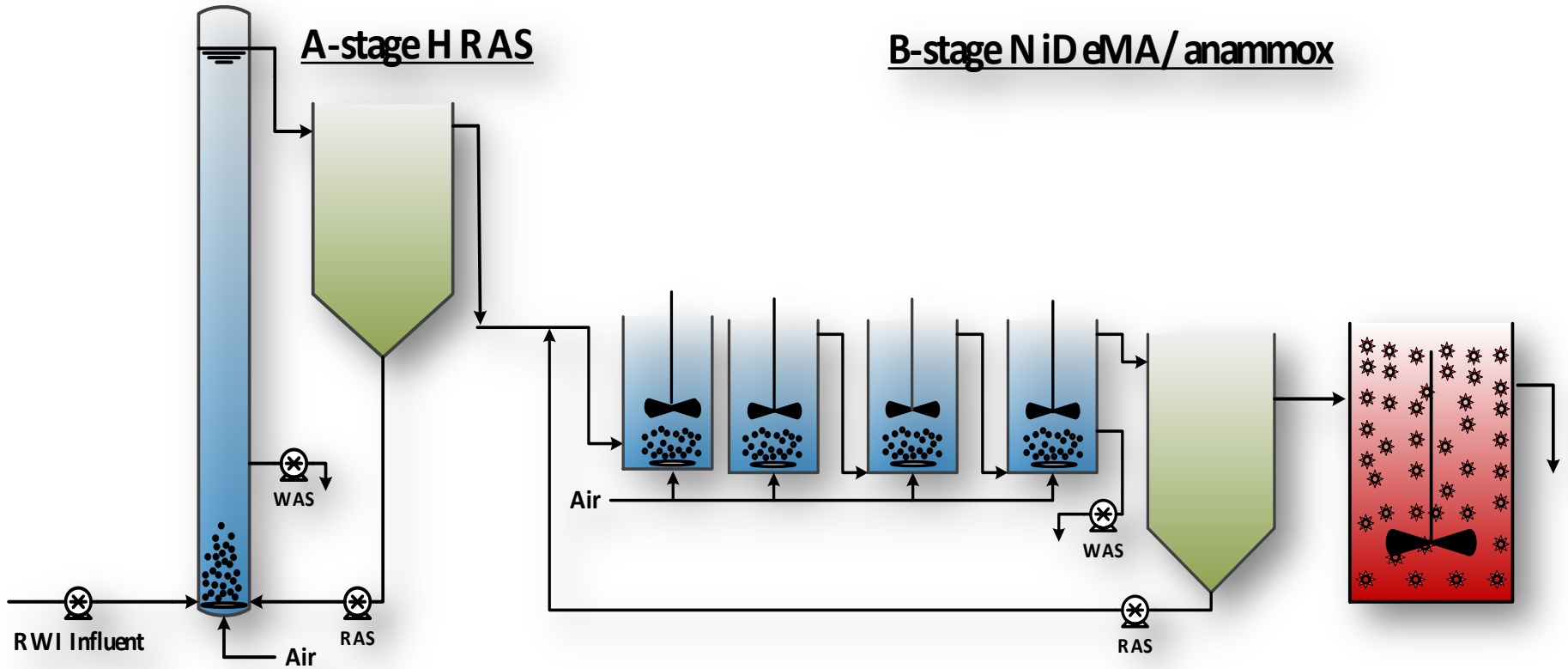
2 mg/L Ammonia Residual



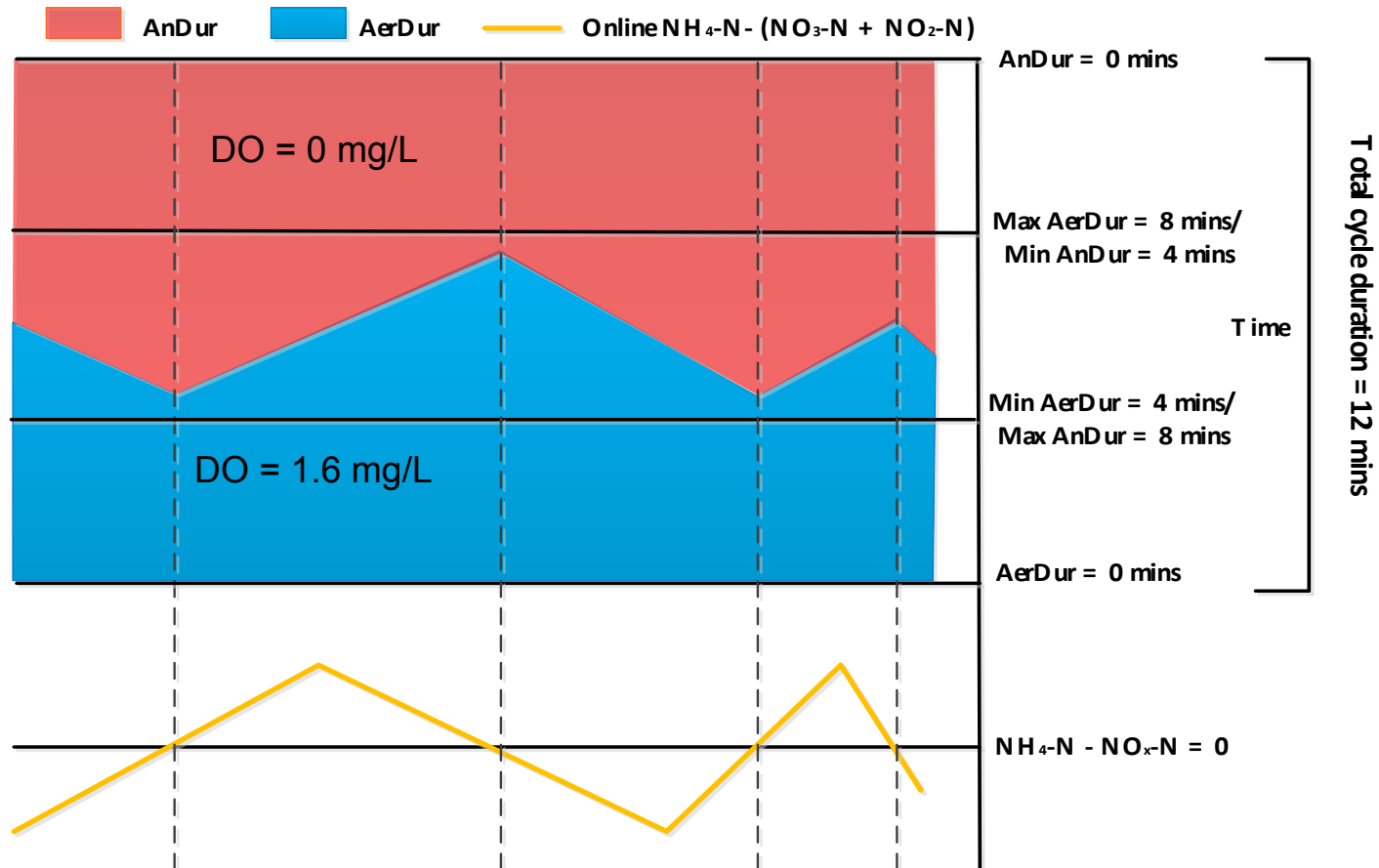
HIGH DO Intermittent Air – “N Profiles”



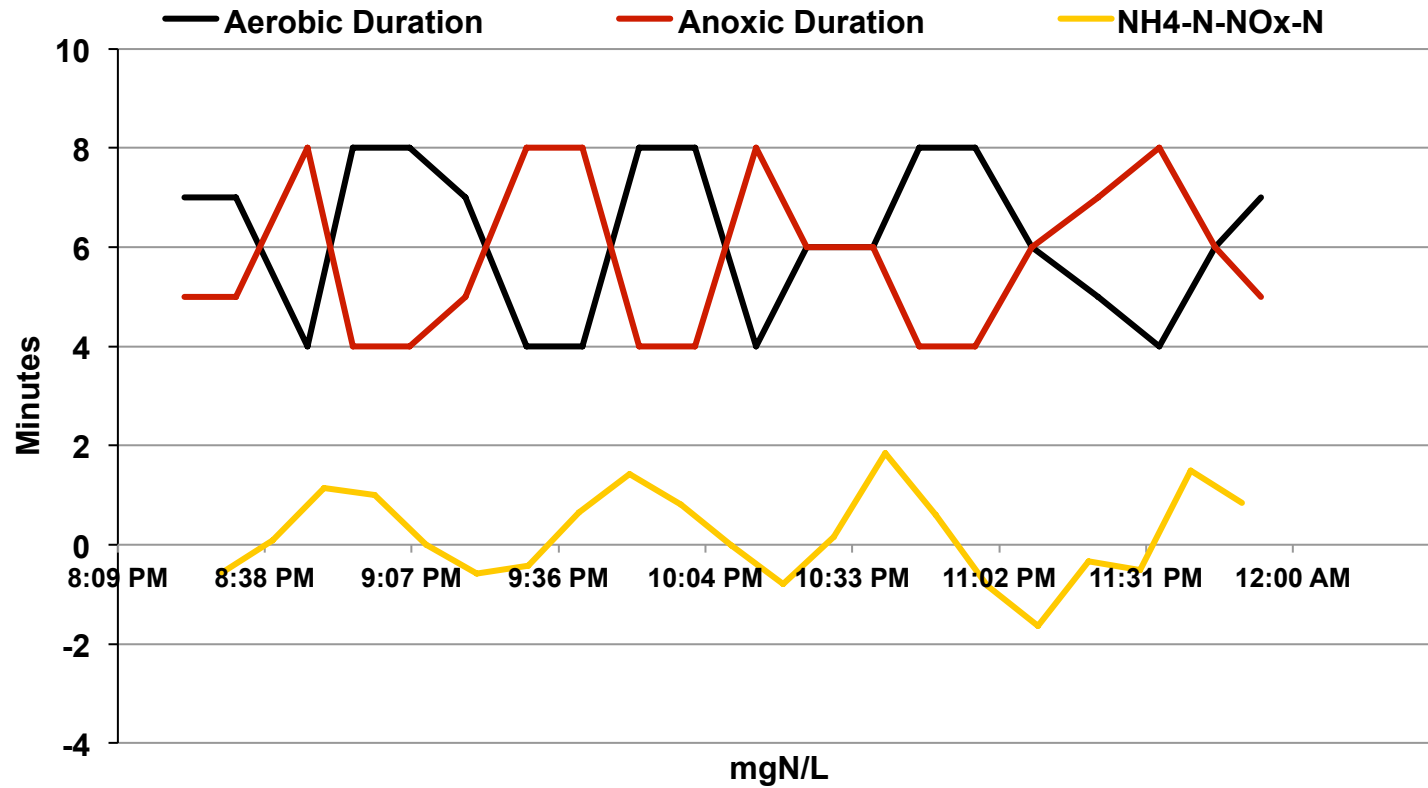
HRSD Process Schematic



Ammonia vs NOx (AVN) Controller



AVN control

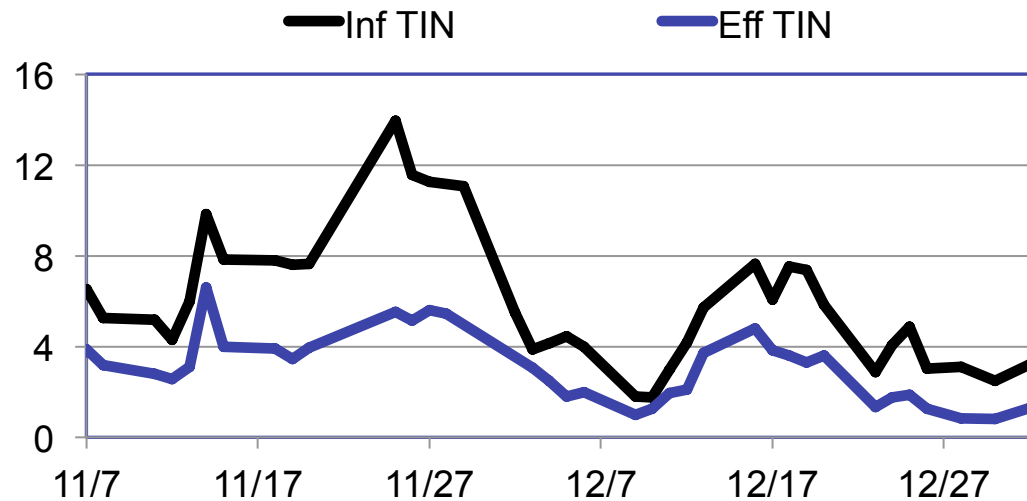
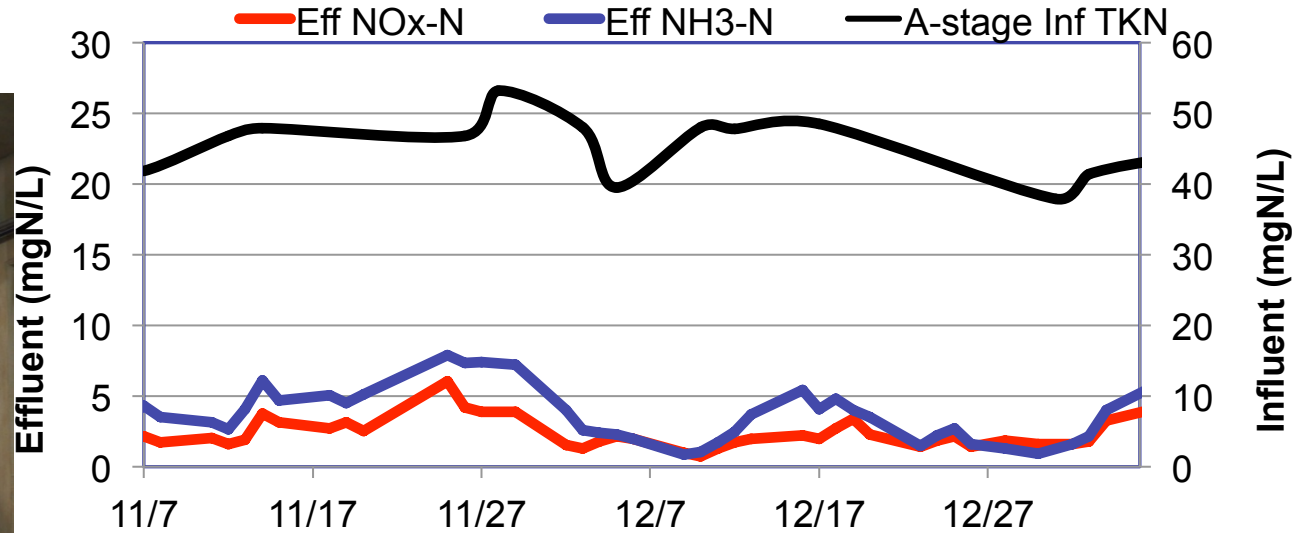


Process Performance

Nitrification/ Denitritation

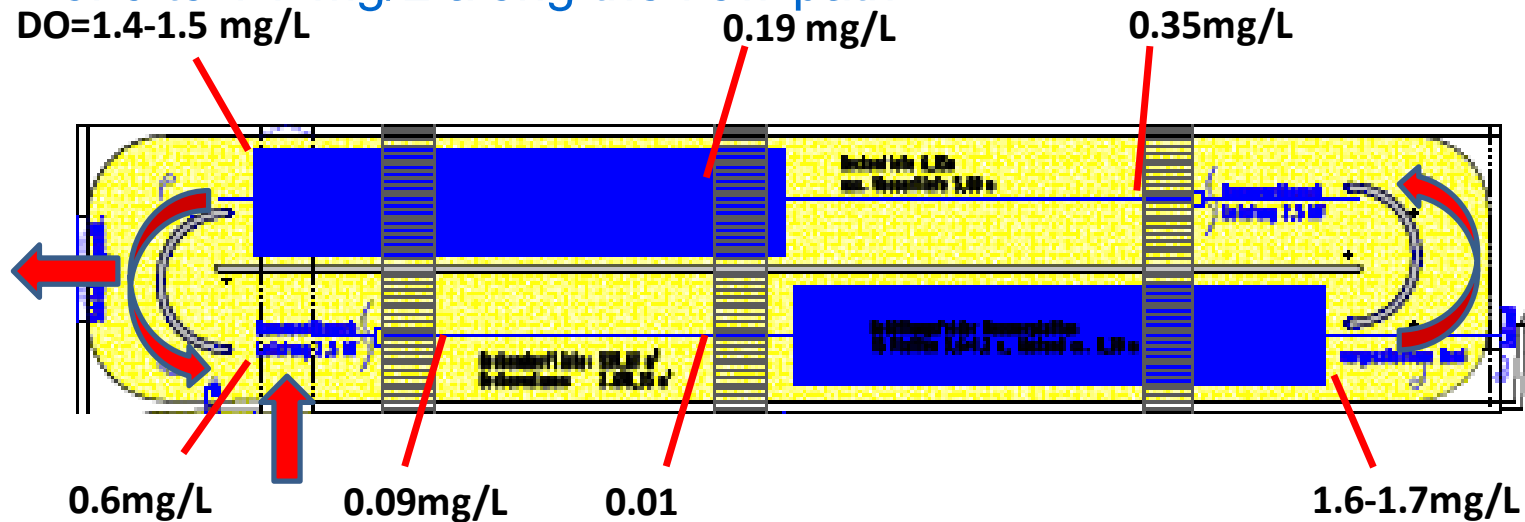


Post-Anoxic Anammox MBBR



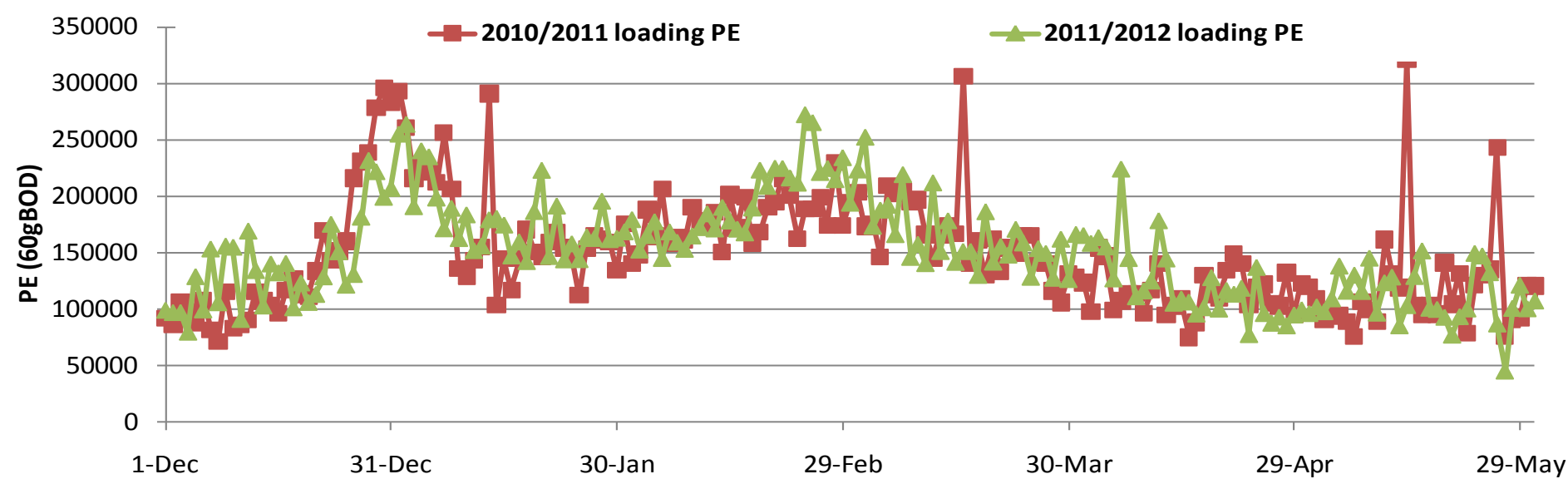
Strass Demonstration

- Carousel type aeration tank at Strass WWTP providing a DO-range of 0 to 1.7 mg/L along the flow-path.

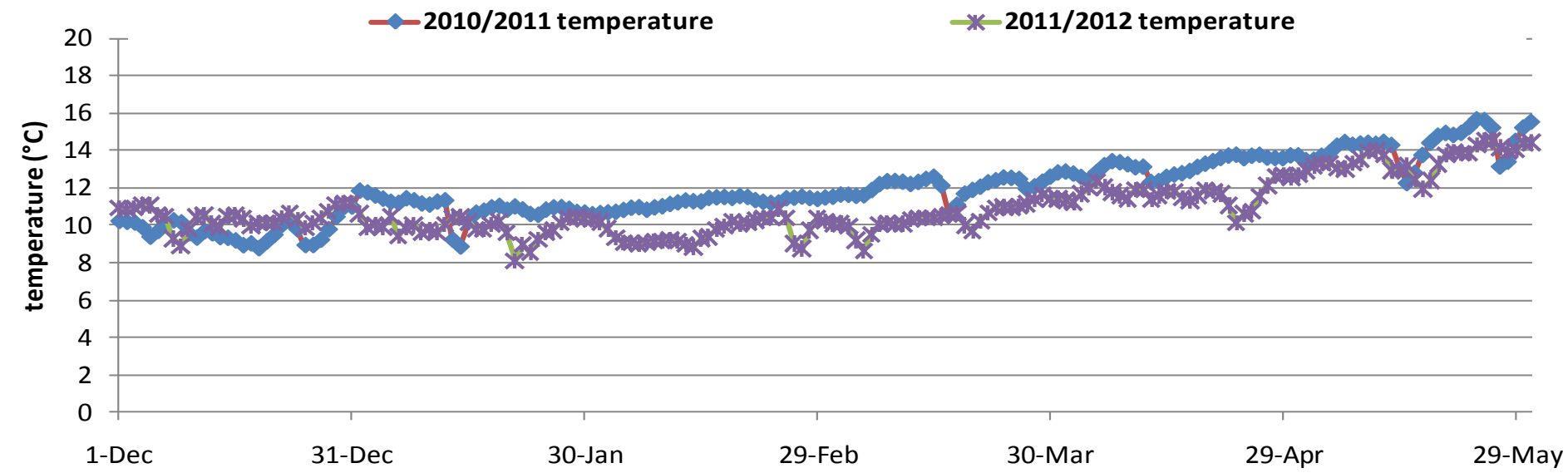


Cyclones installed at the B-stage in Strass, Cyclone A (left), Cyclone B since early September 2011 (right).



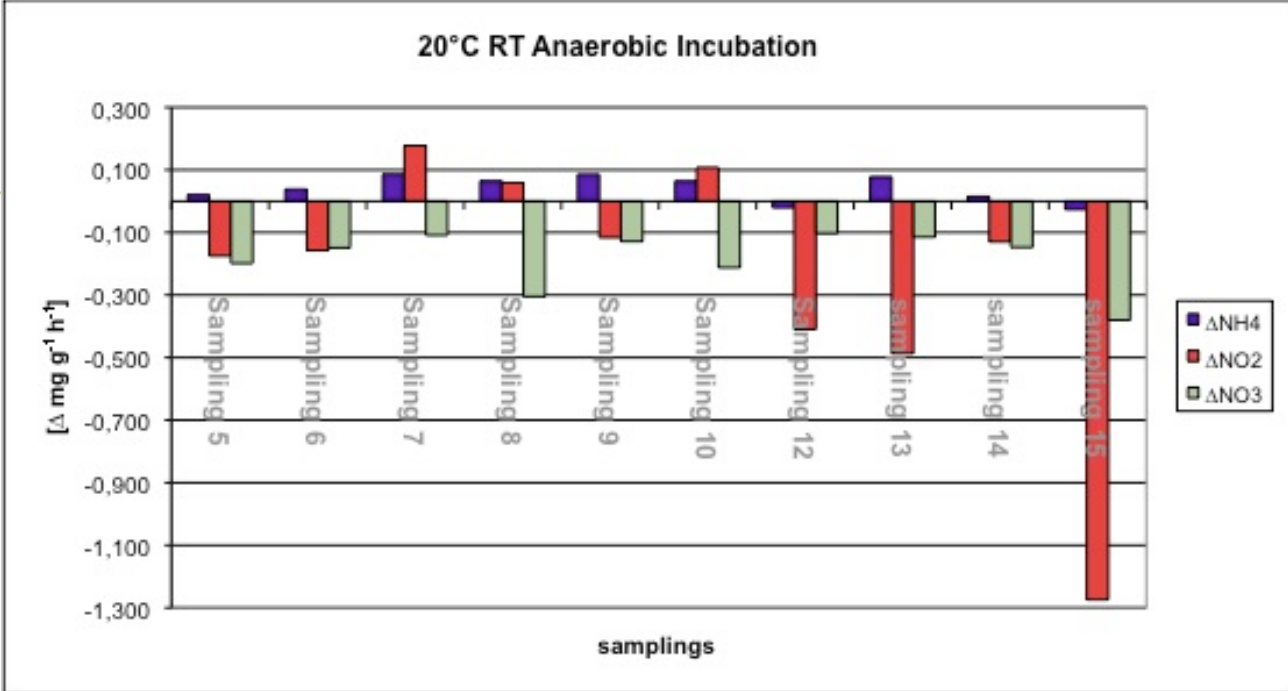


plant loading profiles (PE) before and after project start

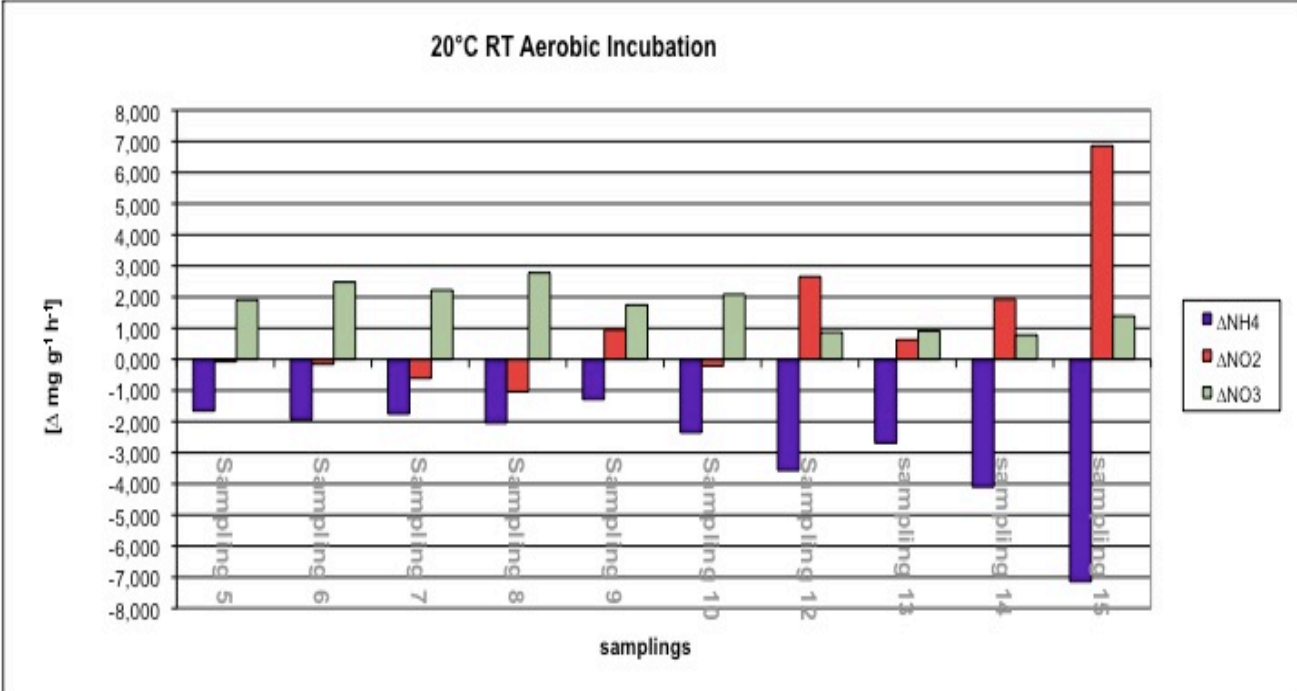


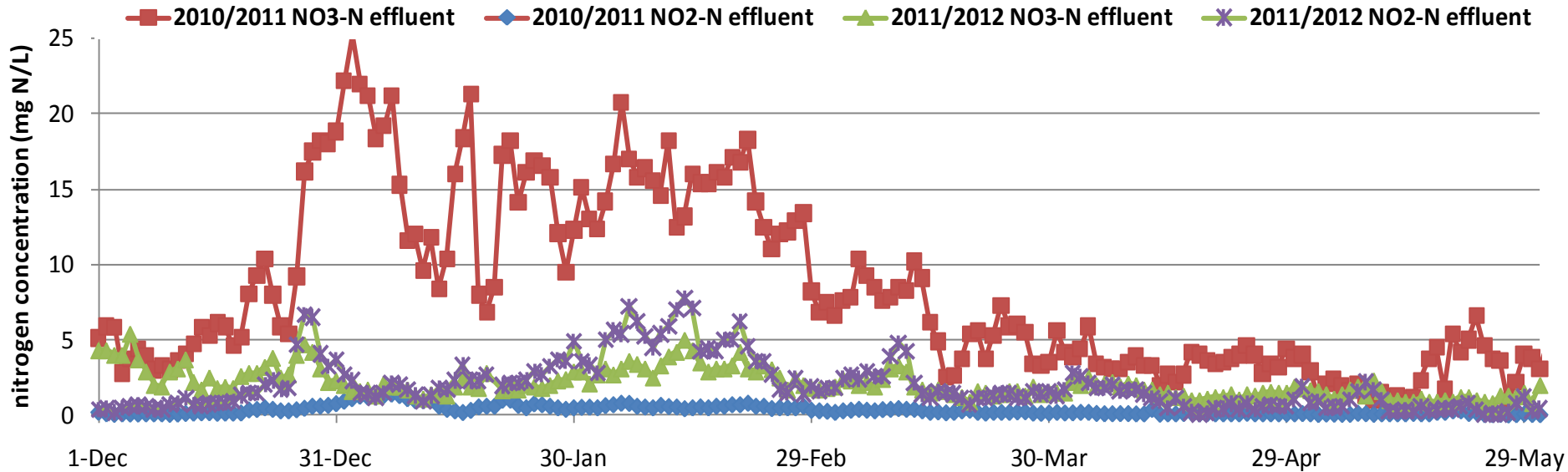
comparison of temperature profiles (°C)

The last samples show ammonia removal during anaerobic activity test (anammox activity)

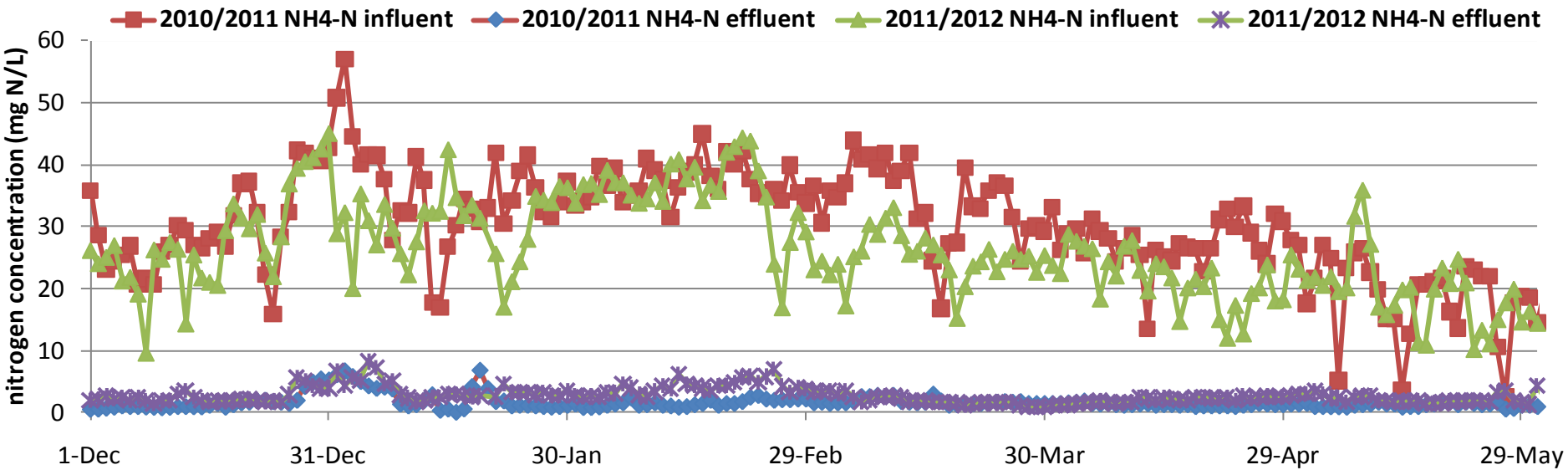


Only 25% of NOx produced from ammonia oxidation is converted to nitrate during aerobic activity test of the last sample





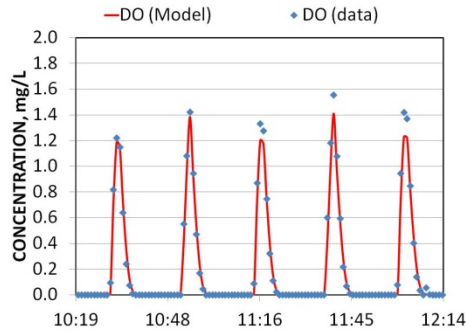
Comparison of this year's and last year's operational data of the full-scale pilot Strass indicating advanced NOB-repression (typically high nitrate level at Christmas peak-load; similar temperature conditions of ca. 10°C, load conditions and ammonia effluent concentrations of ca. 2-5 mgN/L for both years)



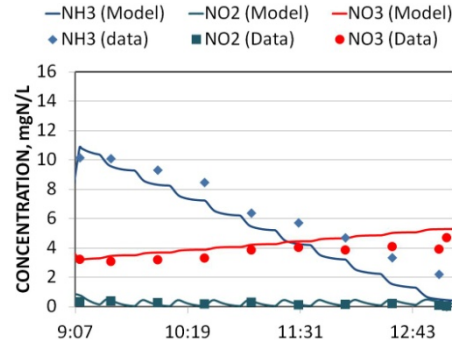
MODEL PARAMETER CALIBRATION

Simulation Results

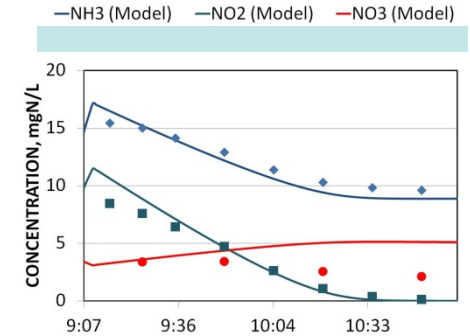
DO Profiles



N Profiles



AMX Activity



High/Intermittent
aeration

	AOB-growth	NOB-growth
	Monod	Monod
$\mu_{\max} * X_a / Y_a$	193	137
k_o [mg DO/L]	0.40	0.06

Specific nitrogen process rates for AOB and NOB yielded from constant DO-tests

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