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**LOS ANGELES COUNTY
SANITATION DISTRICTS**
Converting Waste Into Resources

Stanley Consultants

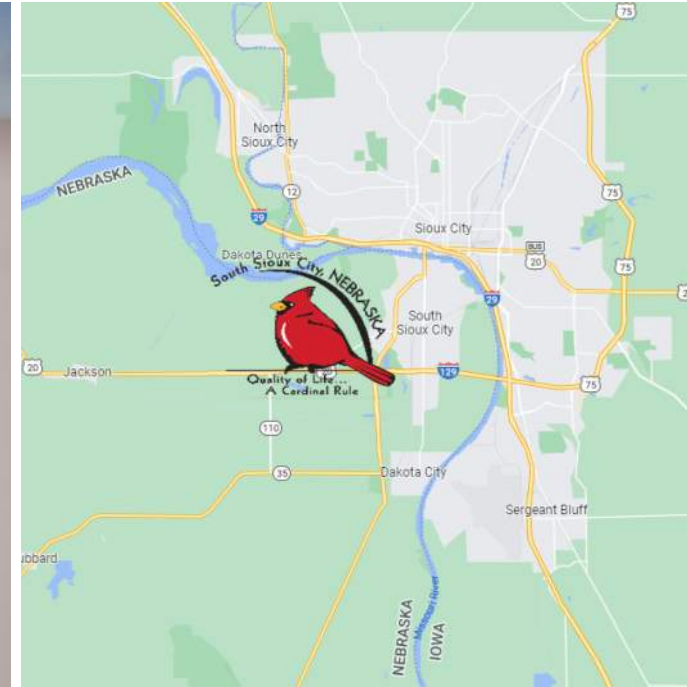
**LA
DWP** Los Angeles
Department of
Water & Power

We will begin our presentation in a few minutes...



Leadership and Excellence in Environmental Engineering and Science





South Sioux City WWTf Improvements

Dillon Devitt, PE, BCEE

NOVEMBER 13, 2024





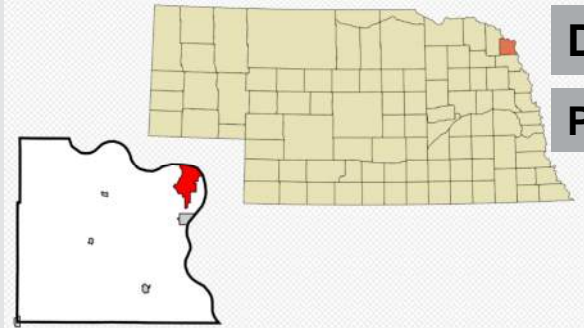
- 01** Background
- 02** Project Needs & Objectives
- 03** Feasibility Study
- 04** AGS Overview
- 05** Design
- 06** Bidding
- 07** Start up
- 08** Looking Forward



01

BACKGROUND

BACKGROUND



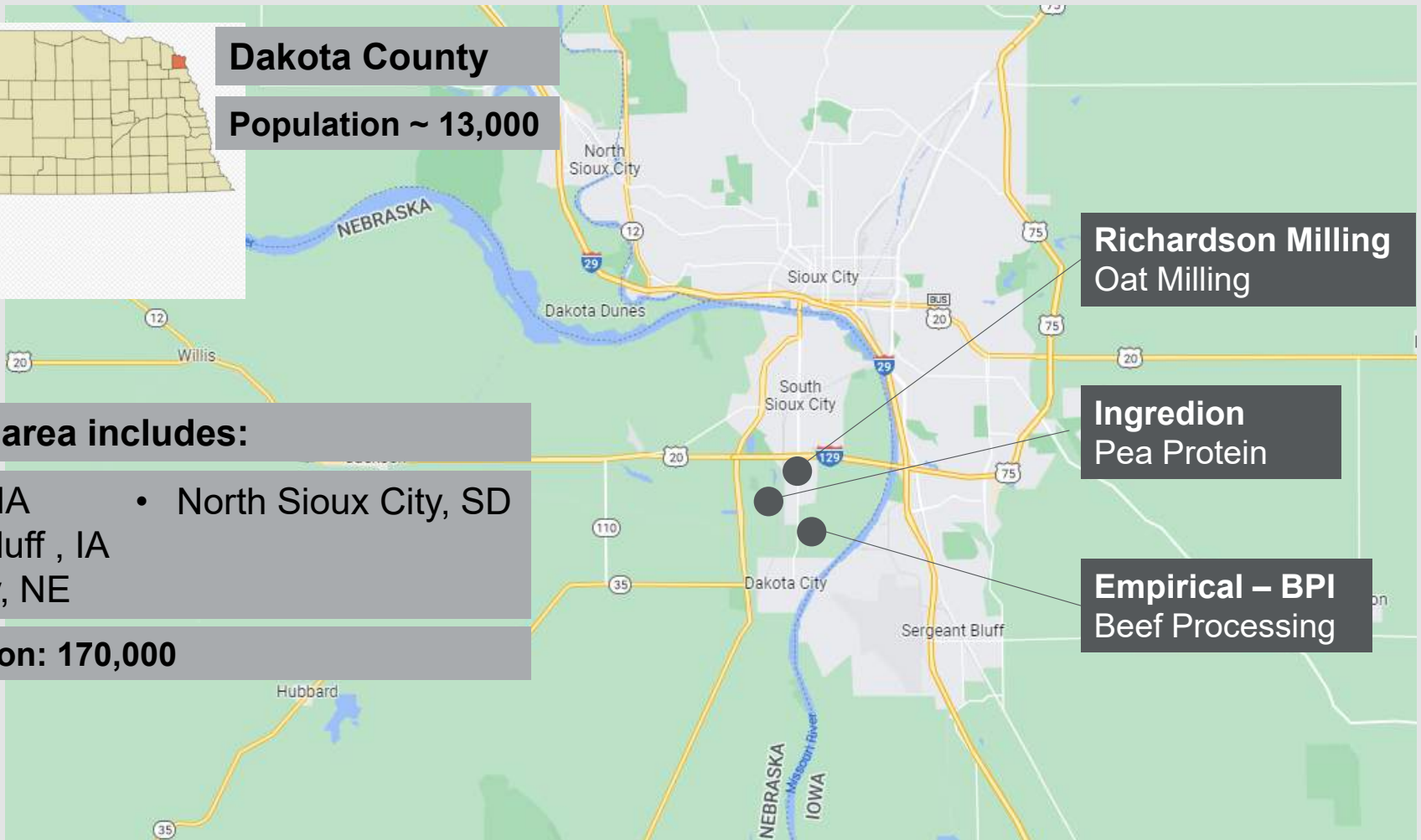
Dakota County

Population ~ 13,000

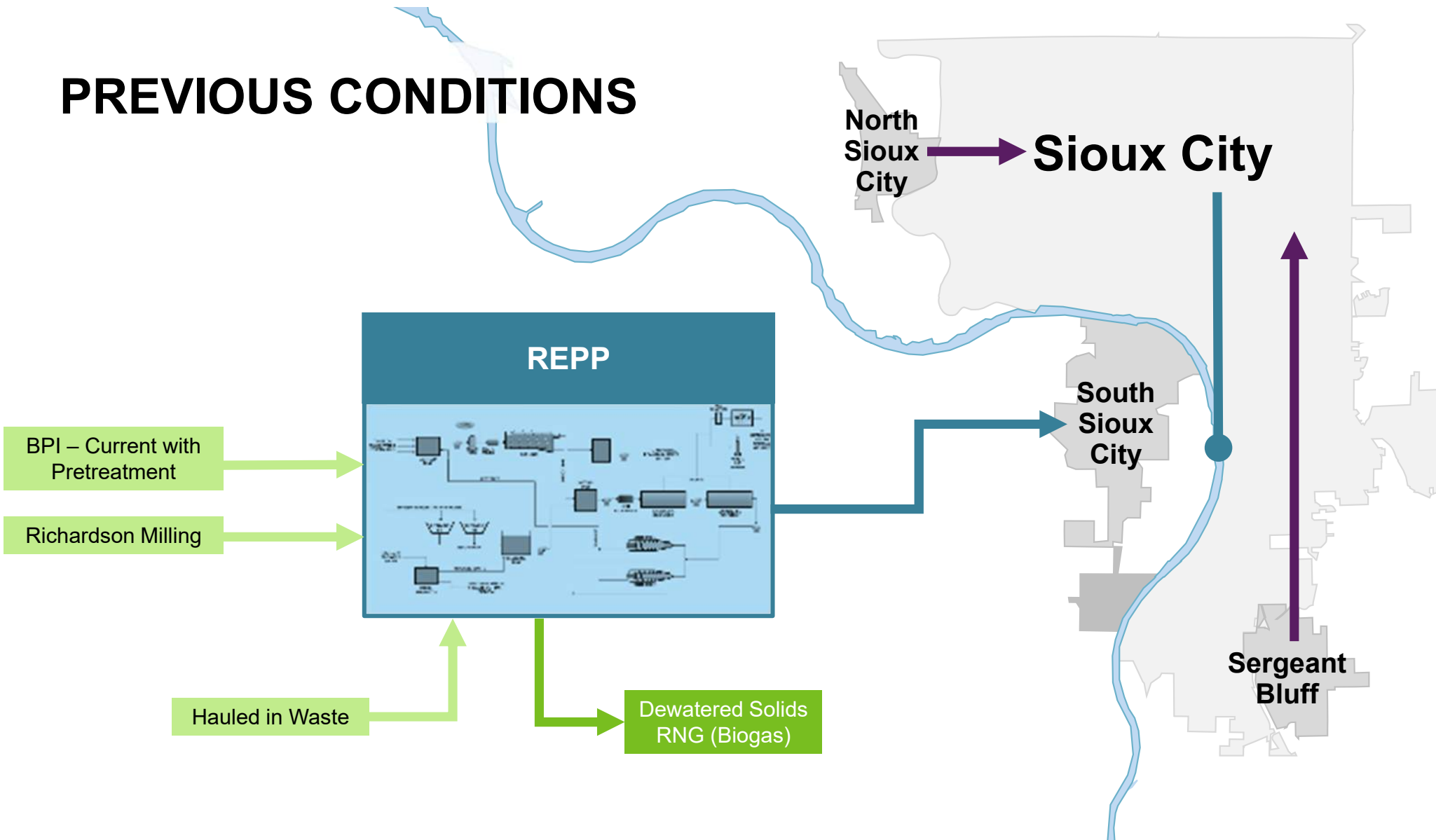
Metropolitan area includes:

- Sioux City, IA
- Sergeant Bluff, IA
- Dakota City, NE
- North Sioux City, SD

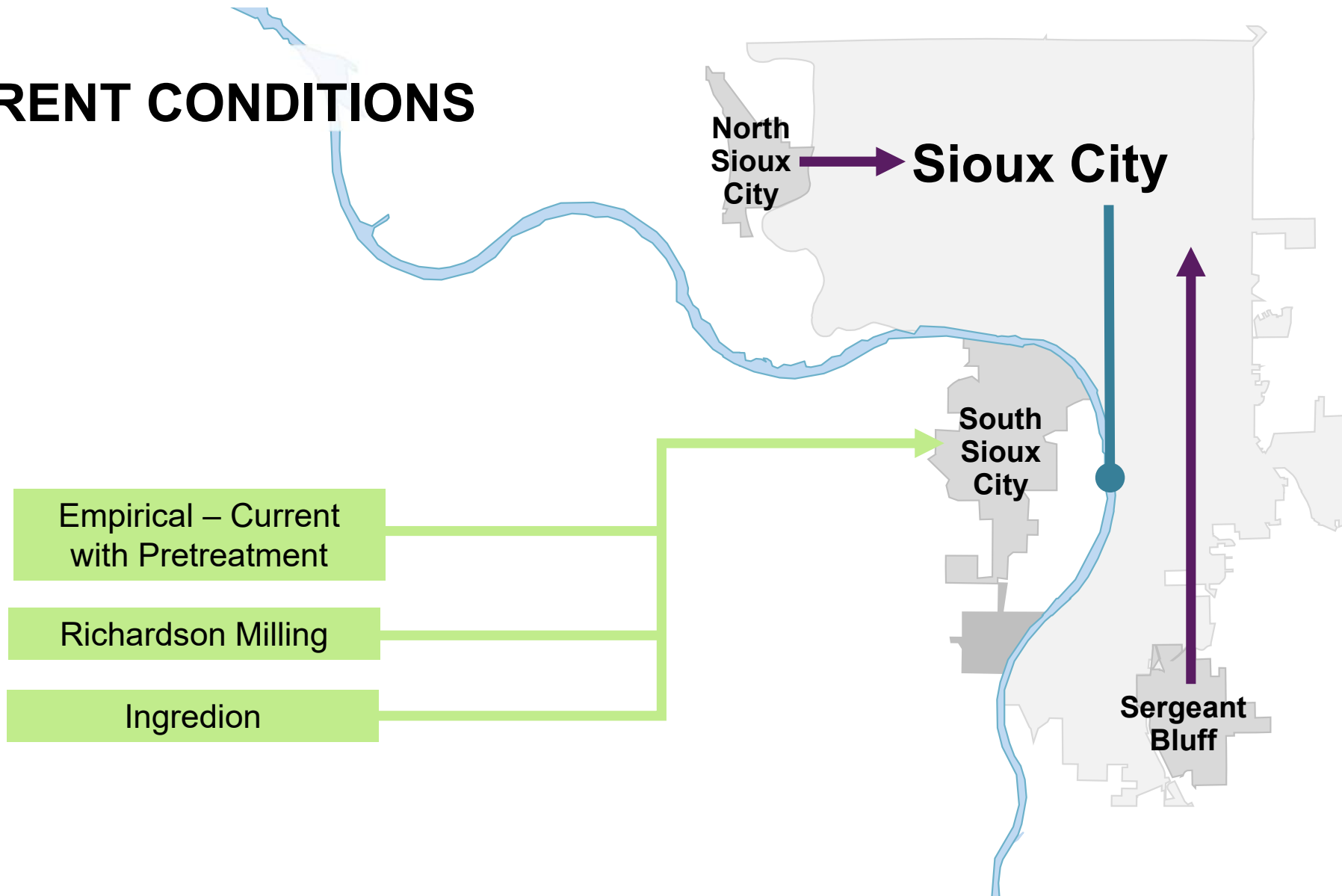
Metro population: 170,000



PREVIOUS CONDITIONS



CURRENT CONDITIONS



- Empirical – Current with Pretreatment
- Richardson Milling
- Ingredion



02

PROJECT NEEDS & OBJECTIVES



PROJECT NEEDS

- Pretreatment facility out of operation
- Capacity restrictions from Sioux City
- Limit future growth of industries
- Rate increases
- Self reliance

OVERALL OBJECTIVES

Identify the most cost-effective (life cycle cost) treatment plant to serve South Sioux City, the industries involved, and potentially the other sister cities

Develop strategies to utilize existing infrastructure where possible

Plant must be implementable, expandable, and flexible

Plant must accommodate future nutrient removal, not generate odors, and be energy efficient



03

FEASIBILITY STUDY

INDUSTRIAL STAKEHOLDERS

Business Name	Type
Empirical – BPI	Beef Processing
Ingredion	Pea Protein
Richardson Milling	Oat Milling

Parameter	Units	Maximum Month	Annual Average
Flow	MGD	2.34	2.01
Flow	gpm	1,625	1,394
cBOD ₅	lb/day	74,800	61,000
TSS	lb/day	26,400	22,800
TKN	lb/day	3,900	3,200
TP	lb/day	1,500	1,200
FOG	lb/day	3,500	3,100
cBOD ₅	mg/L	3,830	3,640
TSS	mg/L	1,350	1,360
TKN	mg/L	200	191
TP	mg/L	76.9	71.7
FOG	mg/L	179	185

FEASIBILITY STUDY: ALTERNATIVES

1

ALTERNATIVE 1

Covered Anaerobic Lagoons

Conventional Activated Sludge

Ultraviolet Disinfection

WAS Storage

2

ALTERNATIVE 2

Covered Anaerobic Lagoons

Aerobic Granular Sludge

Ultraviolet Disinfection

WAS Storage

3

ALTERNATIVE 3

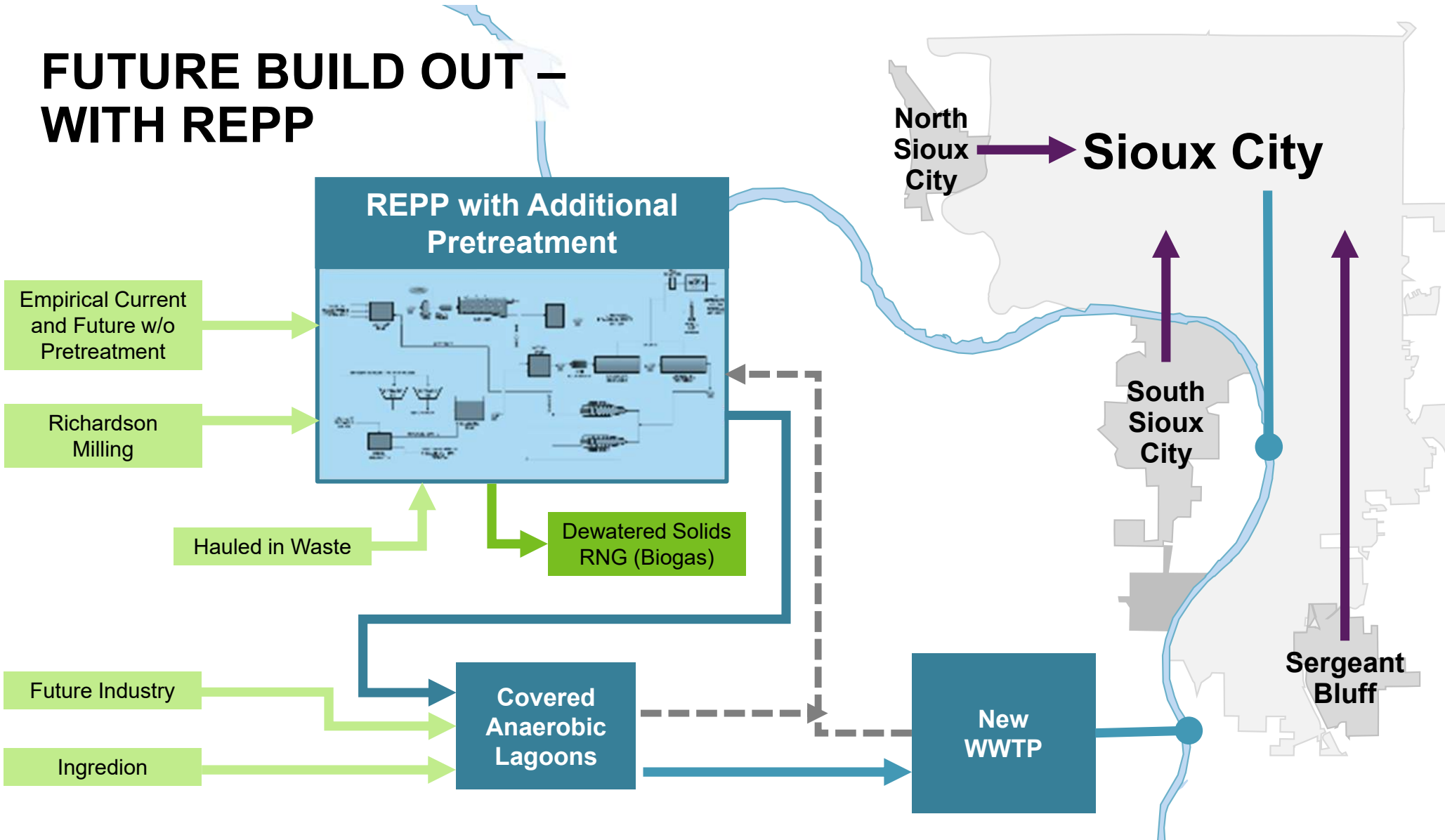
Anaerobic Membrane Bioreactors

Membrane Aerated Bioreactors

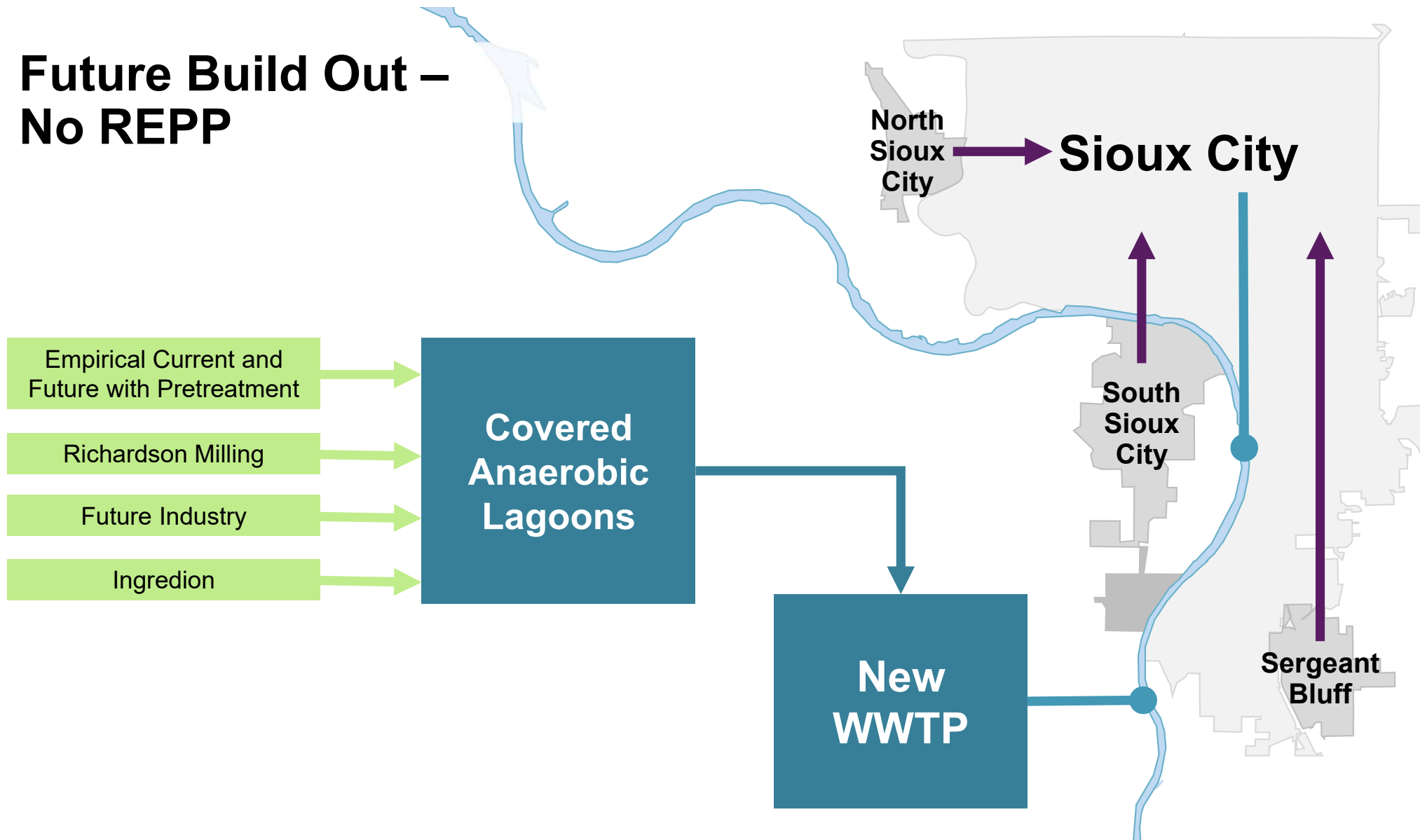
Ultraviolet Disinfection

Most cost effective – OPCC \$ 33M

FUTURE BUILD OUT – WITH REPP



Future Build Out – No REPP



WHY AGS FOR SOUTH SIOUX CITY?

New Greenfield
Plant

Smaller
Footprint

Lowest Life
Cycle Costs

Flow and Load
Equalization
Upstream – Not
limited by peak
flows and can
handle higher
organic strength
wastewater

Modular and
Expandable –
Future Industries
and Residential

Energy Efficient
(20% less than
typical BNR)



04

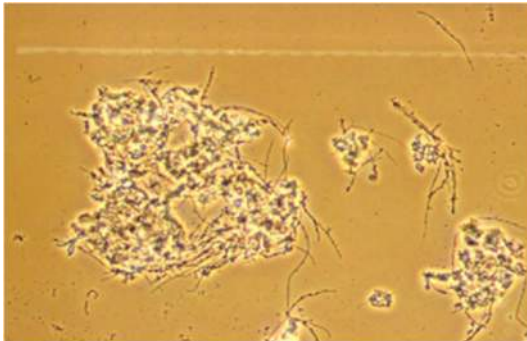
AGS OVERVIEW

INTENSIFIED ACTIVATED SLUDGE

Intensify: escalate; boost, increase; strengthen, augment; amplify, expand, magnify

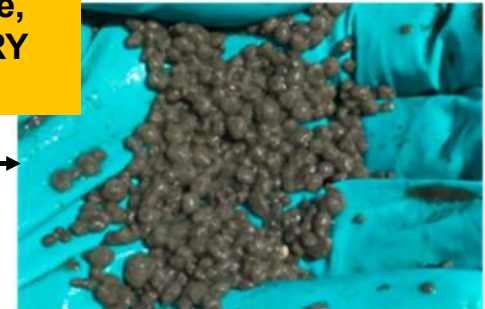
Intensification: doing more within the same volume/footprint, the same concrete. More treatment capacity, better performance, enhanced treatment

0.1 – 0.3 mm



Granules are 2-5 mm in size, settle VERY FAST

2 - 5 mm

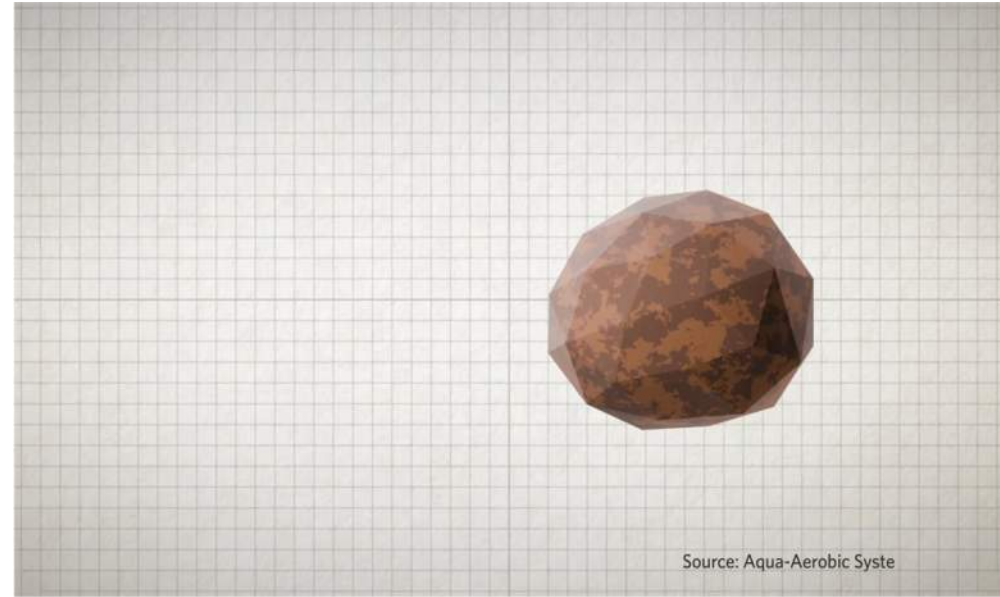


← Activated Sludge Intensification →

Intensification reduces capital investment, increases capacity, and saves operating cost

WHAT IS A GRANULE?

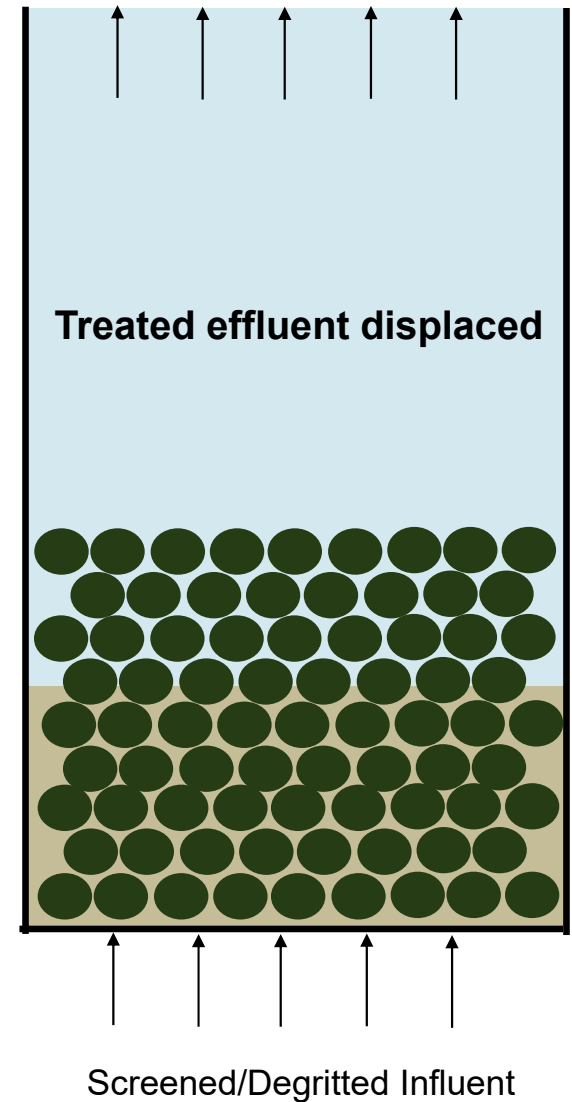
- Layered microbial community
- Not perfectly spherical
- Complex structure with voids & channels
- Faster settling than floc (SVI 5 vs 30)
 - Target SVI $5 < 60$
 - Less than 30% difference between SVI $10 < 30$



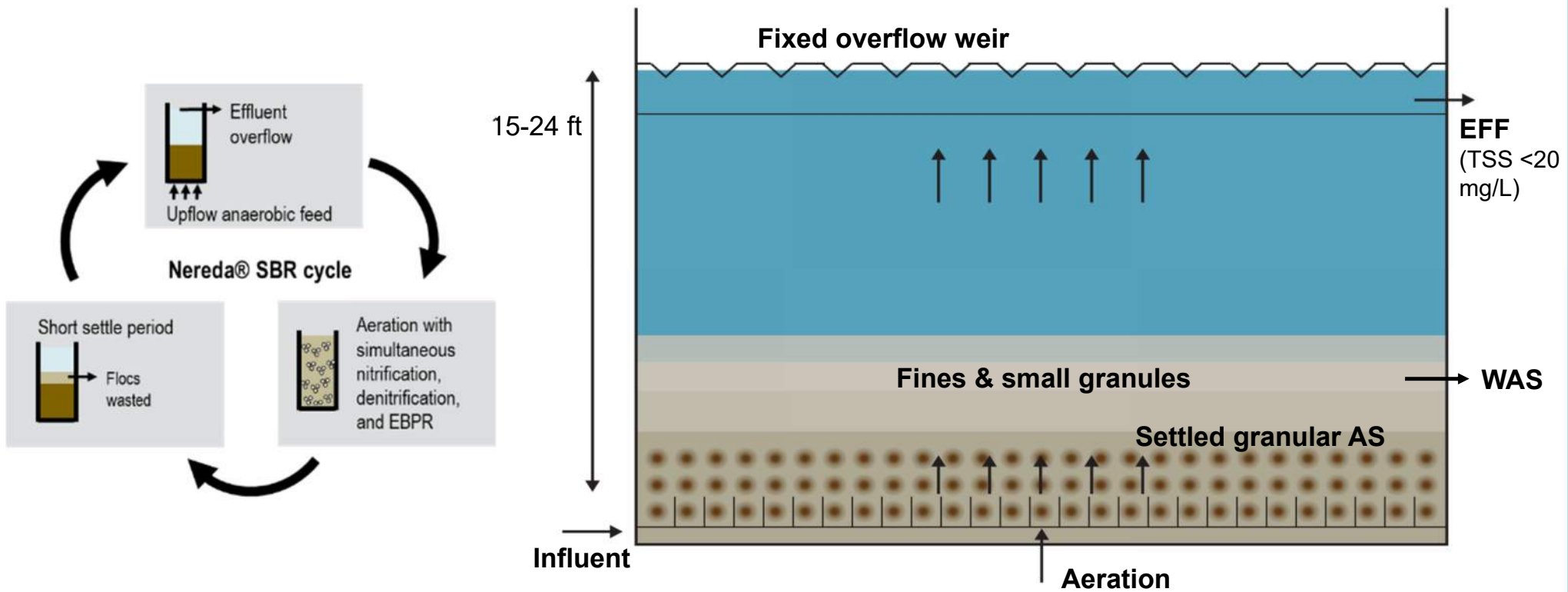
HOW DO GRANULES FORM?

Two Primary Methods:

1. Hydraulic Selection
 - Settle denser granules
 - Selective wasting of lighter floc (midtank)
2. Biological Selection
 - Select for PAOs (form EPS)
 - Slow up-flow feeding through settled granules
 - Provides high F/M contacting and preferential feeding



A LOOK AT HOW IT FUNCTIONS: REACTOR

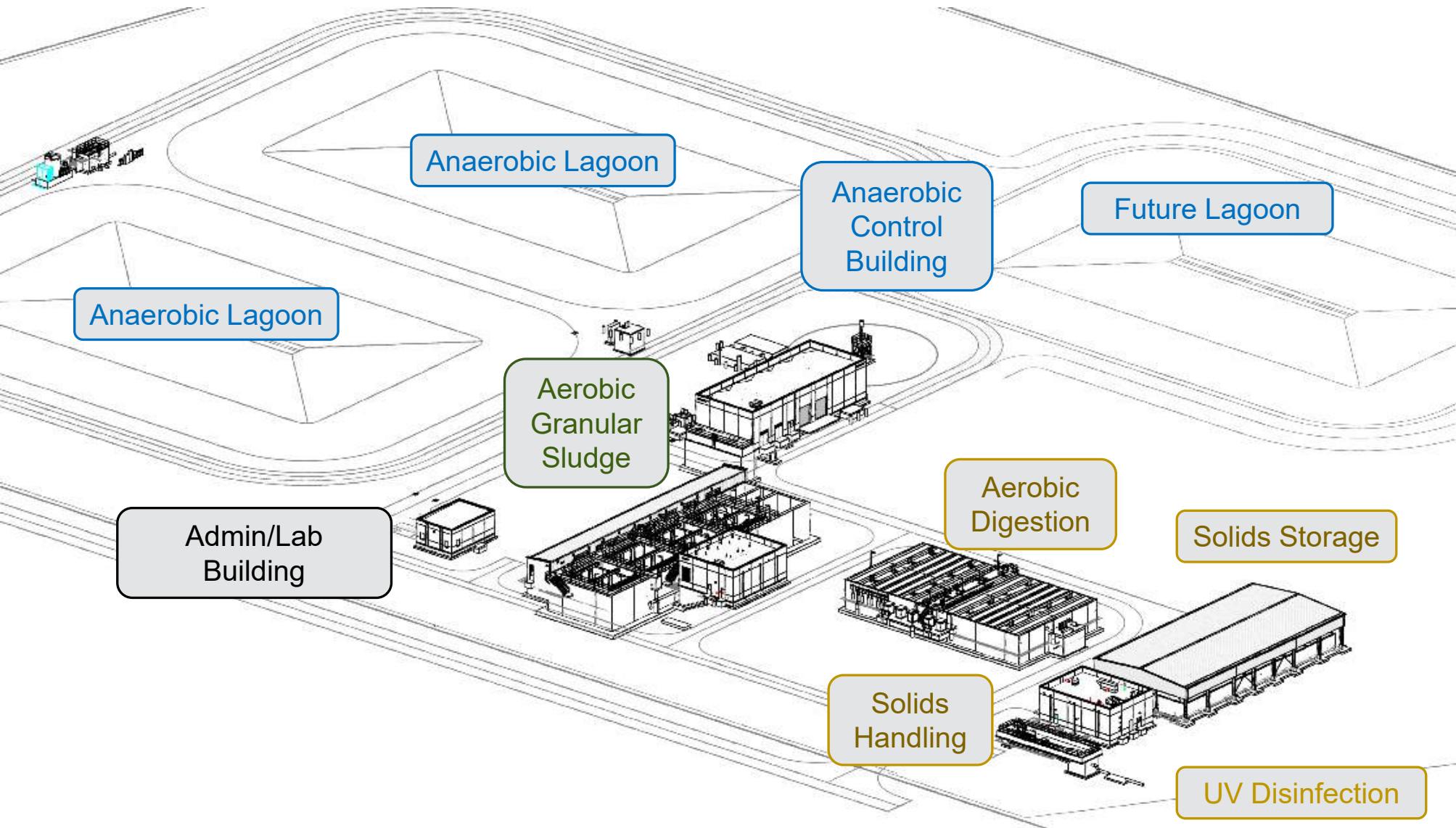




05 DESIGN

TREATMENT EFFLUENT LIMITS

Parameter	Monthly Average	Maximum
Carbonaceous Biochemical Oxygen Demand (5-day)	25.0 mg/L 1,460 lb/d	40.0 mg/L 2,336 lb/d
Total Suspended Solids	30.0 mg/L 1,752 lb/d	45.0 mg/L 2,629 lb/d
pH	6.5 S.U.	9.0 S.U.
Fats, Oils, and Grease (FOG)	10 mg/L	10 mg/L
Spring Ammonia	66 mg/L	100 mg/L
Summer Ammonia	78 mg/L	157 mg/L
Winter Ammonia	69 mg/L	140 mg/L



Anaerobic Lagoon

Anaerobic Control Building

Future Lagoon

Anaerobic Lagoon

Aerobic Granular Sludge

Admin/Lab Building

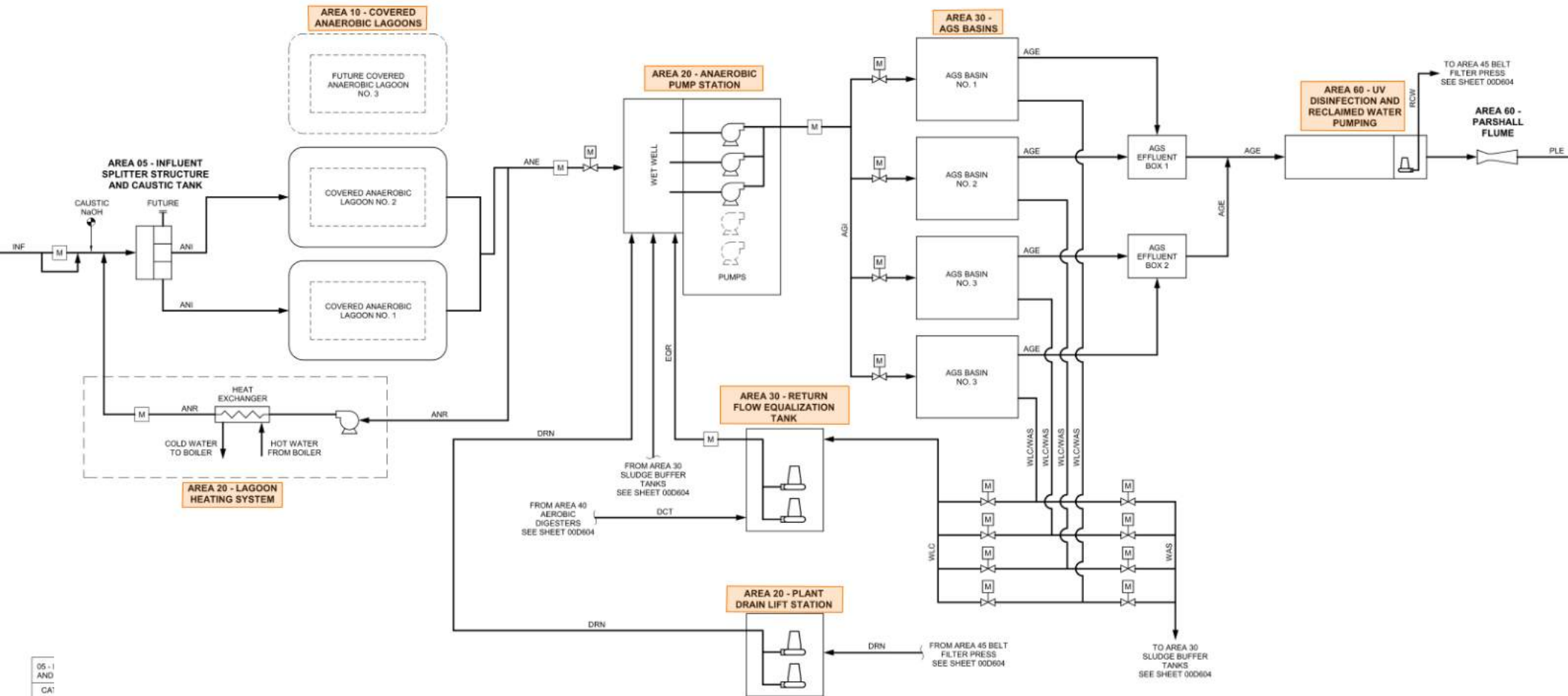
Aerobic Digestion

Solids Storage

Solids Handling

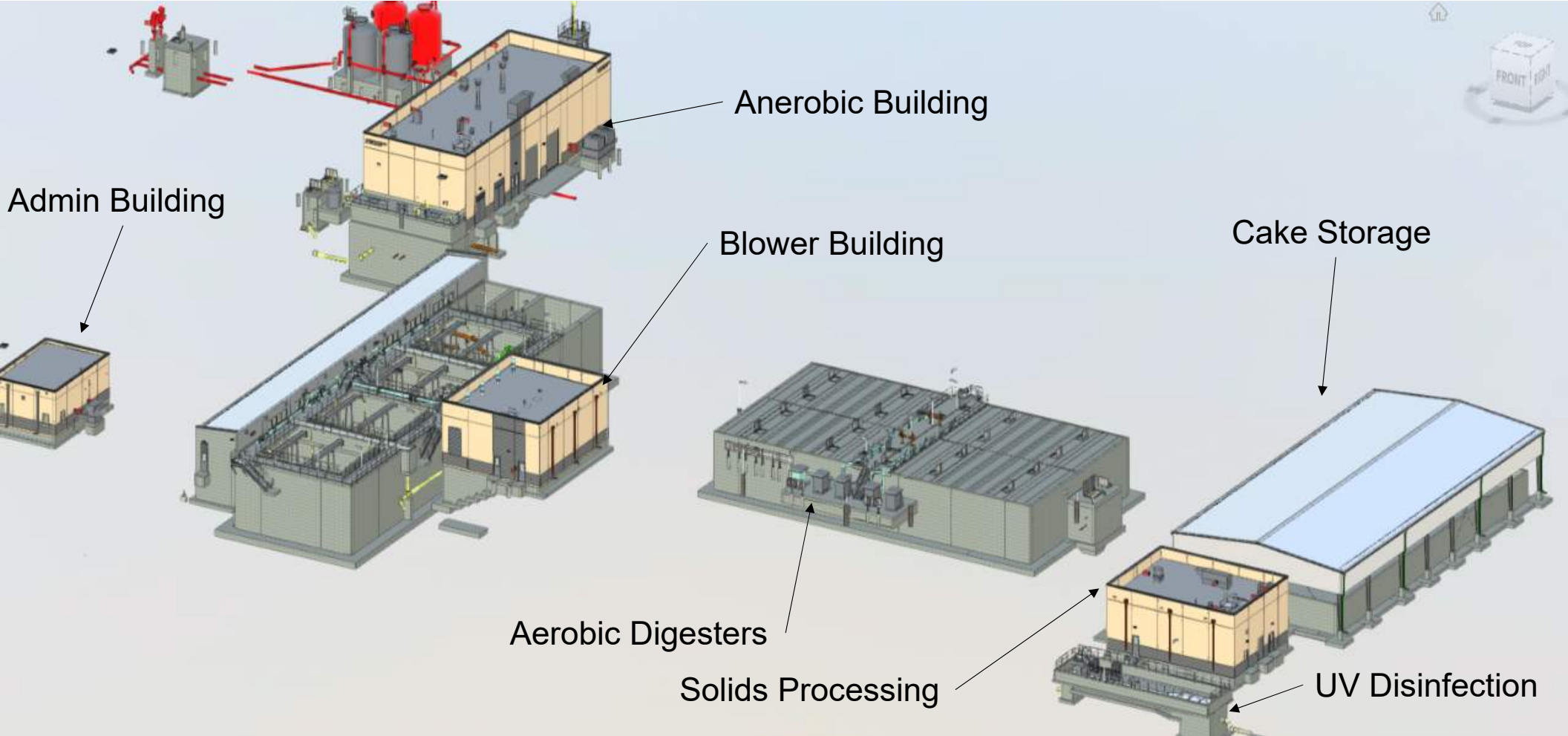
UV Disinfection

PROCESS FLOW DIAGRAM



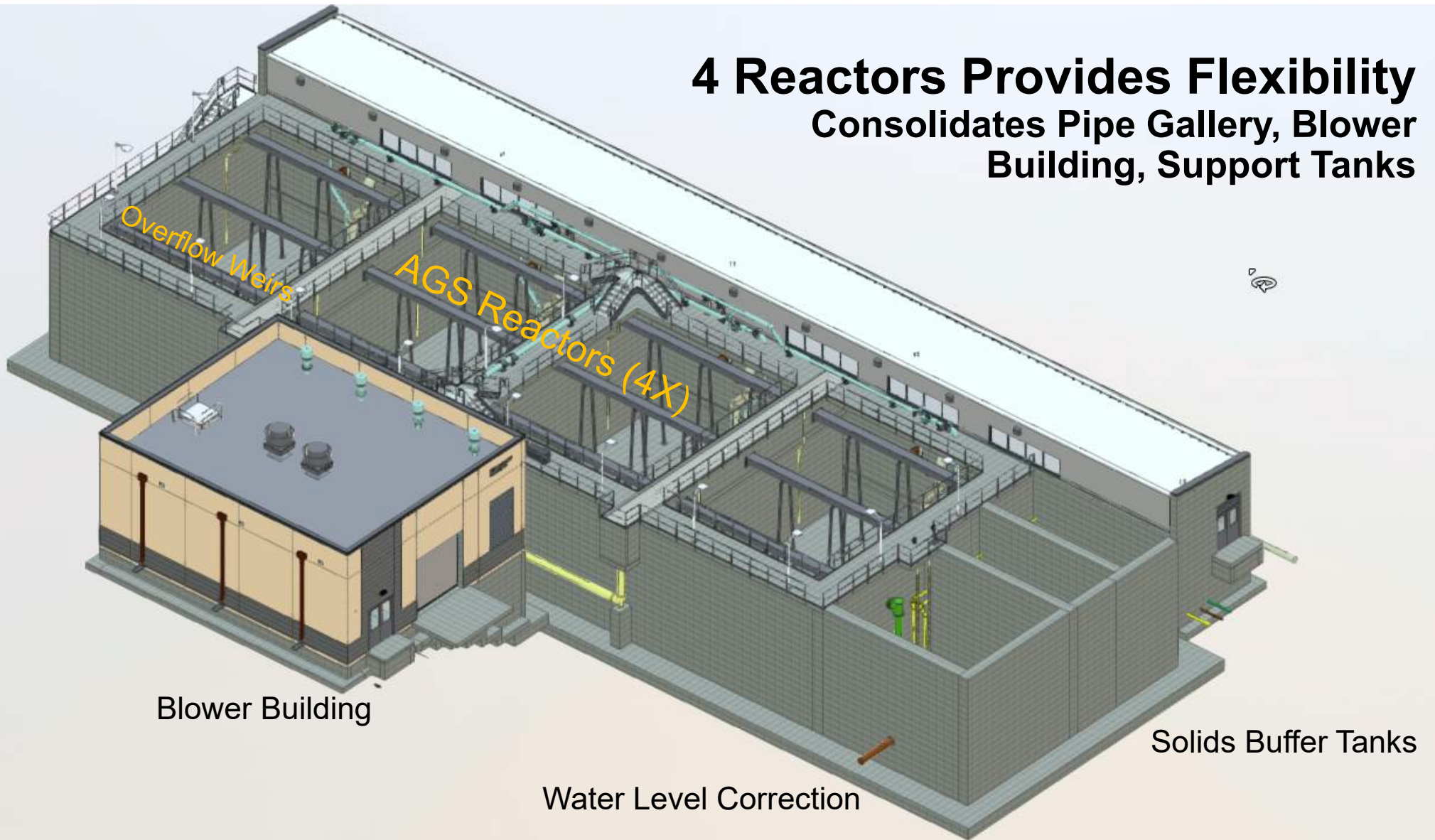
05 - I
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SOUTH SIOUX CITY SITE MODEL



4 Reactors Provides Flexibility

Consolidates Pipe Gallery, Blower Building, Support Tanks





06

BIDDING & MARKET CONDITIONS

Engineer's Estimate

\$33,000,000



Bid Opened: February 25, 2021

Texas Storms: February 10-11, 13-17, and 15-20



3 Bids Received

John T Jones: \$39,215,000

Eriksen Construction: \$40,133,322

Hawkins Construction: \$42,865,775



MARKET CONDITIONS

- Bids Opening in February 2021
- COVID supply chain issues
- Right after Texas Storm
- Supplier quotes were valid for only 2 weeks
- PVC, HDPE had a 40-50% rise in that month
- Rebar/ pre engineered metal building, iron, handrails, metals – 40% higher
- Local market for subs, electrical labor is competitive
- Gas prices

PROJECT FUNDING

- \$1 million VE options were identified
- Additional SRF loan money was acquired
- Project has \$12 million EDA grant funding

PROJECT STATUS

- Received Bids – February 25, 2021
- Notice of Award – April 16, 2021
- Notice to Proceed – June 2, 2021
- Construction Complete – June 2023
- WWTF Expansion Design started - July 2023









**AGS TANKS
AND PIPE
GALLERY**



**AGS PIPE
GALLERY**



**AEROBIC
DIGESTERS**

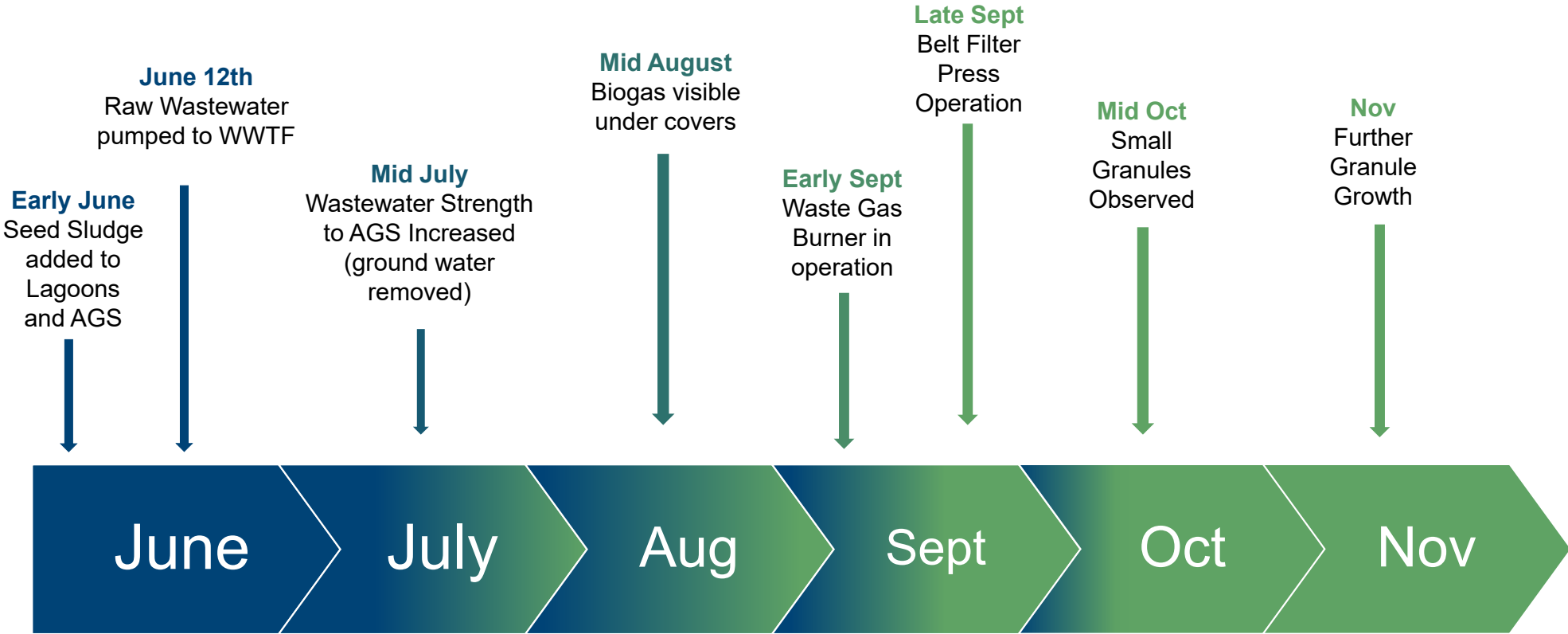




07

START-UP

Timeline of Startup - 2023



SEEDING



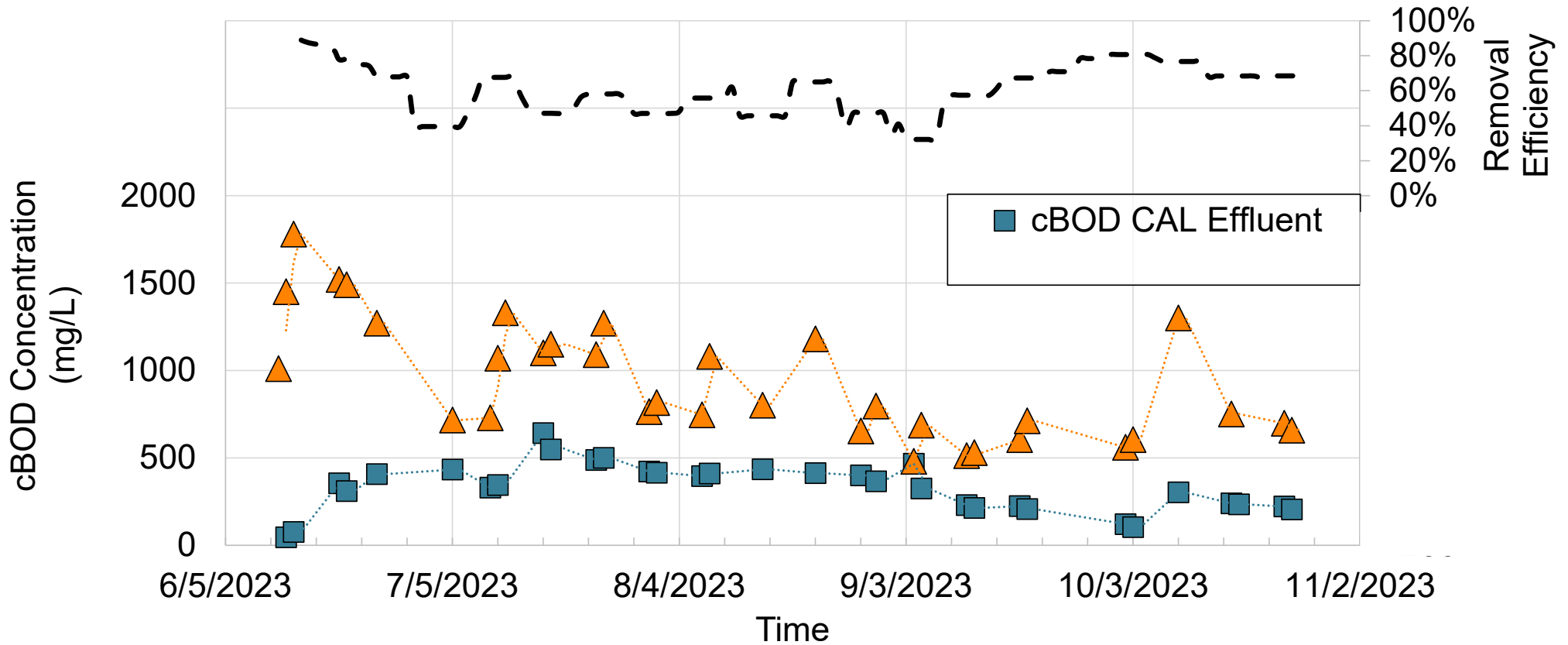
START UP OPERATIONAL MONITORING

- Covered Anaerobic Lagoon (CAL)
 - Operating Temperature: 90-95 °F
 - Caustic dosing for pH control
 - + Maintain residual alkalinity for AGS
 - Water quality: Volatile acids, pH, cBOD, COD
 - Sulfates in anaerobic influent reduced to hydrogen sulfide
 - Quaternary Ammonium Compounds (Quat) measured (6 mg/L)
- AGS
 - D.O., ORP
 - MLSS
 - Settle timing and cycle structure.
 - Wasting visual checks
 - Water quality: COD, cBOD, TKN, NH₃, FOG

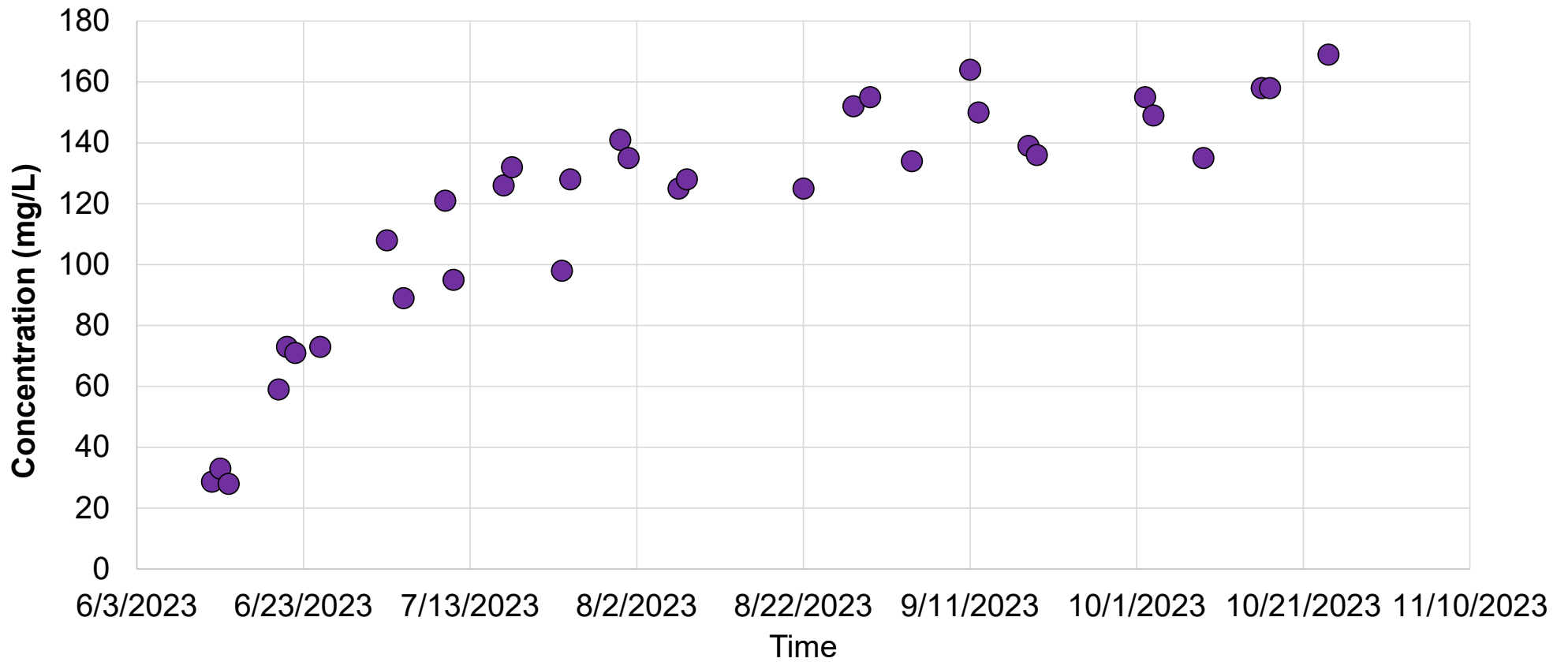
CAL PRETREATMENT TARGETS AND PERFORMANCE

Parameter	Treatment Target	Measured Current Performance
cBOD ₅	80%	75%
TSS	70%	80%
TKN	10%	18%
FOG	90%	90%

CAL cBOD REMOVAL



CAL EFFLUENT AMMONIA TO AGS



SEPTEMBER 5th 2023

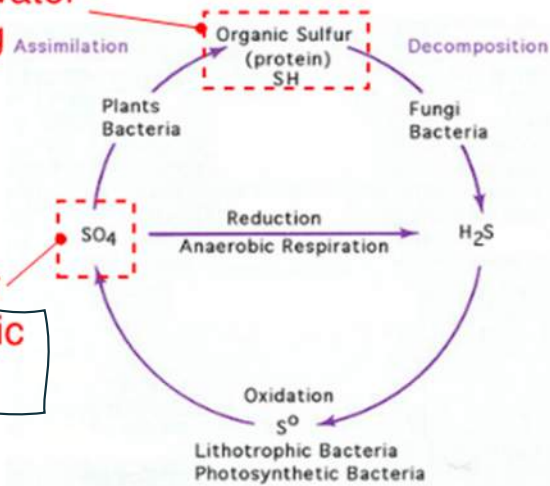


THE SULFUR PROBLEM

1. Original Design Assumptions
 1. Average Biogas Generation → 460 scfm
 2. Biogas H₂S → 2,000 – 3,000 ppmv (based on other lagoon experience)
 3. Proprietary H₂S biogas Scrubbing vessel (Activated Carbon style) → life 1.5 years
2. Current Operating Biogas data
 1. Average Biogas Generation → 200 scfm
 2. Biogas → 14,000 to 20,000 ppmv H₂S (grab samples)
 3. Existing Scrubber → life, around 4 months, removal efficiency questionable.

Industrial Wastewater

- Meat Packaging
- Pea Protein



- Drinking water
- Industry sulfuric acid usage

OSHA Health Hazards Guidelines

Concentration (ppm)	Symptoms/Effects
0.00011-0.00033	Typical background concentrations
0.01-1.5	Odor threshold (when rotten egg smell is first noticeable to some). Odor becomes more offensive at 3-5 ppm. Above 30 ppm, odor described as sweet or sickeningly sweet.
100-150	Loss of smell (olfactory fatigue or paralysis).
200-300	Marked conjunctivitis and respiratory tract irritation after 1 hour. Pulmonary edema may occur from prolonged exposure.
500-700	Staggering, collapse in 5 minutes. Serious damage to the eyes in 30 minutes. Death after 30-60 minutes.
700-1000	Rapid unconsciousness, "knockdown" or immediate collapse within 1 to 2 breaths, breathing stops, death within minutes.
1000-2000	Nearly instant death

Analytical Results

Sample ID: Before Flare 1	Sampling Location: City of South Sioux Waste Water Plant	
Lab ID: 2405350001		
Method: Light Hydrocarbons by GC-FID	Media: SKC 232-01, Tedlar Bag 1L	
Dilution: 100	Sampling Parameter: Air Volume 1 L	
Analyte	Result (ppm)	RL (ppm)
Methane	660000	1000
Method: Sulfur Gases Scan	Media: SKC 232-01, Tedlar Bag 1L	
Dilution: 50000	Sampling Parameter: Air Volume 1 L	
Analyte	Result (ppm)	RL (ppm)
Hydrogen sulfide	20000	350

SULFUR MANAGEMENT OPTIONS

1. Source Control → Reduce sulfuric acid usage at the industries.
 1. Pilot Testing in planning stage.
2. Install full treatment Chemical Biogas scrubbing system.
 1. Large capitol costs \$4.0 – 5.0 Million
3. Install partial treatment Chemical Biogas scrubbing system and Control pH.
 1. Large capitol costs \$2.0 – 3.0 Million, plus \$0.75 Million/year in chemical cost
4. Control pH ~8.0, continue to use existing scrubber
 1. Large O&M costs ~ \$1.0 - 1.5 Million/year in chemical and media costs.

Solution is most likely a combination of Options.

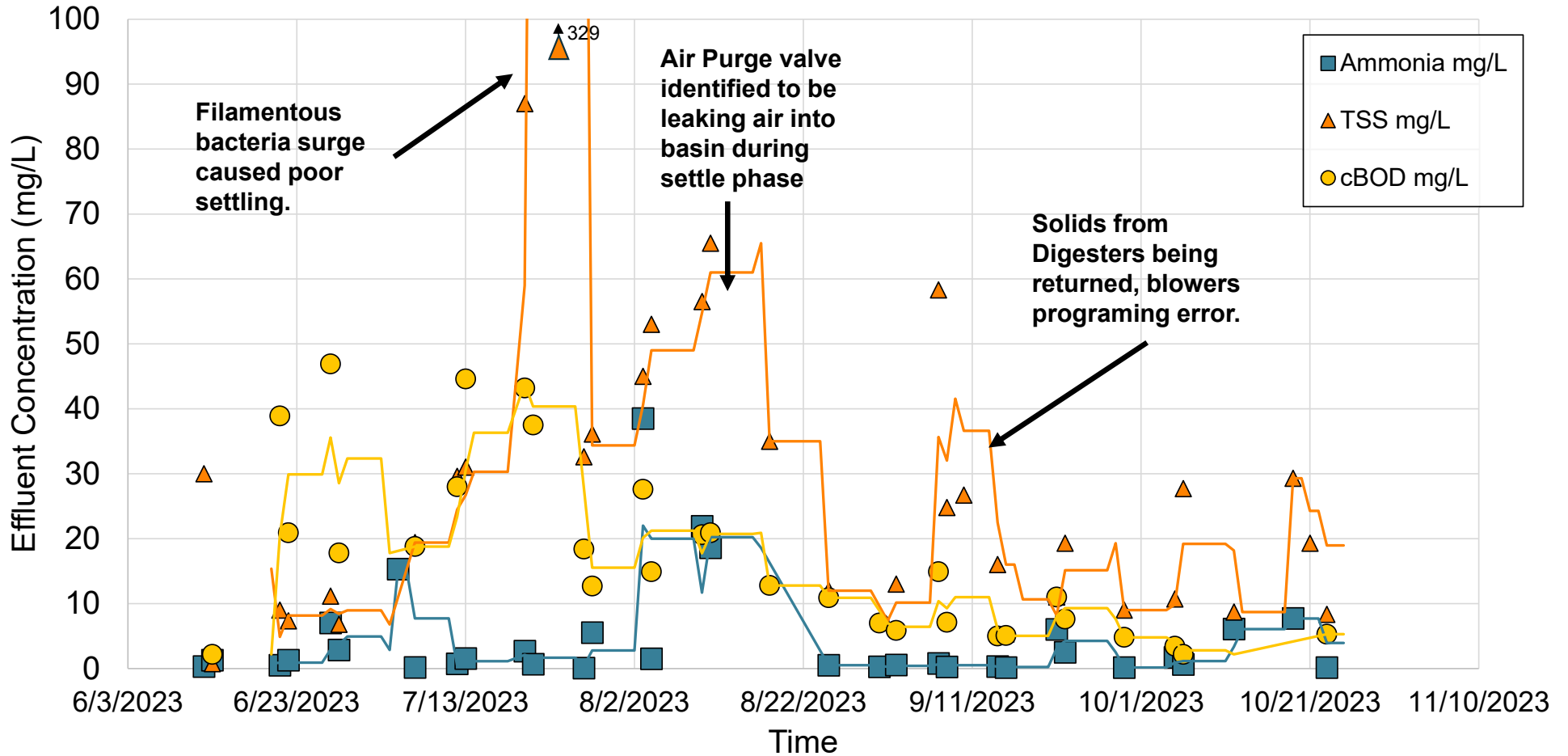
AGS OPERATION

- MLSS concentration:
 - Design: 8,000 mg/L
 - Current: 3,500 – 4,500 mg/L
- Operating Cycle:
 - Fill: 1.5 hr
 - React: 3.5 hr
 - Settle/WAS: 40min
- Operating Temperature: 83-93 °F
- Aeration Control:
 - Ammonia based aeration control
 - Dissolved oxygen control

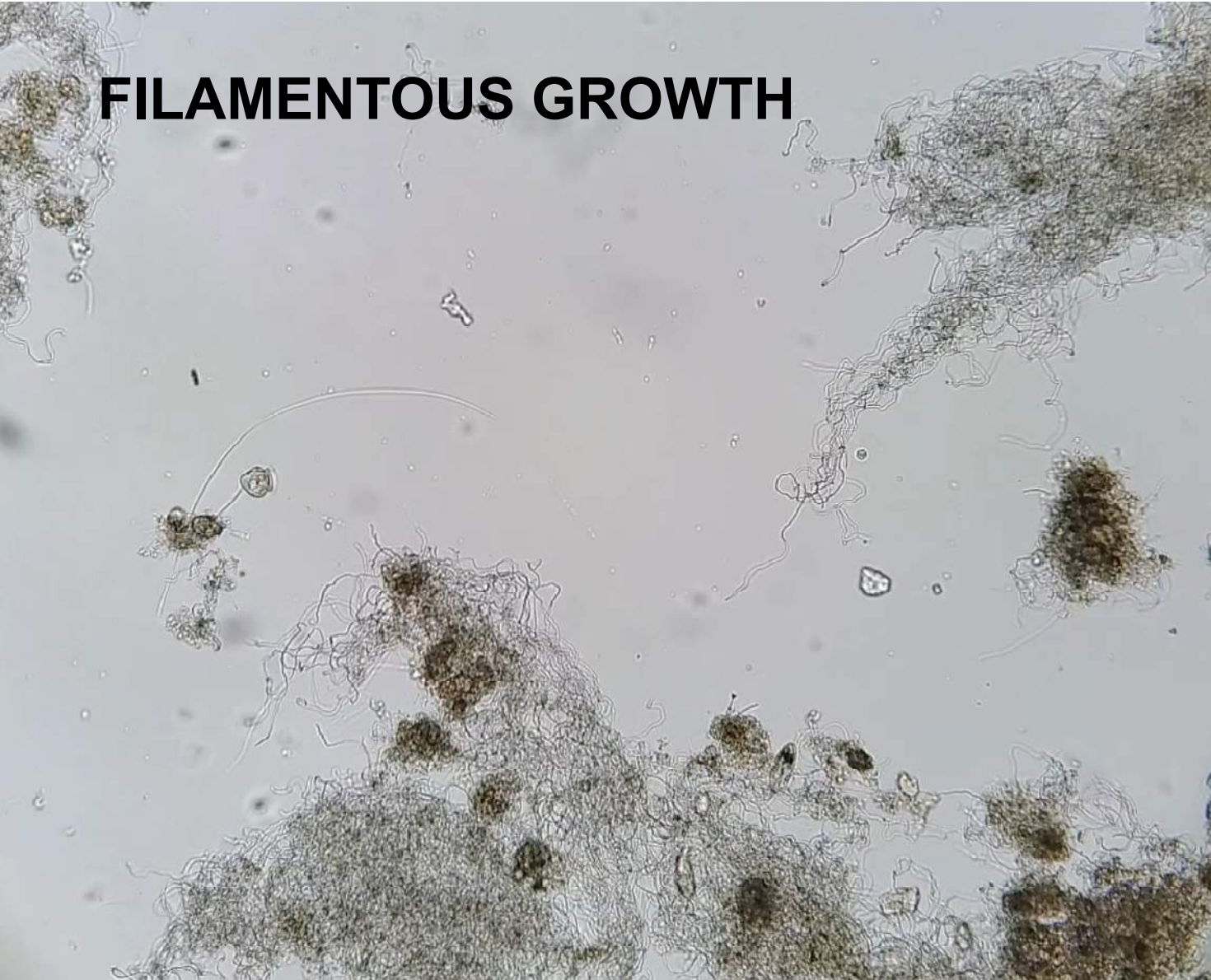


AGS during fill/decant cycle October 31st

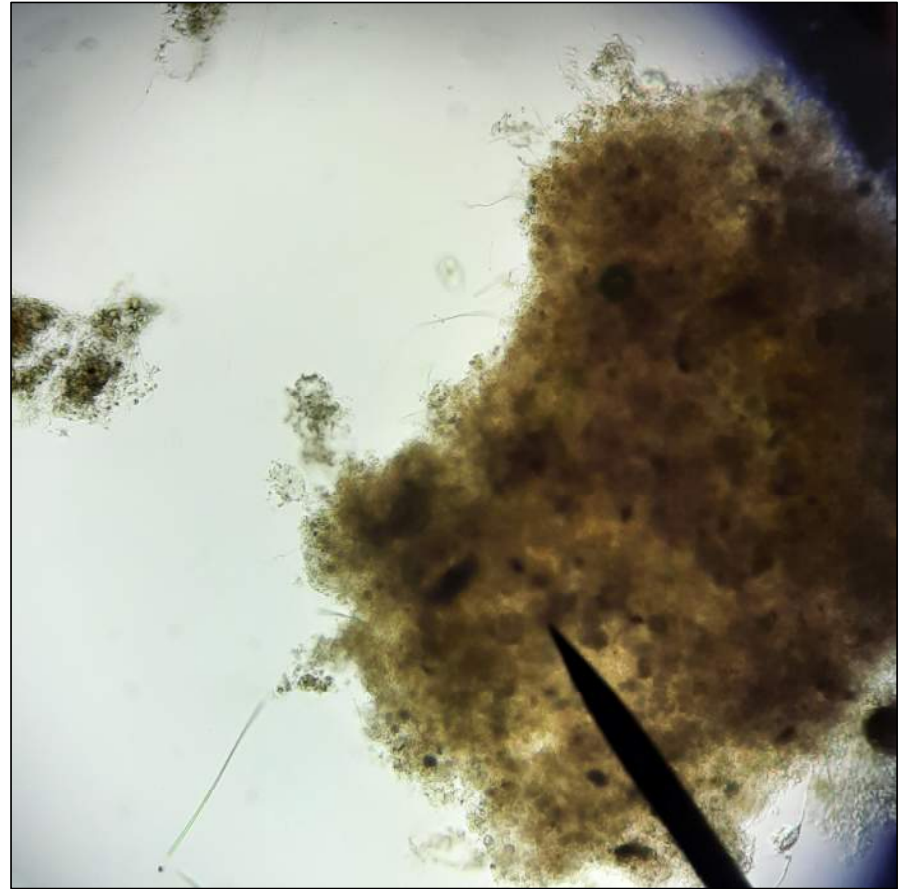
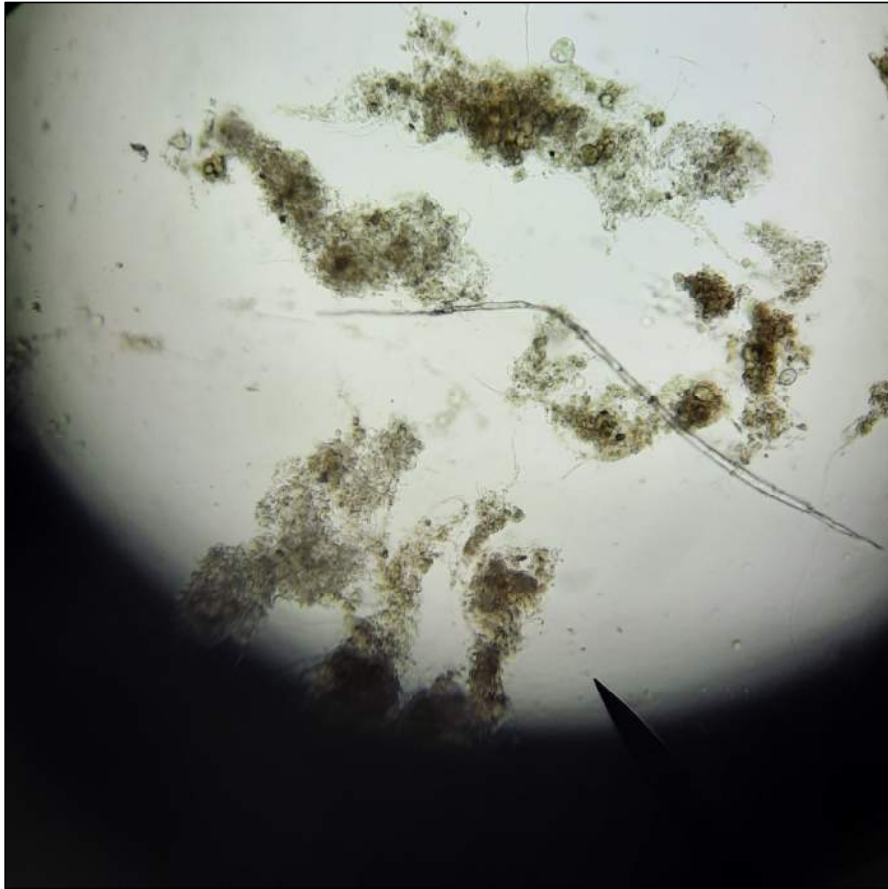
AGS STARTUP EFFLUENT QUALITY



FILAMENTOUS GROWTH



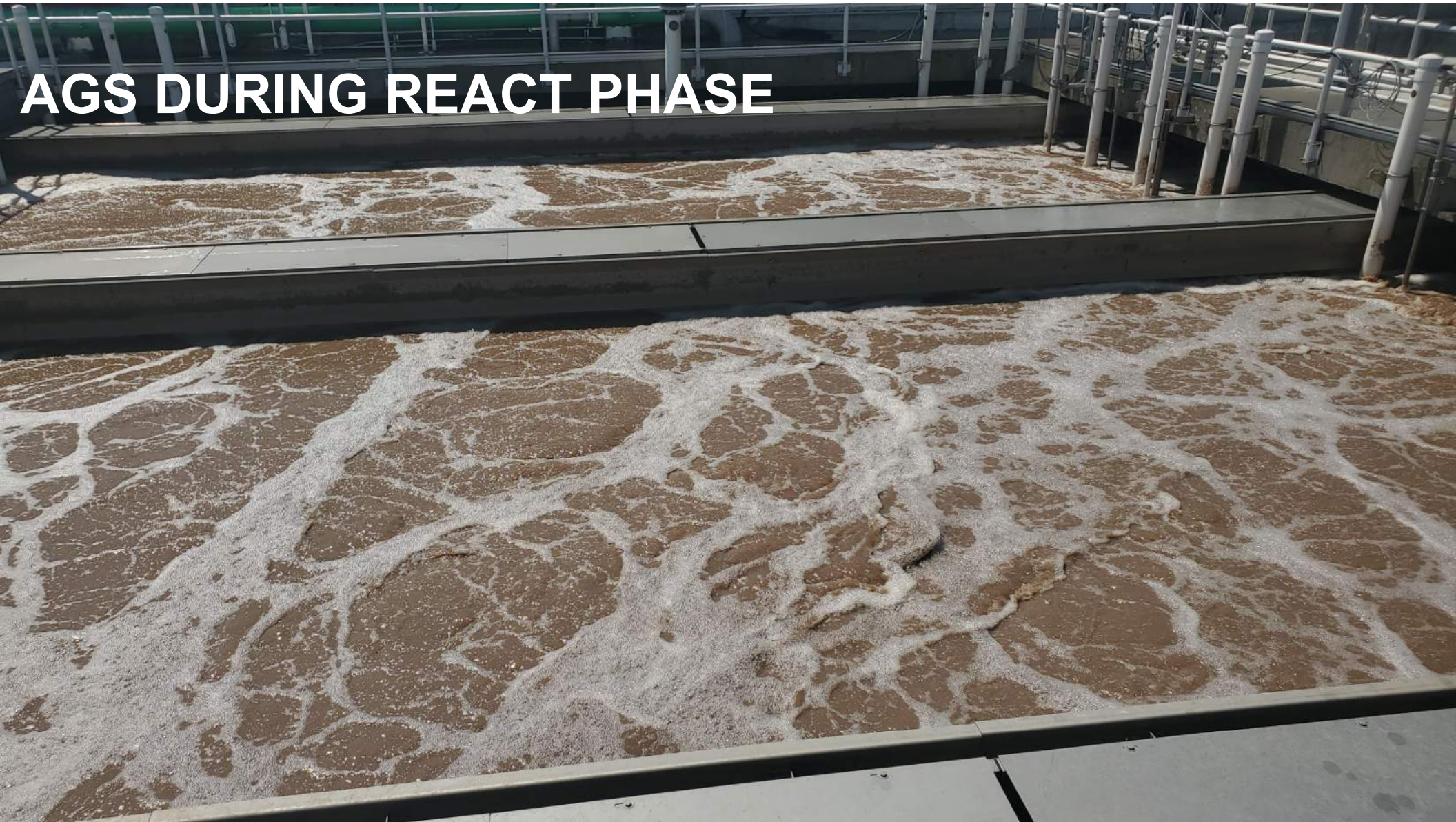
GRANULATION IN PROGRESS – 8/30



AGS DURING FILL/DECANT PHASE – OCT. 25TH

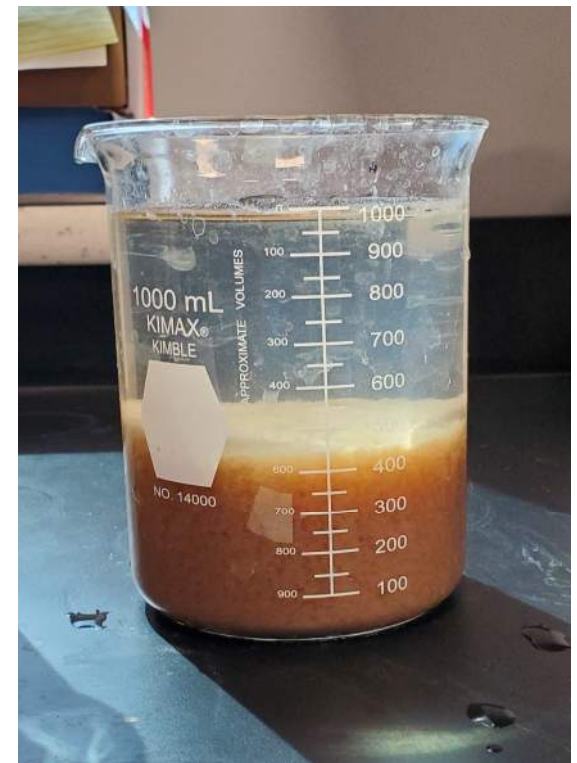
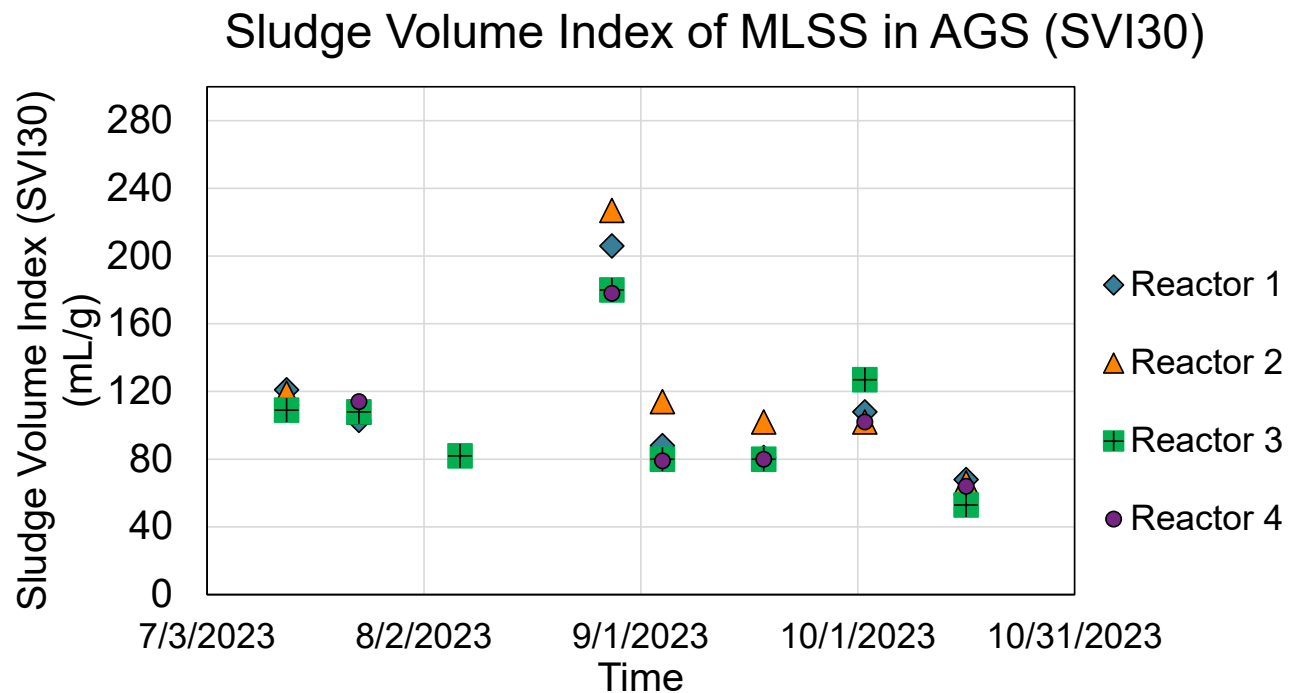


AGS DURING REACT PHASE



SETTLING AND WASTING

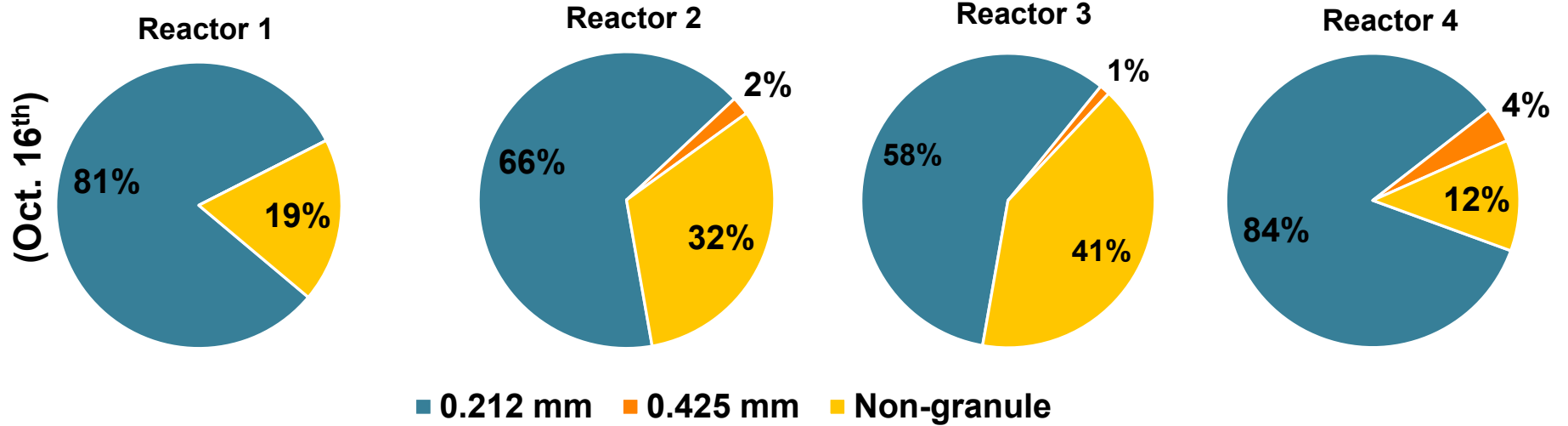
- Driving down settling times (45 to 30min)



Settled Waste Activated Sludge

BABY GRANULES ARE GROWING – Oct 17TH

MLSS Distribution



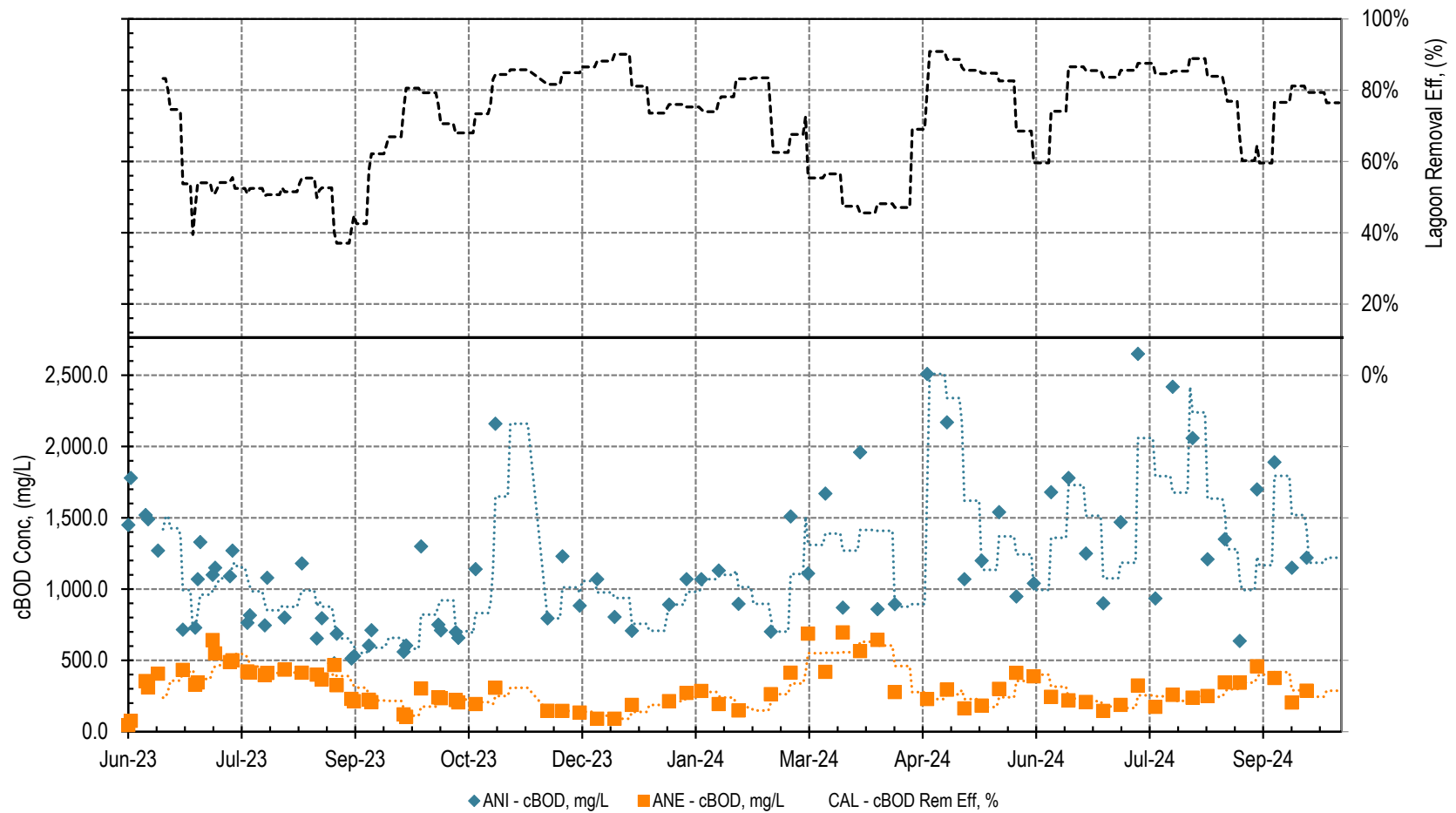




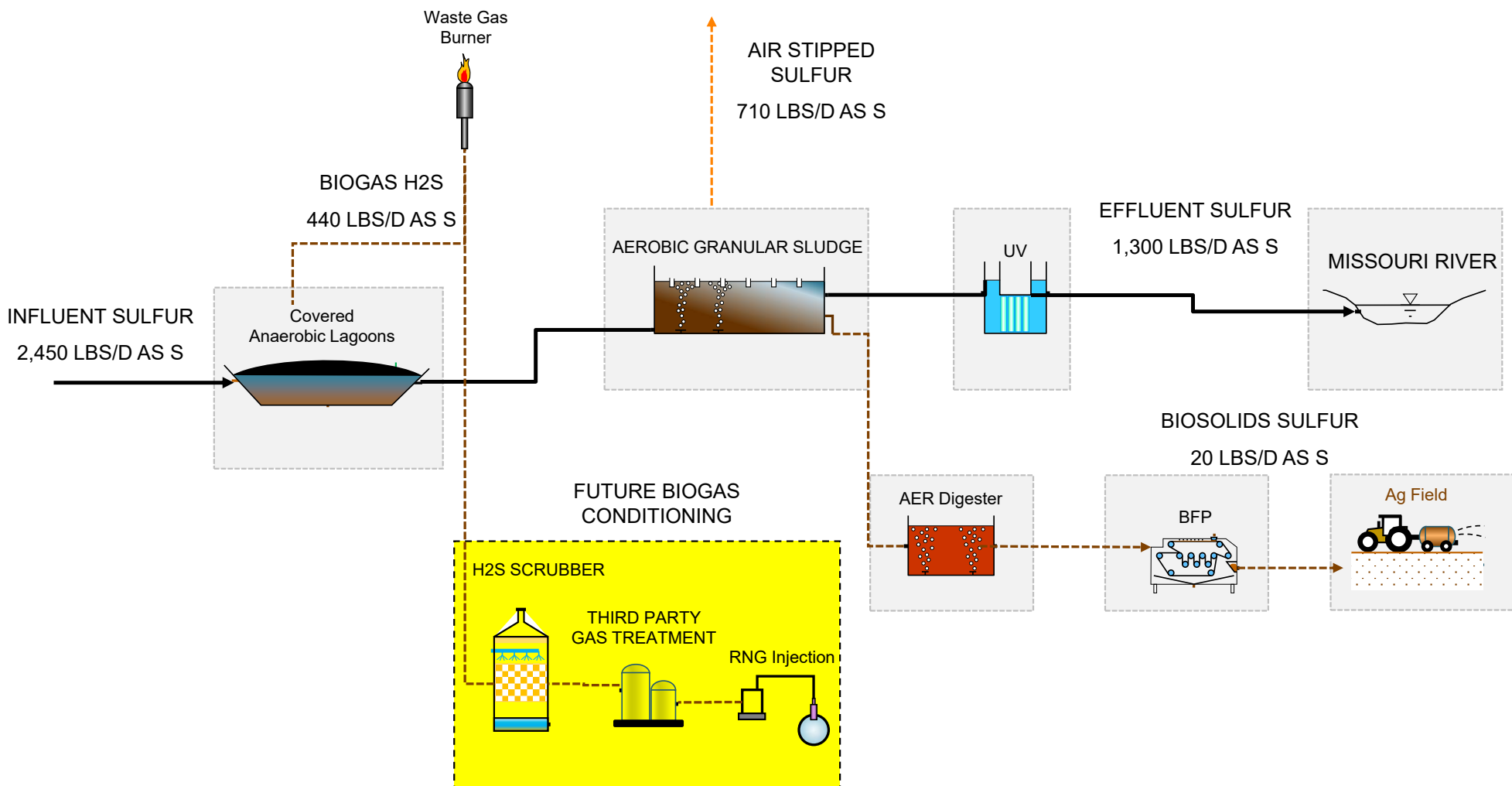
08

Looking Forward

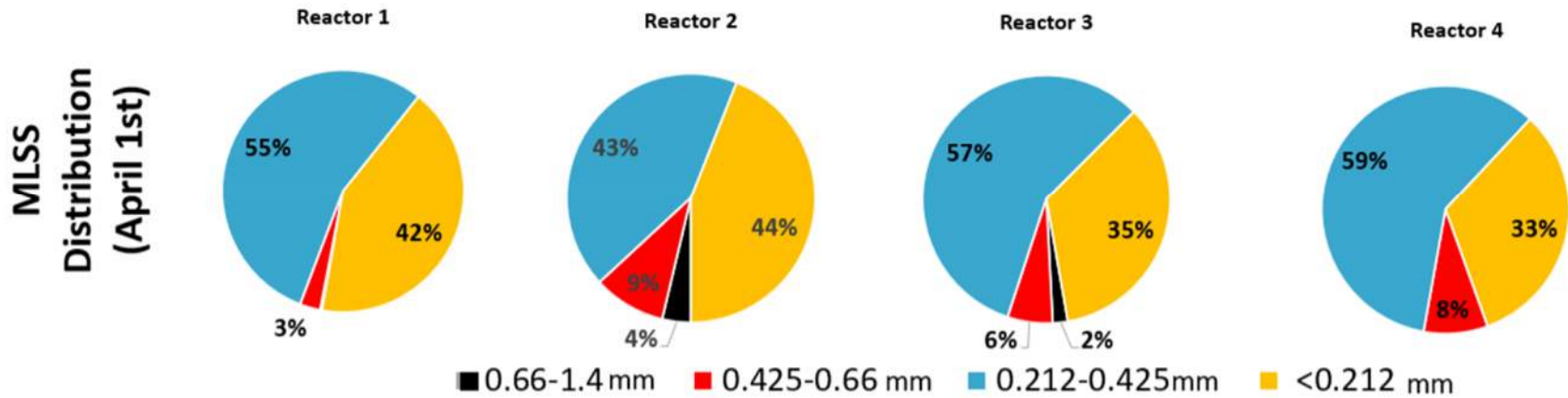
CAL cBOD Removal



FUTURE BIOGAS CONDITIONING

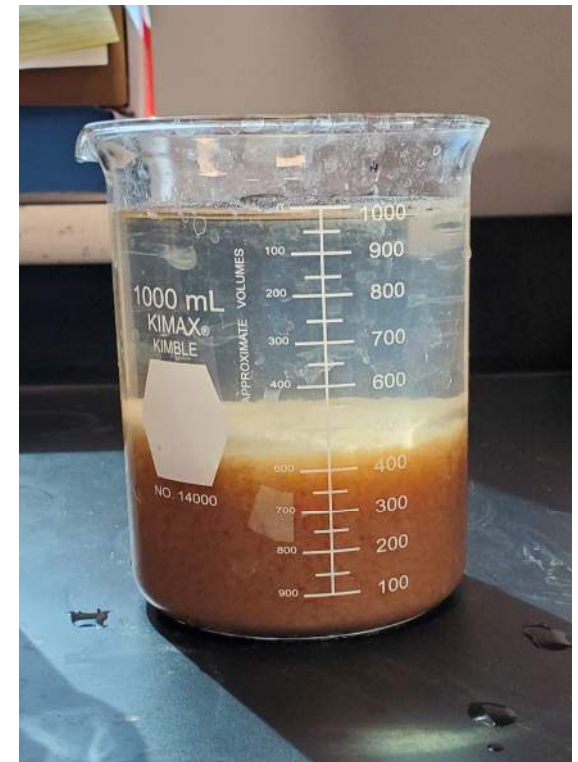
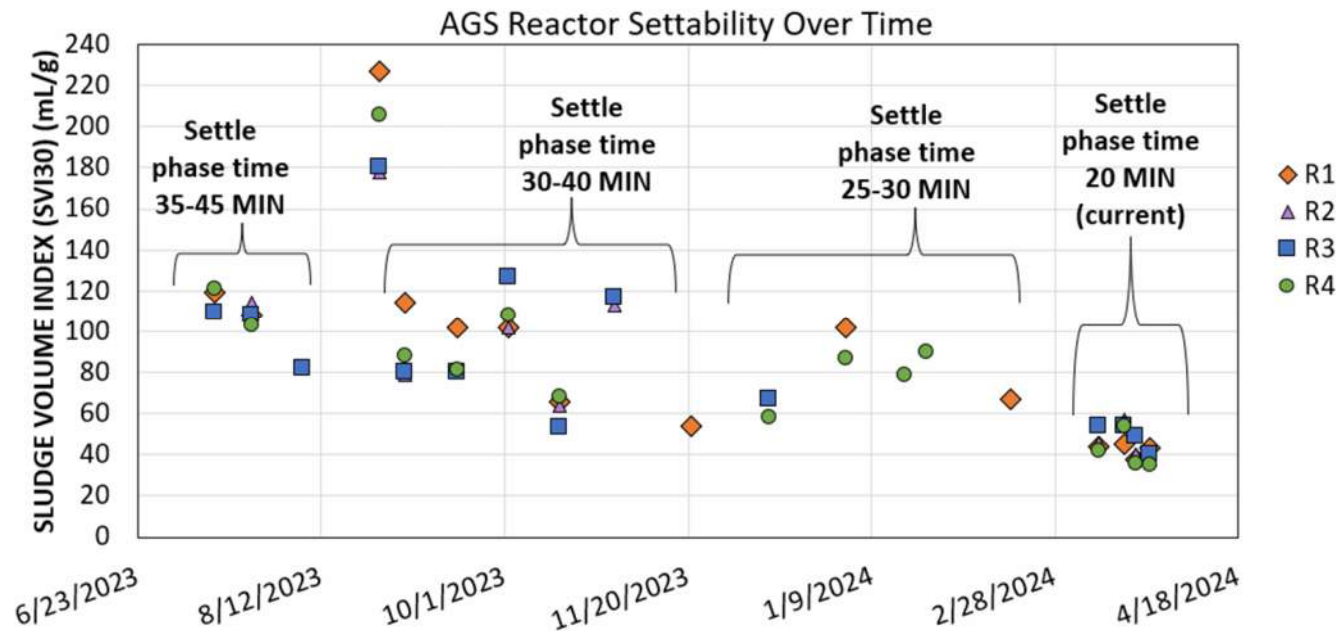


BABY GRANULES ARE GROWING – APRIL 1ST



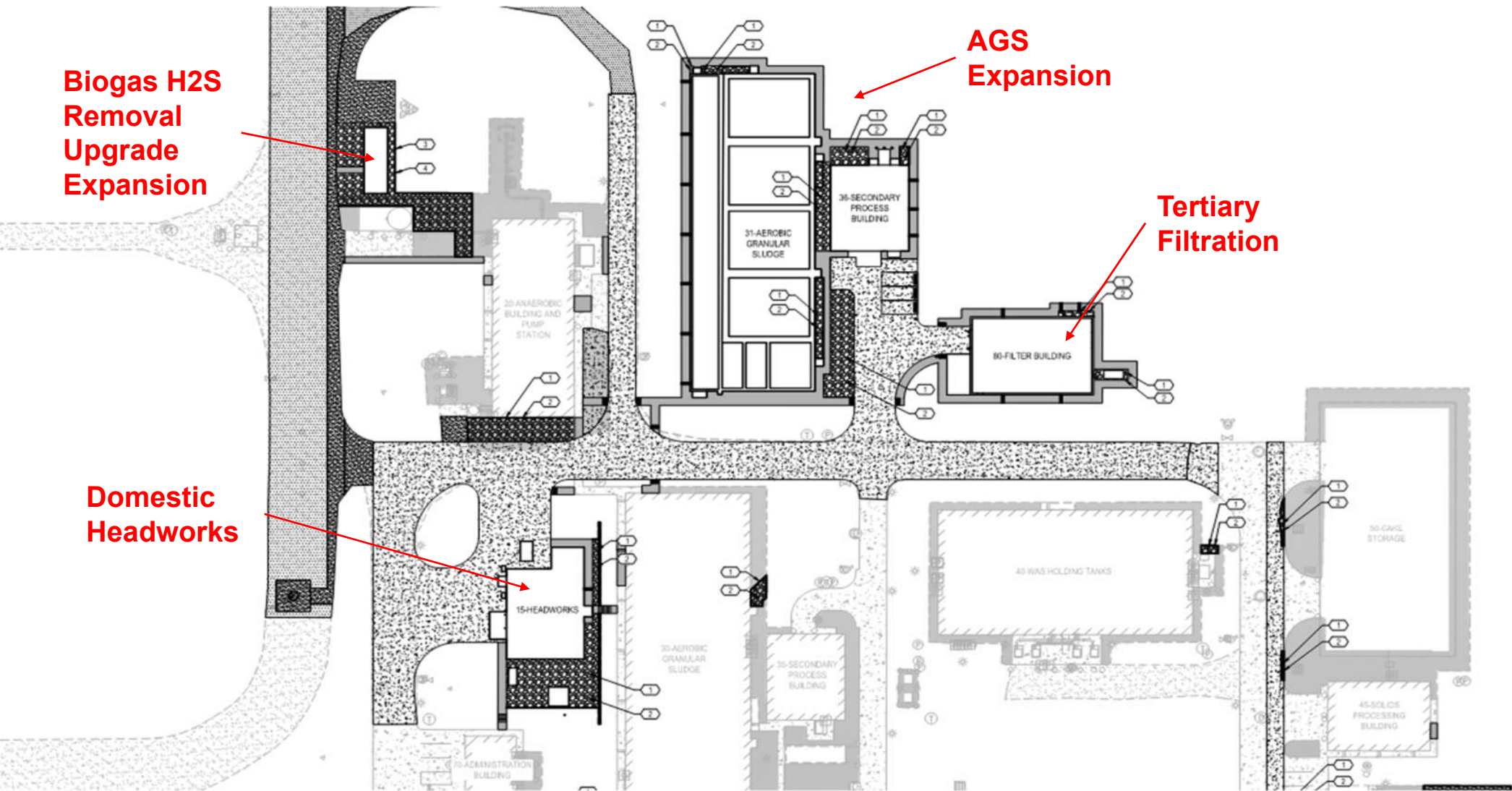
Settling and wasting

- Settleability has improved significantly with granulation
 - SVI30: 35-45 mL/g
 - SVI15: 50-60 mL/g



Settled Waste Activated Sludge

FUTURE DOMESTIC HEADWORKS AND AGS EXPANSION





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Questions?

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